



# Deposition prediction in a pilot scale pulverized fuel-fired combustor

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# Where is Cranfield University?





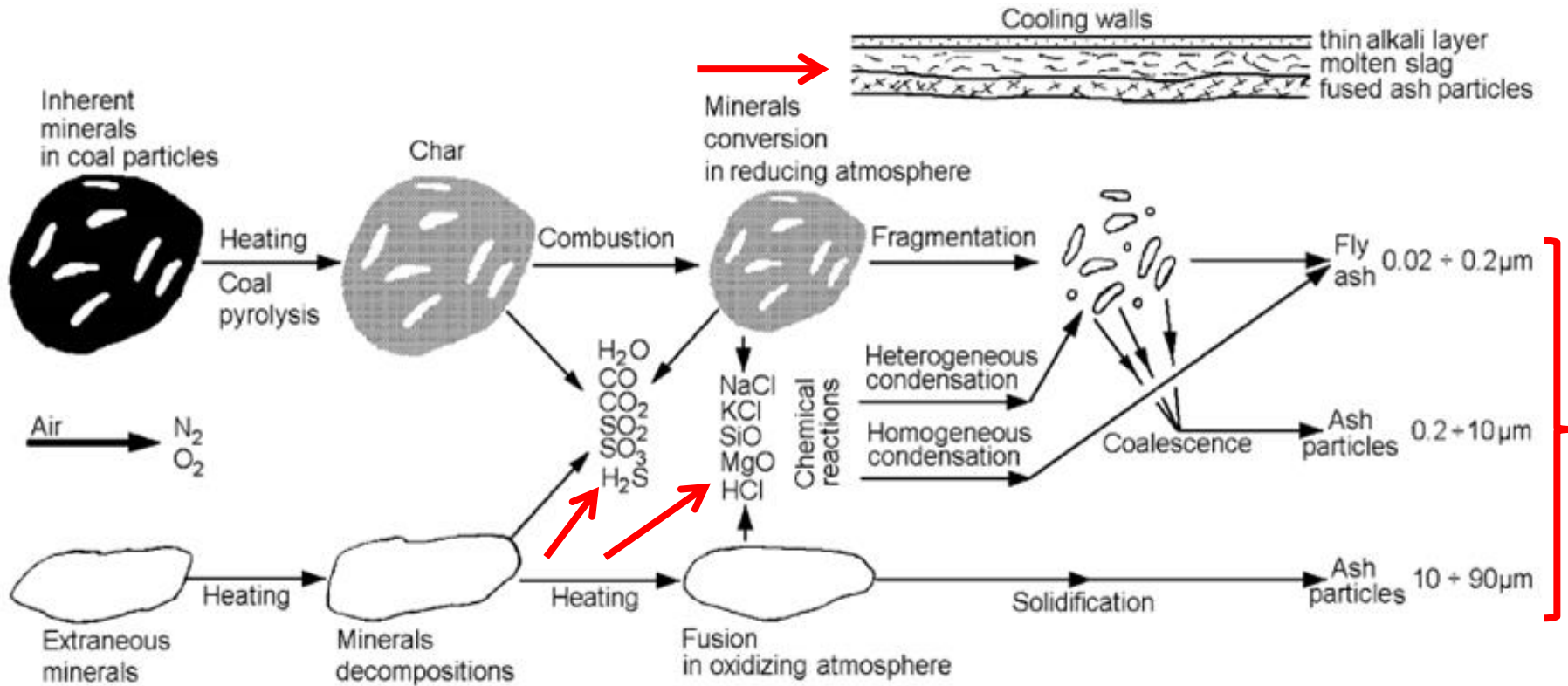
# Presentation Outline

- Background
- Methodology
  - Experiments
  - Modelling
- Results and Discussions
  - Deposit characterization
  - Model prediction
- Conclusions



Slag on superheaters tubes ([www.boilers.guide](http://www.boilers.guide))

# Background



Mineral matter transformation mechanism (Tomeczek and Palugniok, 2002)



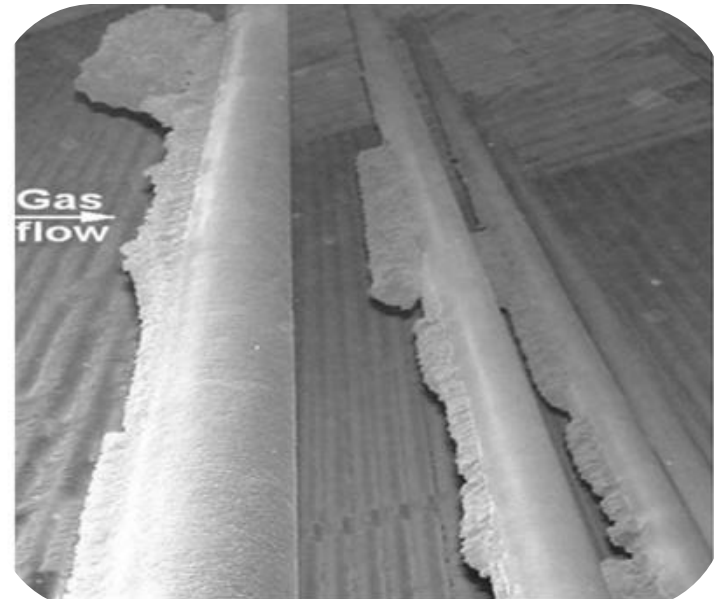
# Background

## Consequences (Rushdi et al., 2005a; Wacławiak and Kalisz, 2012)

- Insulation of heating surfaces and deterioration of boiler thermal efficiency.
- Corrosion of tubes leading to outages.
- High maintenance costs.

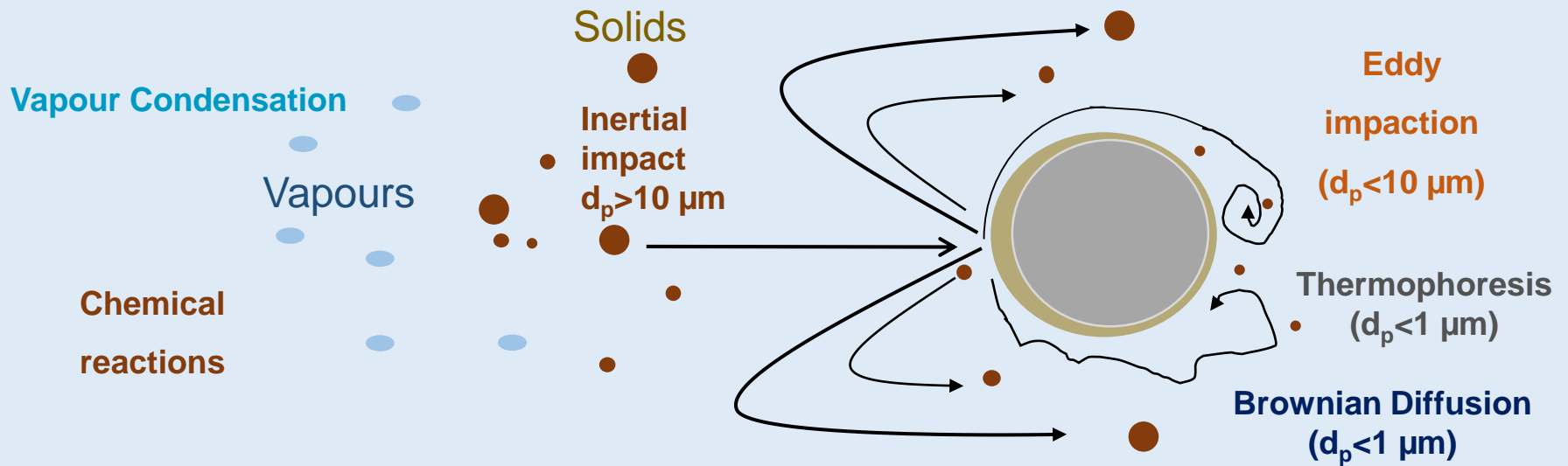


Fouling in heat exchangers (<http://scopewe.com>)

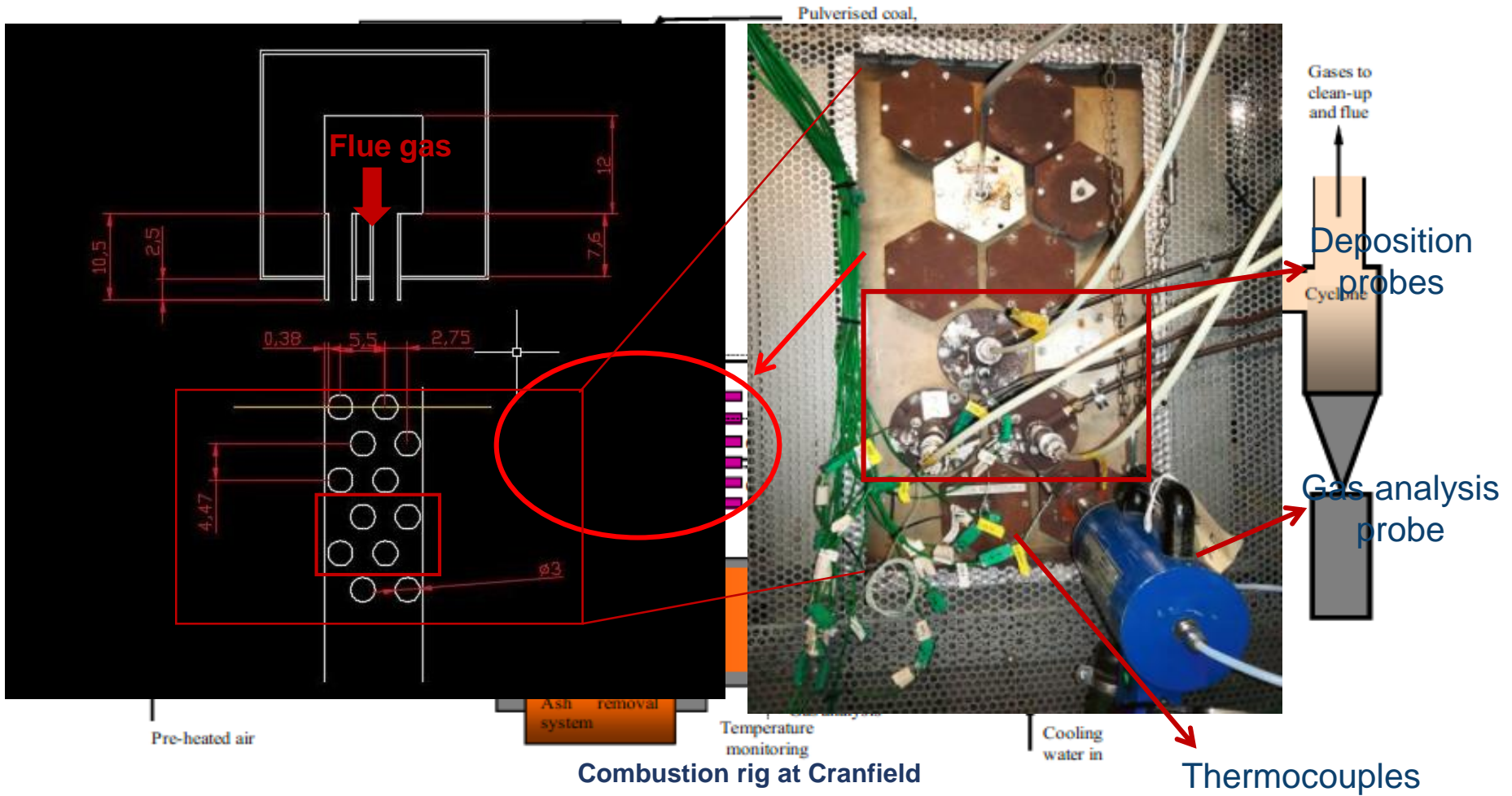


Deposit on real superheater tubes (Tomeczek and Palugniok, 2004)

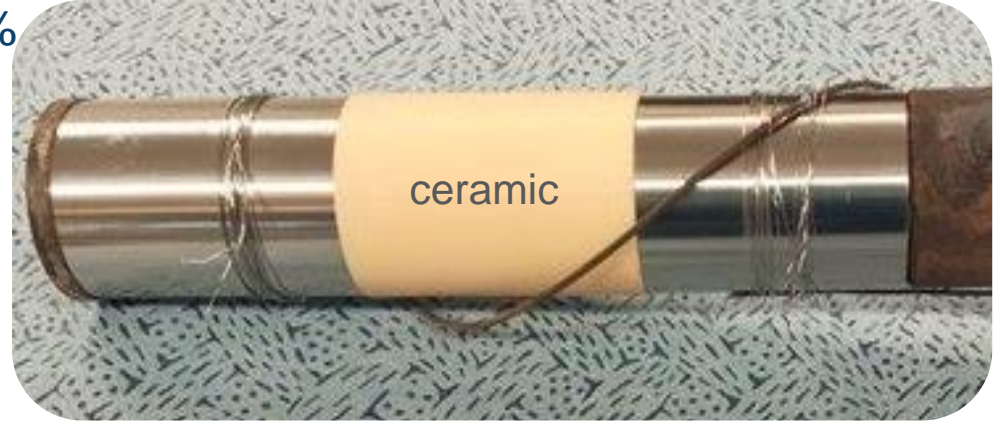
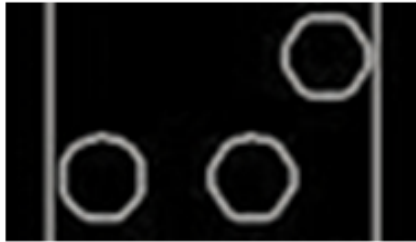
# Background Deposition Mechanisms







- Fuel: Daw Mill-Miscanthus 12 wt. %
- Probe configuration:



$T_{\text{PROBE}} = 773 \text{ K}$

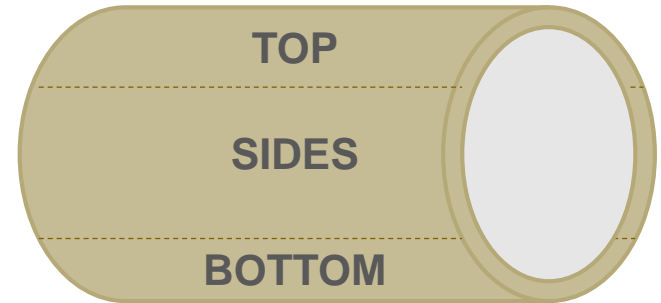






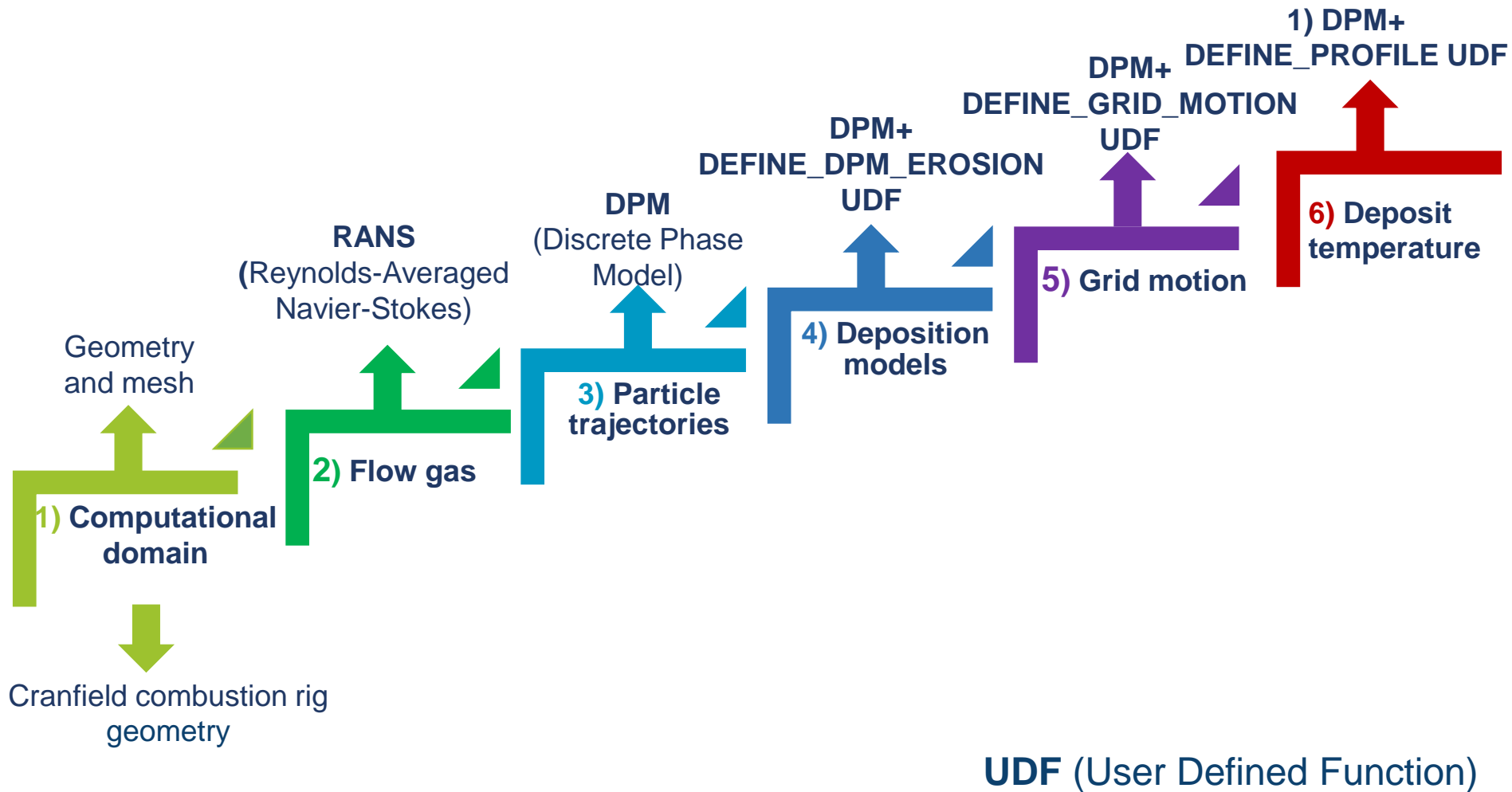
# Methodology Experiments

- Ash collection
- Deposition flux [ $\text{mg}/(\text{cm}^2 \text{ hr})$ ]
- Ash analysis – Scanning electron microscope
- Ash particle size distribution - Laser diffraction





# Methodology CFD Modelling





# Methodology CFD Modelling

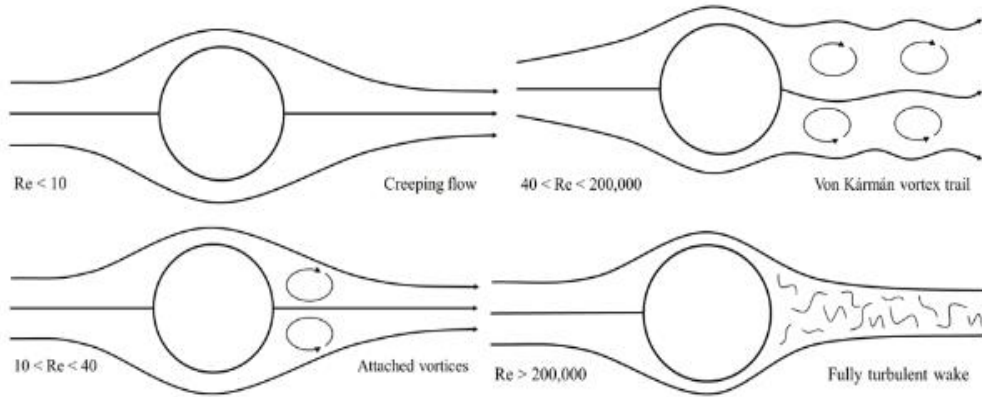
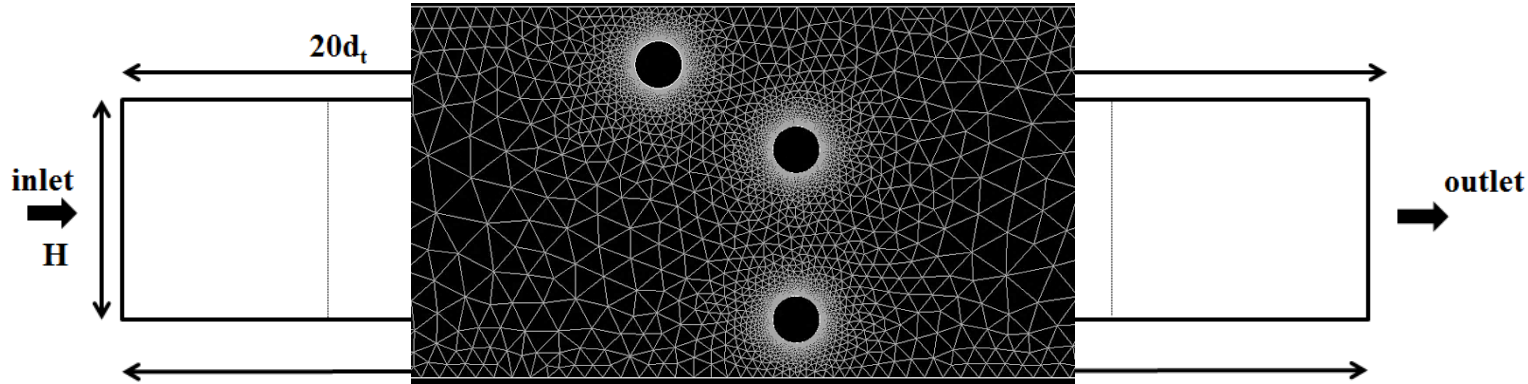
$$U_0 = 2 \text{ m/s}$$

$$T_{\text{in}} = 1273 \text{ K}$$

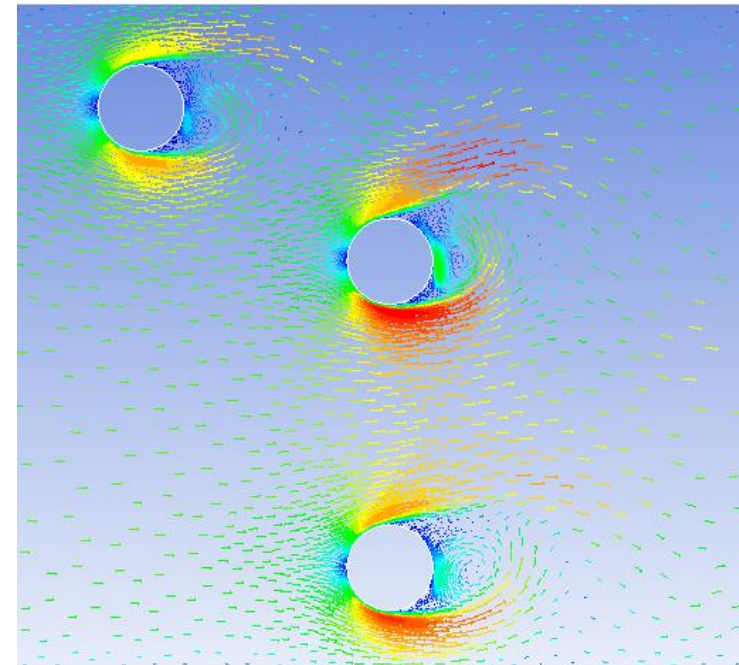
$$T_{\text{wall}} = 773 \text{ K}$$

$$d_t = 0.039 \text{ m}$$

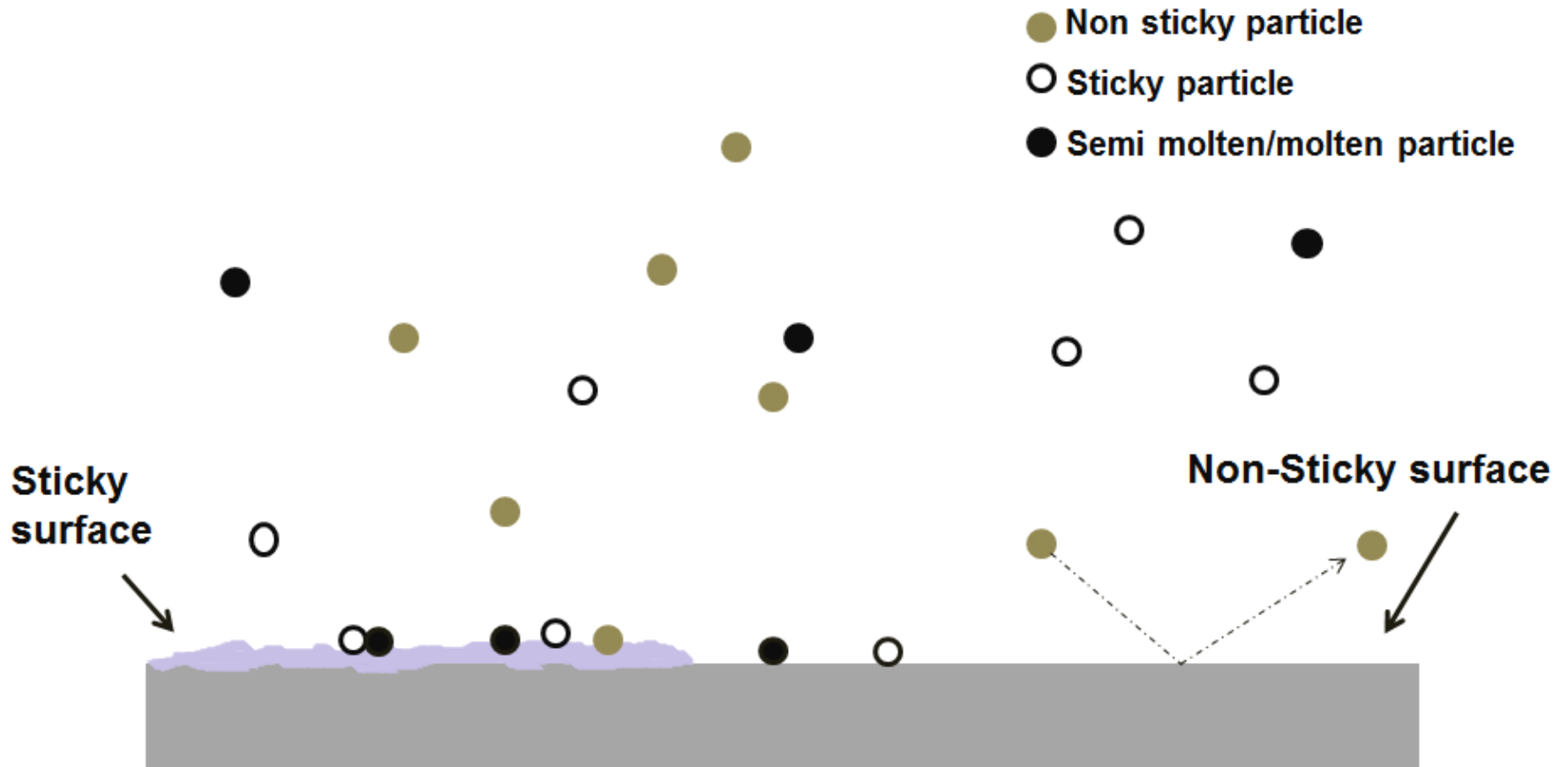
$$Re = \frac{\rho_g u_g d_t}{\mu_g} \approx 610$$



Flow around a cylinder



Velocity vectors

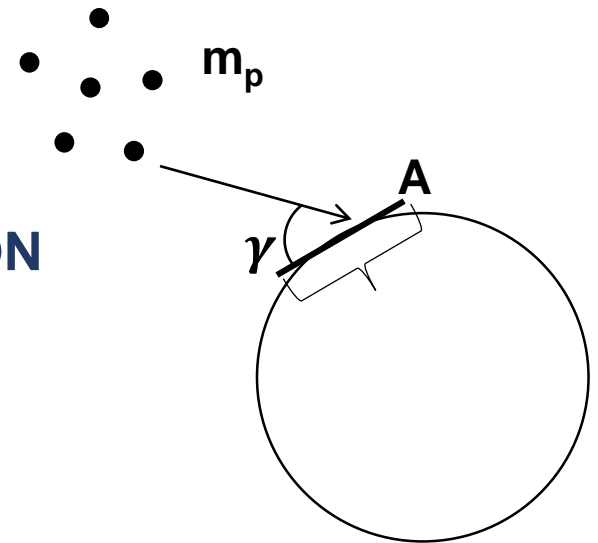


## MODIFIED FLUENT UDF: DEFINE\_DPM\_EROSION

Deposition flux:

$$m_{TOT,A} = P_{TOT} \frac{dm_p}{dA} \sin(\gamma) + m_{c,A} \text{ [kg/(m}^2 \text{ s)]}$$

$$P_{TOT} = P_S + P_P - P_S P_P$$



$P_S$  = surface stickiness probability = f(vapour condensation)

$P_P$  = particle stickiness probability = f(ash composition, ash T) → critical viscosity model

$m_c$  = condensation flux



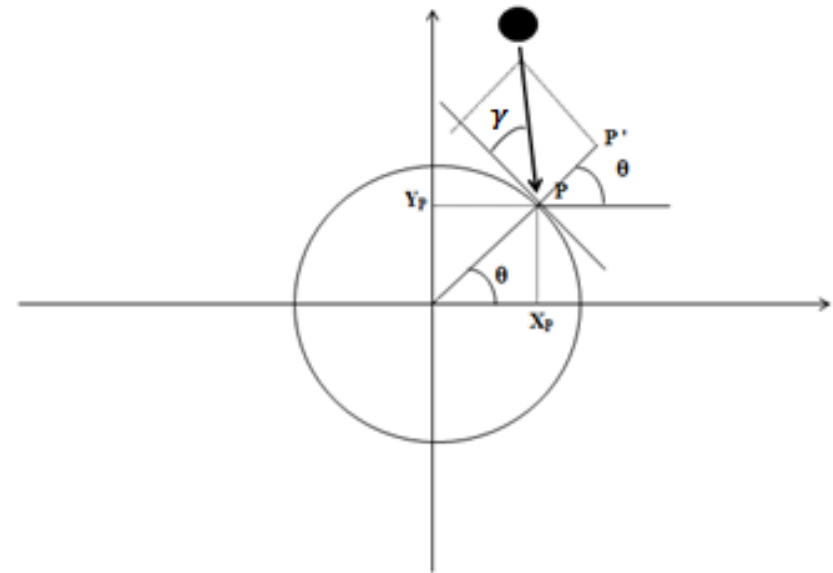
## MODIFIED FLUENT UDF: DEFINE\_GRID\_MOTION

$$\delta_i = \frac{(m_{f,A})_i}{\rho_{dep}} * t$$

$\delta_i$  = deposition thickness at node  $i$  [m];

$\rho_{dep}$  = deposit density [kg/m<sup>3</sup>];

$t$  = time [s].



$$\begin{cases} x'_p = x_p + \delta_i \cos \theta \\ y'_p = y_p + \delta_i \sin \theta \end{cases}$$

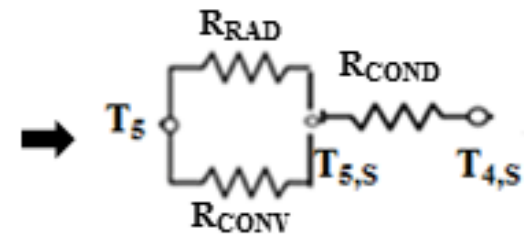


- Deposit shape
- Deposit temperature

## MODIFIED FLUENT UDF: DEFINE\_PROFILE

### NO DEPOSIT

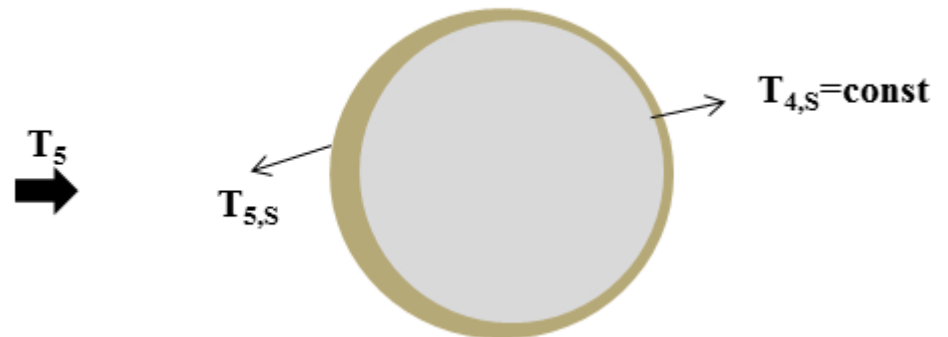
$$\dot{q}_{tot} = h_{conv} (T_5 - T_{4,S}) + h_{rad} (T_5 - T_{4,S})$$



### DEPOSIT

$$T_{5,S} = \dot{q}_{tot} R + T_{4,S}$$

$$R = \frac{\delta_i}{k_{dep}}$$



# Results and Discussion

## Deposition Flux



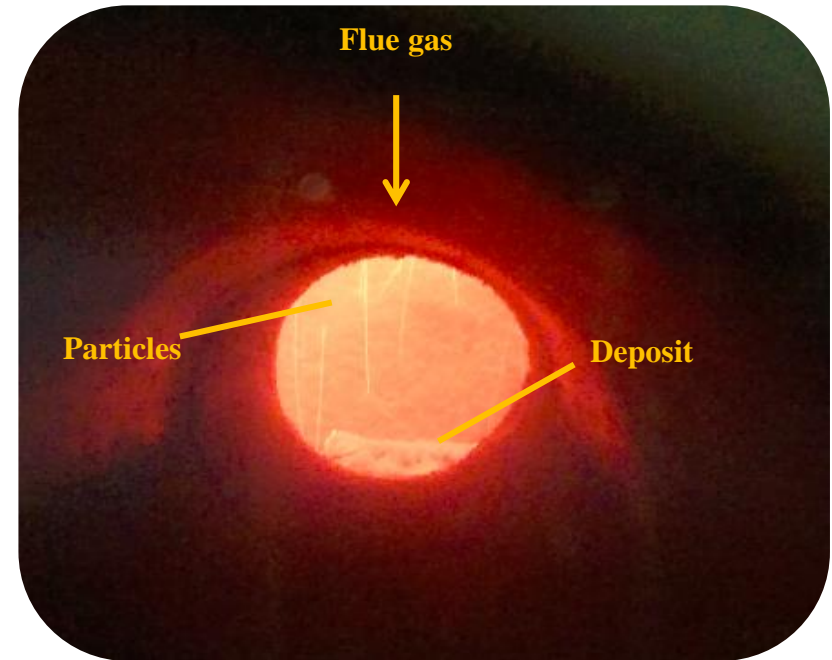
Deposit after 2.5 hours



Deposit after 5 hours



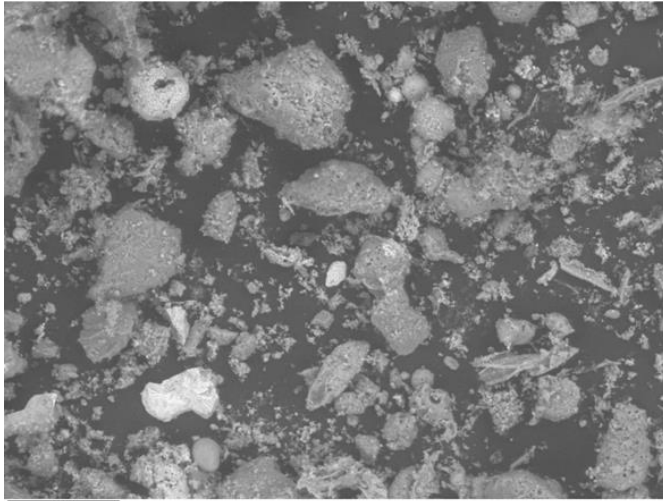
video-1519143187.mp4



Deposition probe during test

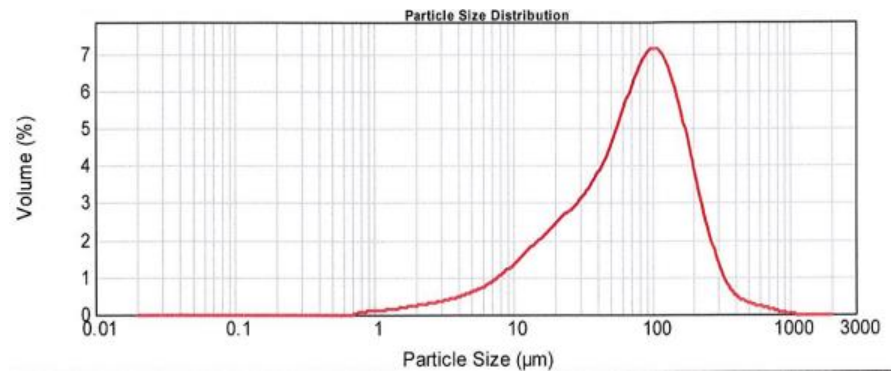
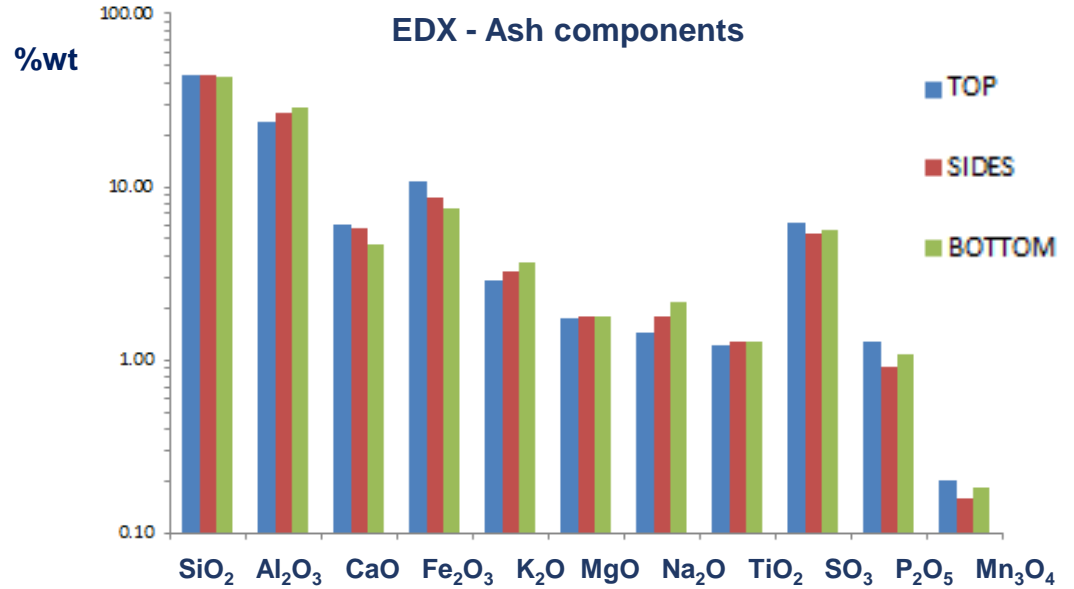
# Results and Discussion

## Ash Analysis



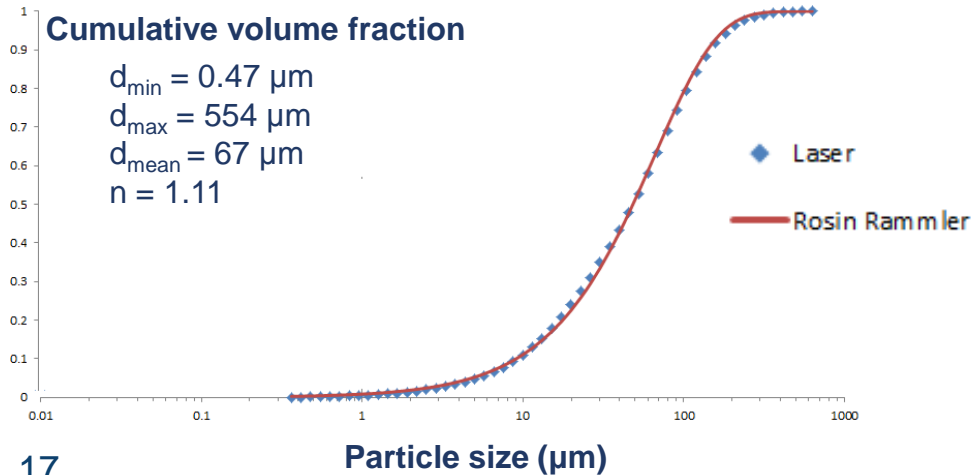
100  $\mu\text{m}$

SEM analysis



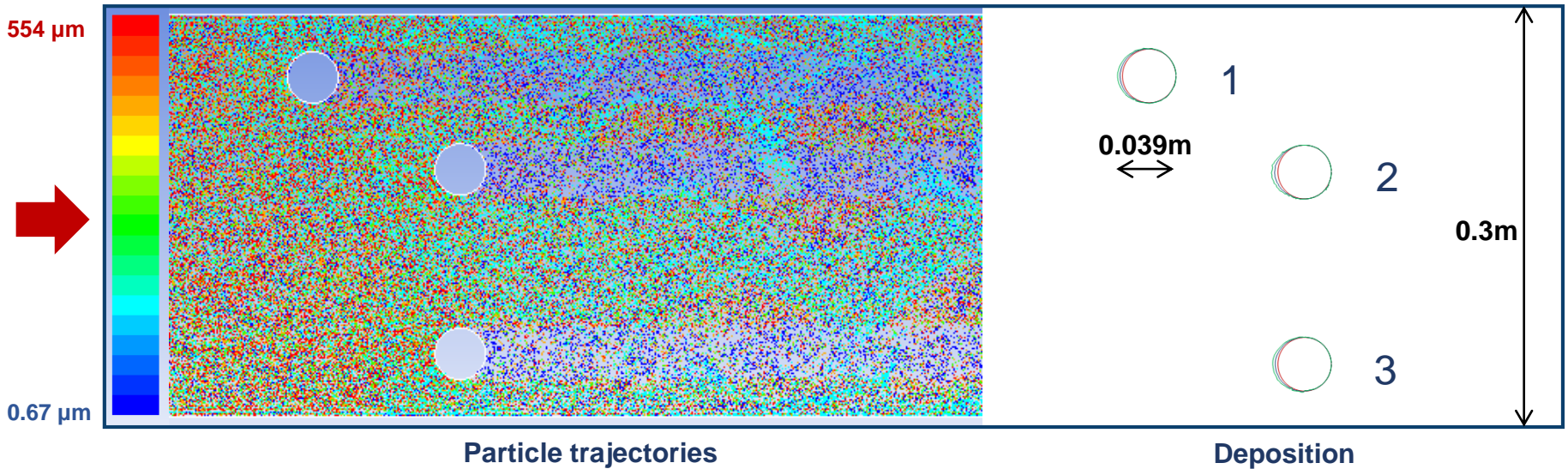
Cumulative volume fraction

$d_{\min} = 0.47 \mu\text{m}$   
 $d_{\max} = 554 \mu\text{m}$   
 $d_{\text{mean}} = 67 \mu\text{m}$   
 $n = 1.11$

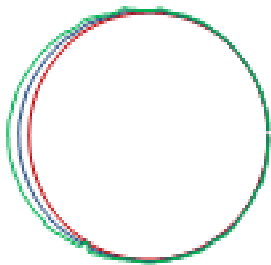


# Results and Discussion

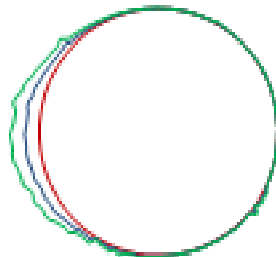
## Modelling – Particle trajectories and deposit shape



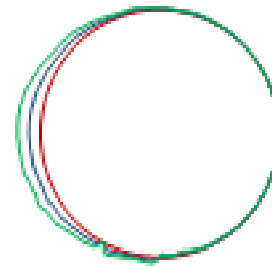
Probe 1



Probe 2



Probe 3



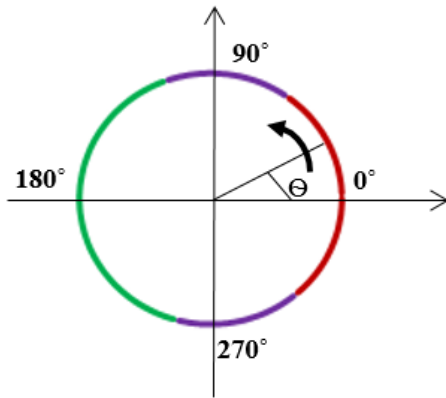
- cylinder
- t= 2.5 hrs
- t= 5 hrs



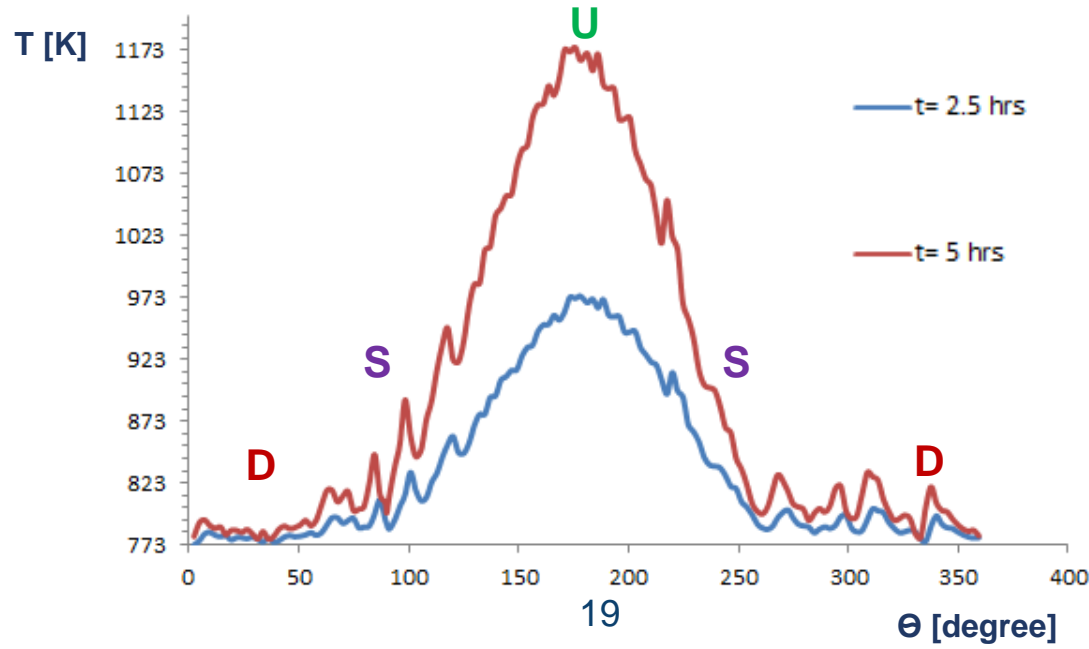
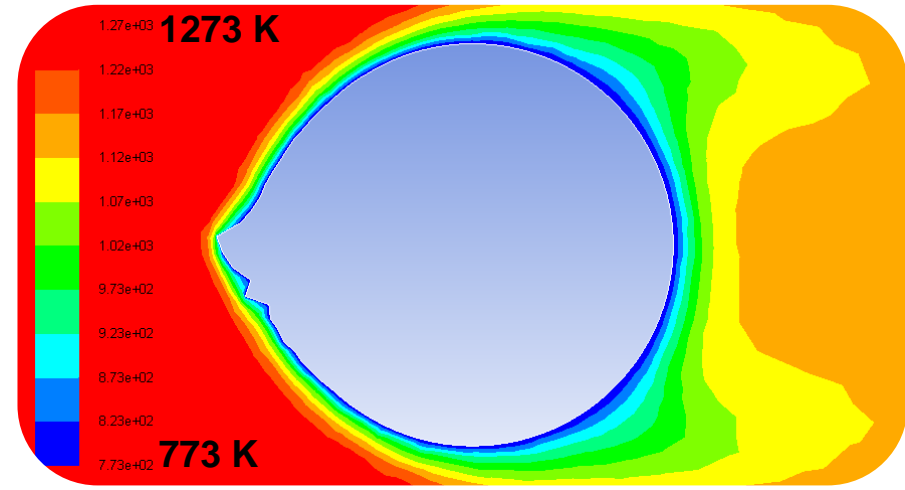


# Results and Discussion

## Modelling – Deposit temperature



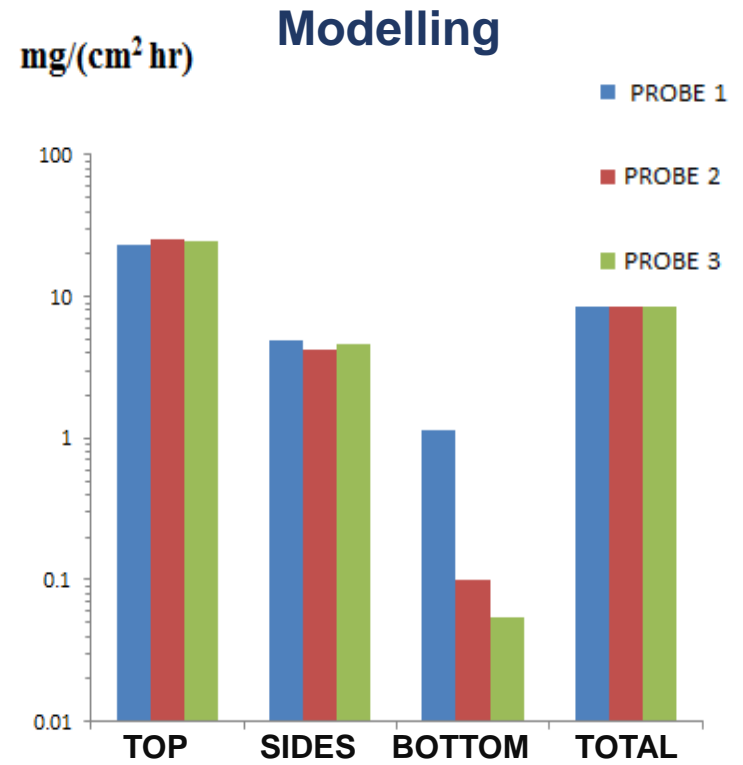
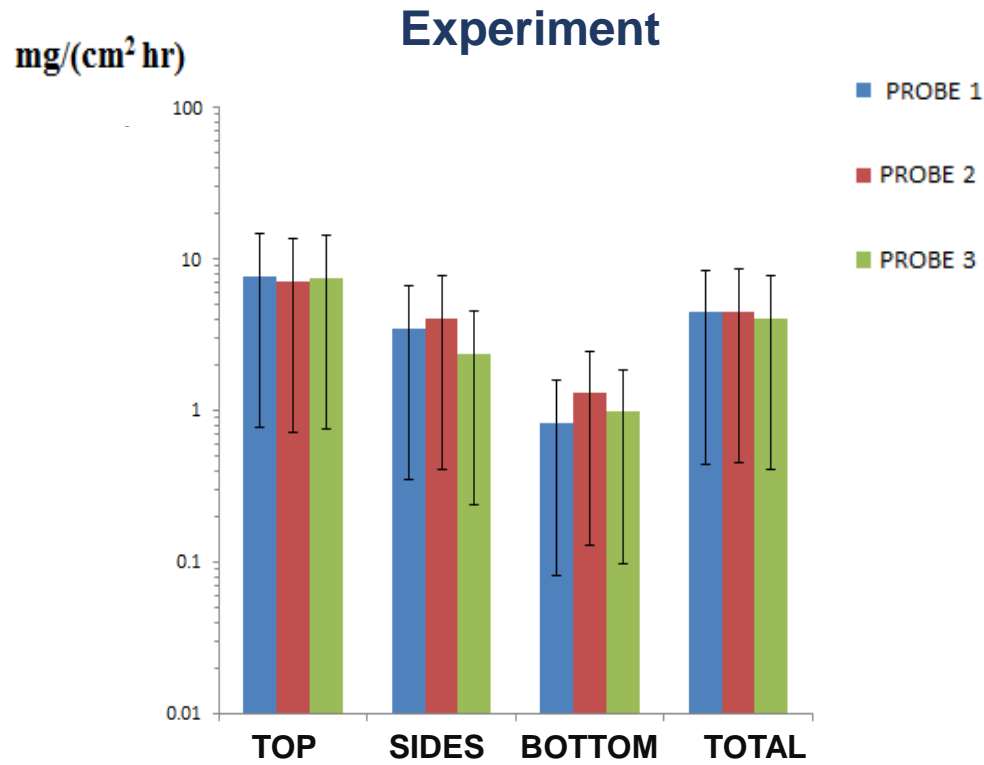
- UPSTREAM
- SIDESTREAM
- DOWNSTREAM





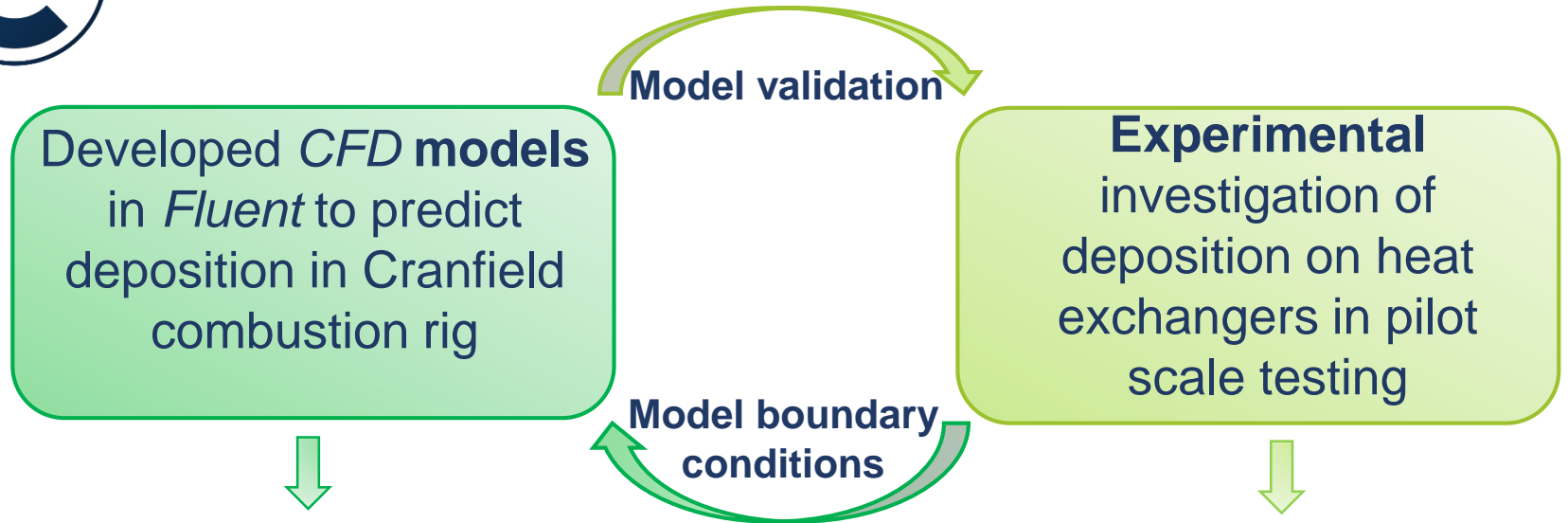
# Results and Discussion

## Model Validation





# Conclusions



Developed *CFD* models in *Fluent* to predict deposition in Cranfield combustion rig

**Experimental** investigation of deposition on heat exchangers in pilot scale testing

- Ash particle trajectories (DPM)

Modified UDFs:

- Deposition flux (DEFINE\_DPM\_EROSION)
- Deposit shape (DEFINE\_GRID\_MOTION)
- Deposit temperature (DEFINE\_PROFILE)

Predictions:

Deposition fluxes, deposit shapes...

- Daw Mill and Miscanthus 12 wt.%
- Ash composition and fly ash particle size distribution analyses
- Deposition flux measurements
- Deposit shapes



# Acknowledgment

- Flex E Plant Consortium
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  - Prof. Nigel Simms
  - Prof. John Oakey



**Thank you for your attention!!!**

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