

Presentation Overview

- Introduction /Motivation
- Aims and Objectives
- Methodology
- Results and Discussions
- Conclusion

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Introduction

- There is a worldwide drive to dispose tyres effectively;
- This is due to the huge number of waste tyres produced annually;
- 2.7 billion units of tyres were produced in 2017 and 1 billion units were disposed;
- The disposal of waste tyres is currently a challenge,
- Dumping of tyres in landfills is no longer permitted in some countries

Motivation

- Energy recovery from waste tyre through gasification is an alternative process for the effective disposal of tyres;
- Gasification of tyres is a process in which air, oxygen and or steam reacts with tyres in an endothermic reaction to produce mainly syngas (CO and H_2) and other byproducts are CO₂, light hydrocarbons and char
- $Tyres \rightarrow heavy hydrocarbons + light hydrocarbons + char$
- chars \longrightarrow CO + H ₂

Problem Statement

- One challenge is the low rate of tyre char gasification; this leads to a lower overall efficiency of the tyre gasification process
- One way of increasing the rate of tyre char gasification is by co-gasification with fuels that have a higher rate of gasification
- Lahijani et al (2013) co-gasified tyre and Palm empty fruit bunch and Almond shell.
- They reported that the rate of tyre gasification was increased in the blends with the Tyre+ Palm fruit having the highest gasification rate.
- The was observed by the reduction of the activation energy in the tyre-char/ Palm fruit blend
- There have not been any report on the co-gasification of tyre and bamboo and tyre and Refuse Derived fuel (RDF) from Municipal Solid Waste .
- This study aims to evaluate the co-gasification tyre of bamboo and RDF and determine its kinetic parameters such as Activation energy (Ea) and pre-exponential factor (A).



Methodology

- Waste tyre was shredded to remove steel cords and cut into small granules of 500 micron
- Bamboo (Dendrocalamus asper) was also shredded into 500 micron
- Refuse derived fuel was obtained from MSW (Paper +Plastics) was also shredded into 500 micron

Sample	Waste Tyre (WT)	Bamboo (BA)	Refuse Derived Fuel (RDF)
Proximate- Analysis (wt%)			
Inherent Moisture Content	0.7	5.45	2.38
Volatile Matter Content	65.6	71.93	87.67
Ash	5.6	3.71	3.15
Fixed Carbon(by difference)	28.1	18.91	6.81
Gross Calorific Value (MJ/kg)	37.83	17.87	30.42
Ultimate Analysis (wt%)			
Carbon	83.8	45.80	64.50
Hydrogen	8.18	6.14	11.17
Nitrogen	0.24	0.68	3.92
Total Sulphur	1.58	0.93	0.18
Oxygen (by difference)	6.2	47.38	14.70

Methodology

- Gasification experiments were carried out in a thermogravimetric analyser and carbon dioxide was used as the gasifying agent.
- At 800°C, 850°C,900°C and 950°C

Sample
100% Tyre
100% Raw Bamboo
100% RDF
20% B + 80% T
40% B + 60% T
50% B + 50% T
60% B + 40% T
80% B + 20% T
20% RDF + 80% T
40% RDF + 60% T
60% RDF + 40% T
80% RDF + 20% T

B:Dendrocalamus Asper Bamboo

T: Tyre; RDF: Refuse Derived Fuel



Data Analysis

- DTG Weight loss per min (%/min)
- Carbon Conversion
- X is carbon conversion, m_o is the initial sample mass, m_t sample mass at time t and m_{ash} is the mass of the residual ash
- Rate of gasification
- where k is the apparent gasification rate constant and function of carbon conversion and temperature (T)
- Ko is the pre-exponential factor, E is the activation energy and R is universial gas constant.

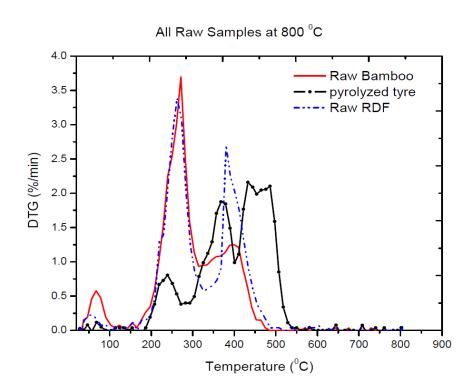
 $X = \frac{m_o - m_t}{m_o - m_{ash}}$

 $R = \frac{dX}{dt} = k(T)f(X).$

 $k = koe^{-E/RT}$

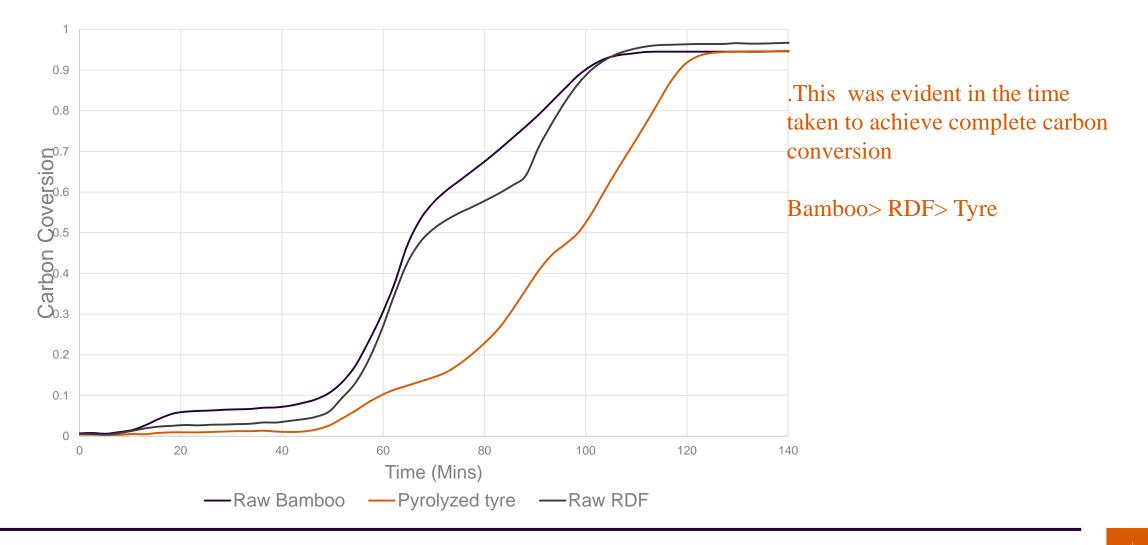


Results and Discussion

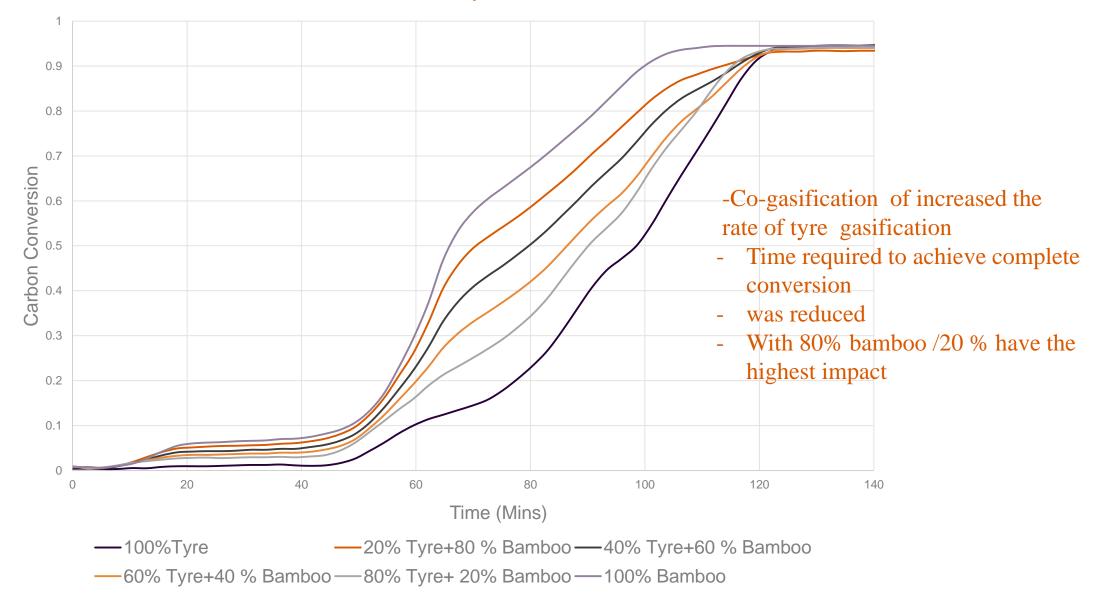


- Based on DTG Curve for the fuel samples(Raw Bamboo, Pyrolyzed Tyre and Raw RDF), there are three main stages of gasification; firstly drying and then devolatilisation and lastly char gasification
- The degree of weight loss for each of the stages were different for the different fuel samples
- Drying ; Raw Ramboo (~10%), Raw RDF(~5%), Pyrolyzed char(~2%)
- Devolatisation; Ramboo (~76%), Raw RDF(~74%), Pyrolyzed char(~48%)
- Char gasification; Ramboo (~10%), Raw RDF(~7%), Pyrolyzed

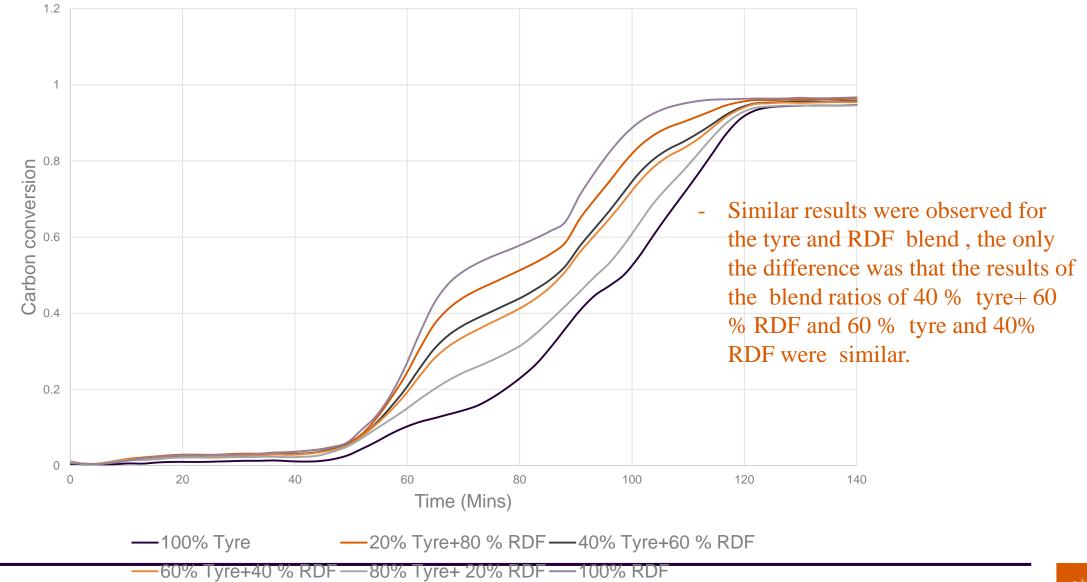
<u>char(~2%)</u>



Blends of Tyre and Bamboo



Blends Tyre and RDF



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Kinetic parameters of the samples during gasification

Sample	R ²	Ea	А	
		(kJ/mol)	(min) ⁻¹	
100% Tyre	0.9726	41.10	7.23E+02	
100% Raw Bamboo	0.9182	27.01	1.70E+02	
100% RDF	0.9095	31.40	2.72E+02	
20% B + 80% T	0.9875	29.80	1.22E+02	
40% B + 60% T	0.9684	27.04	8.15E+01	
60% B + 40% T	0.9451	26.00	7.75E+01	
80% B + 20% T	0.9055	25	7.62E+01	
20% RDF + 80% T	0.9809	31.70	1.54E+02	
40% RDF + 60% T	0.9555	30.90	1.62E+02	
60% RDF + 40% T	0.9399	30.50	1.57E+02	
80% RDF + 20% T	0.9205	30.50	1.87E+02	

- There was a reduction in the activation energy for tyre co-gasification with the cogasificaton of bamboo having the highest reduction.
- The highest reduction in activation energy of the tyre-char gasification was from 41kJ/mol to 30 kJ/mol in tyre-RDF blend; to 25 Kj/ mol in tyre-bamboo blend
- At 80 % Bamboo + 20% Tyre and 80%
 RDF + 20% for both types of blends
- In the RDF + tyre blend the activation energy at 40% RDF+ 60% tyre; 60% RDF+ 40 tyre and 80% RDF + 20% tyre were similar.

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Conclusions

- Bamboo had the highest rate of gasification followed by RDF and lastly tyre
- The co- gasification of tyre and bamboo and RDF increased the rate of tyre-char gasification by reducing its activation energy during gasification
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- The highest reduction in activation energy of the tyre–char gasification was from 41kJ/mol to 30 kJ/mol in tyre-RDF blend; to 25 Kj/ mol in tyre-bamboo blend was obtained at 80 % Bamboo + 20% tyre and 80% RDF + 20% tyre for both types of blends .
- The effect of blend ratio on activation energy was slightly different for the two different blends.
- In the RDF + tyre blend the activation energy the blend ratios of 40% RDF+ 60% tyre; 60% RDF+ 40 tyre and 80% RDF + 20% tyre were similar, while it was different for the Bamboo- tyre blend



Thank you!!!