





# Efficient Sm modified Mn/TiO<sub>2</sub> catalysts for selective catalytic reduction of NO with NH<sub>3</sub> at low temperature

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**01** Research background

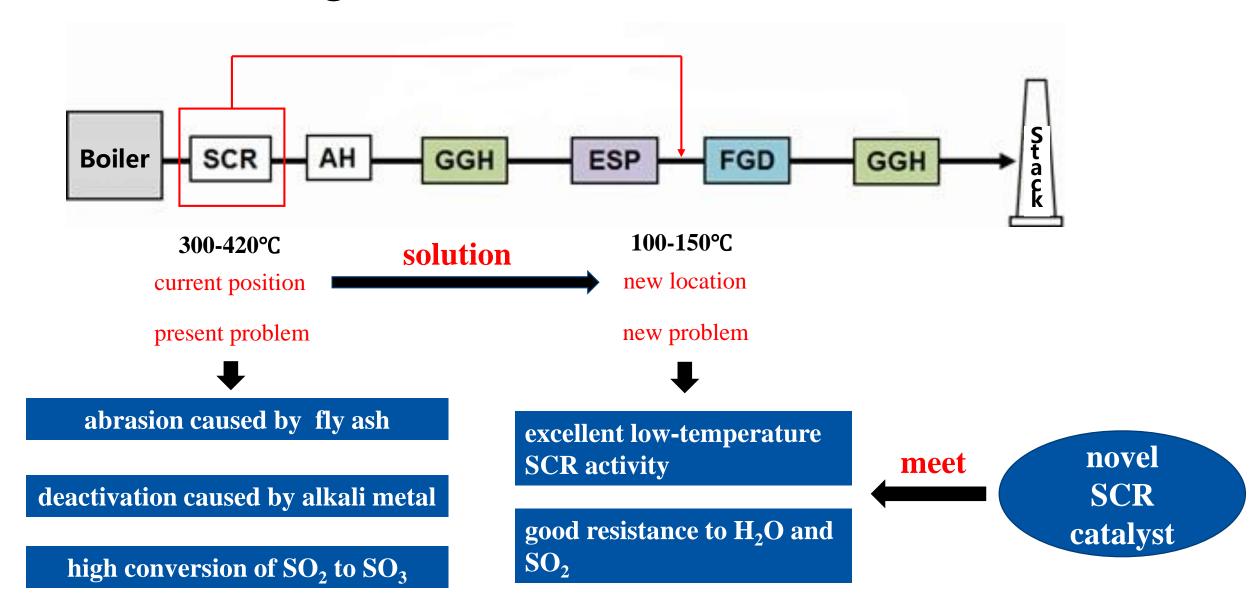
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### Research background





### **Experimental**

### Catalyst design

MnO<sub>x</sub> has excellent low temperature SCR activity

Mn<sup>[1]</sup>-Sm/TiO<sub>2</sub><sup>[2]</sup>

**Propose** 

TiO<sub>2</sub>-supported MnO<sub>2</sub> catalysts showed more promising SCR activity

Sm can prevent transition from Mn<sup>4+</sup> to Mn<sup>3+</sup>

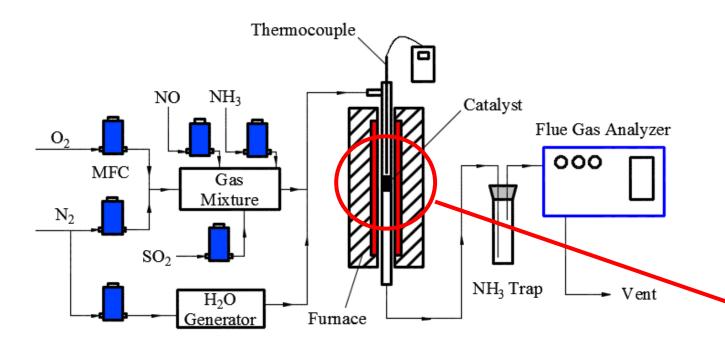
[1] D.A. Peña, B.S. Uphade, P.G. Smirniotis, J. Catal. 221 (2004) 421-431.

[2] P.G. Smirniotis, P.M. Sreekanth, D.A. Peña, R.G. Jenkins, Ind. Eng. Chem. Res. 45 (2006) 6436-6443.



### **Experimental**

#### **Catalytic activity test**



#### Schematic diagram of the experimental system.

$$NO_x$$
 conversion =  $\frac{[NO_x]_{in} - [NO_x]_{out}}{[NO_x]_{in}} \times 100\%$ 

$$N_{2} \text{ selectivity} = \frac{[NO_{x}]_{in} + [NH_{3}]_{in} - [NO_{x}]_{out} - [NH_{3}]_{out} - 2[N_{2}O]_{out}}{[NO_{x}]_{in} + [NH_{3}]_{in} - [NO_{x}]_{out} - [NH_{3}]_{out}} \times$$

#### **Test condition**

#### Simulated flue gas:

500 ppm NO, 500 ppm NH<sub>3</sub>, 5% O<sub>2</sub>, 5%  $H_2O(when used)$ , 100 ppm  $SO_2(when used)$  and  $N_2$  as balance

**Total flow rate:** 1L/min

Particle size: 40-60 mesh

Gas hourly space velocity: 60000 h<sup>-1</sup>

#### **Characterization**

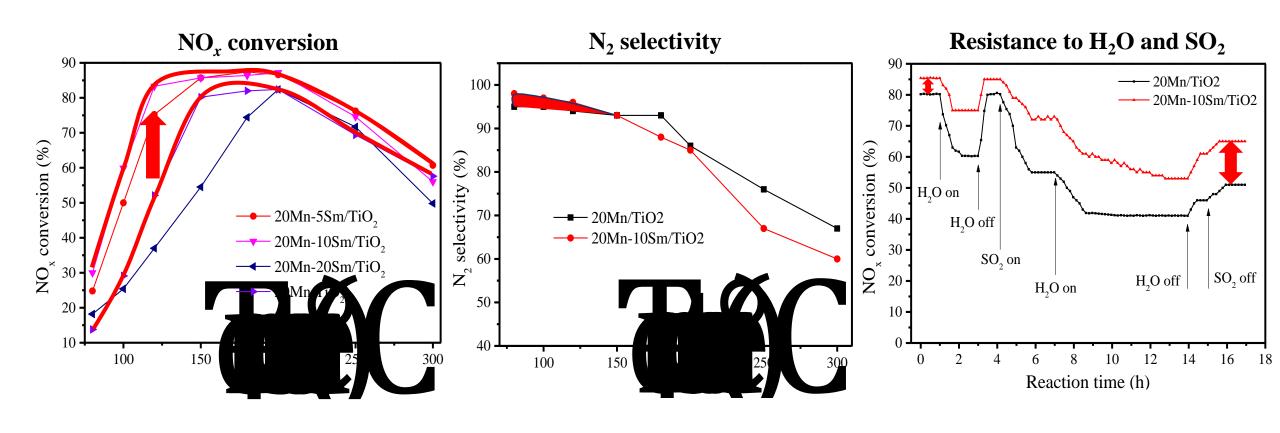
#### Physicochemical properties

XRD BET XPS NH<sub>3</sub>-TPD H<sub>2</sub>-TPR

#### **Reaction mechanism**

in situ DRIFTS

#### **Catalytic performance**



**Optimum loading: 10%** 

 $50\% \rightarrow 85\%$  at 120 °C

Higher N<sub>2</sub> selectivity

Over 95% at 80-150 °C

 $85\% \rightarrow 70\%$  for Mn-Sm

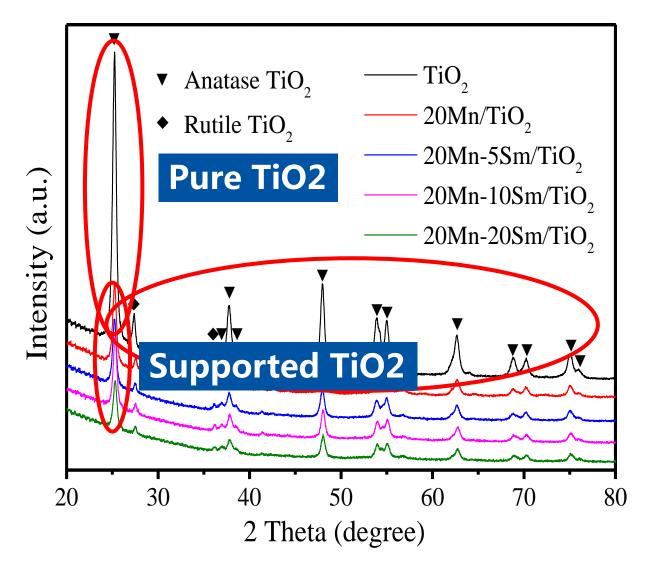
 $80\% \to 55\%$  for Mn

### **Specific surface area: BET**

catalyst	BET surface area	pore volume	average pore size	
	$(m^2/g)$	$(cm^3/g)$	(nm)	
$TiO_2$	50.45	0.24	19.41	
20Mn/TiO <sub>2</sub>	43.67	0.34	31.55	
$20 \text{Mn-5Sm/TiO}_2$	45.93	0.30	26.24	
$20 \text{Mn-}10 \text{Sm/TiO}_2$	47.69	0.33	27.38	
$20 \text{Mn-}20 \text{Sm/TiO}_2$	38.40	0.29	30.67	

- > The surface areas of Mn-Sm/TiO<sub>2</sub> catalysts increased in the presence of Sm<sub>1</sub>
- > The doped Sm could promote the dispersion of manganese oxide

### **Crystal structure: XRD**

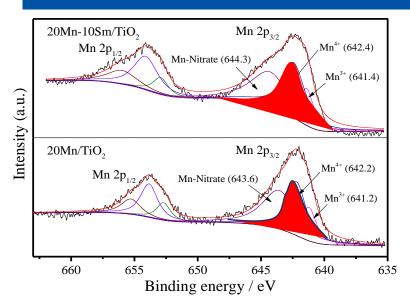


Diffraction peaks of TiO<sub>2</sub> are observed

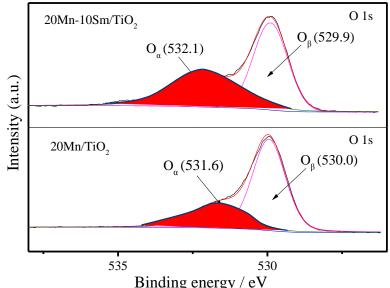
No Mn and Sm species are detected

Strong interaction between Mn and Ti

#### Oxidation state and surface atomic concentrations: XPS

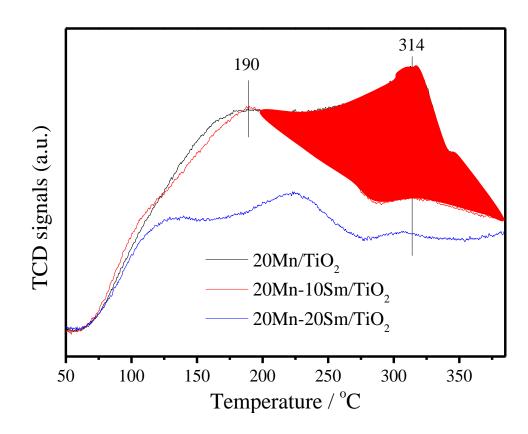


catalyst	surface atom concentration					
	Mn <sup>4+</sup> /Mn <sup>3+</sup>	Mn <sup>4+</sup> /Mn	Mn/Ti	$O_{\alpha}/O_{\beta}$	O <sub>\alpha</sub> /O	
$20 \mathrm{Mn/TiO}_2$	2.08	36.81%	0.21	0.38	27.75%	
20Mn-10Sm/TiO <sub>2</sub>	2.46	41.57%	0.43	0.54	35.10%	



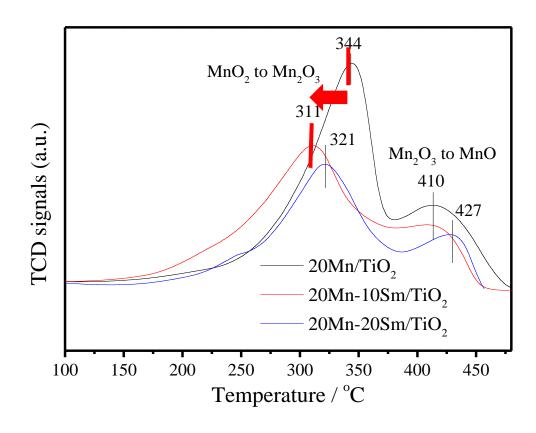
- ➤ The presence of Sm could inhibit the crystallization of manganese oxide;
- $\triangleright$  Mn could incorporate into lattice structure of TiO<sub>2</sub>;
- ➤ The addition of Sm could promote the surface active oxygen species.

### Acidity: NH<sub>3</sub>-TPD



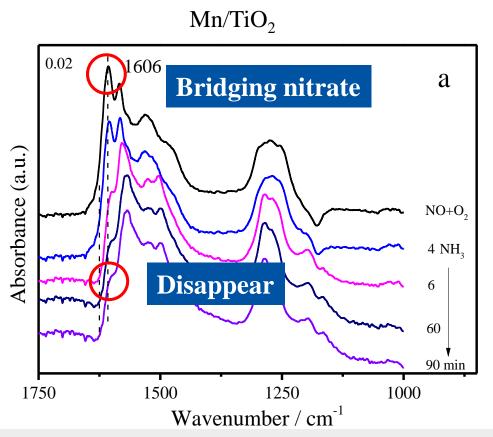
➤ Lewis acid site might not be the main factor in low-temperature NH<sub>3</sub>-SCR of NO<sub>x</sub> over these catalysts.

#### Redox property: H<sub>2</sub>-TPR

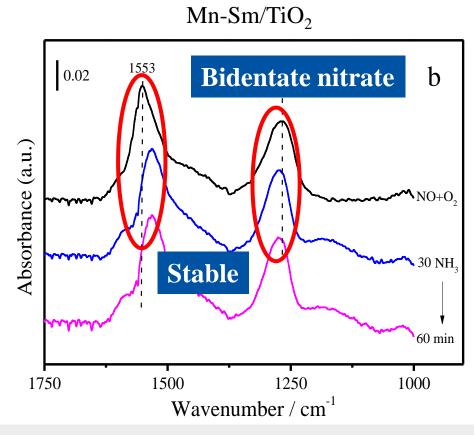


➤ The reducibility may be play an important role in low-temperature SCR activity.

#### Reaction of $NH_3$ with pre-adsorbed $NO + O_2$ : In situ DRIFTS

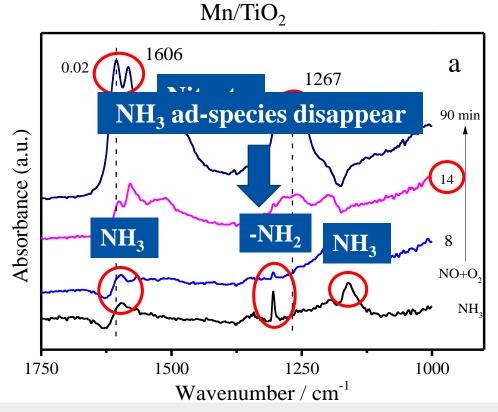


- The bridging nitrates are the main active nitrate species;
- ➤ The SCR reactions over the Mn/TiO<sub>2</sub> catalyst can proceed through L–H mechanism.

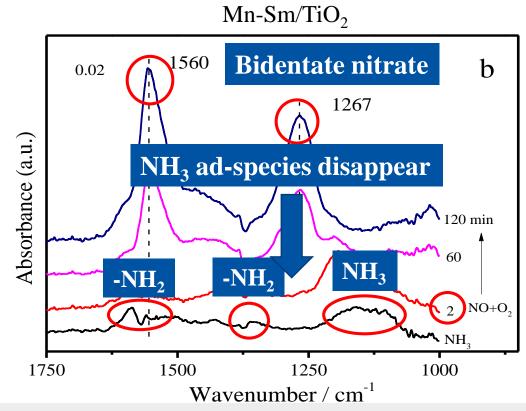


- ➤ The bridging nitrates were not formed on the surface of Mn-Sm/TiO<sub>2</sub> catalyst;
- ➤ The SCR reactions over the Mn-Sm/TiO<sub>2</sub> catalyst can not happen via L-H mechanism.

#### Reaction of NO + $O_2$ with pre-adsorbed NH<sub>3</sub>: In situ DRIFTS

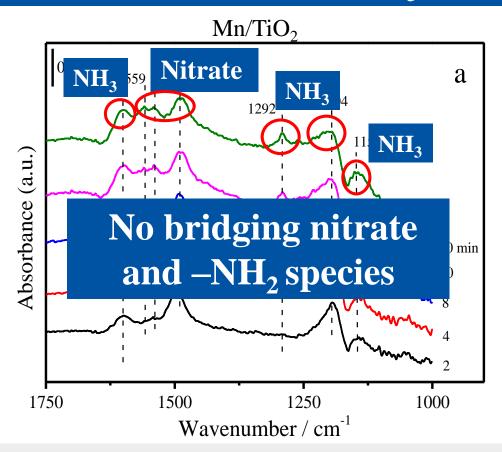


- ➤ All bands of coordinated NH<sub>3</sub>, NH<sub>4</sub><sup>+</sup> and -NH<sub>2</sub> species disappeared gradually after exposure to NO + O<sub>2</sub>;
- ➤ The SCR reactions over the Mn/TiO<sub>2</sub> catalyst can proceed through E–R mechanism.

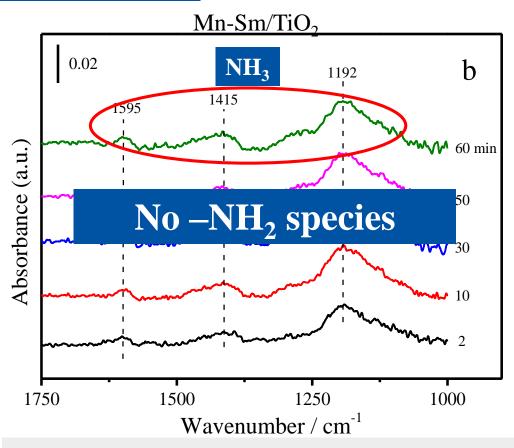


- ➤ The reaction of preadsorbed NH<sub>3</sub> with NO + O<sub>2</sub> on Mn-Sm/TiO<sub>2</sub> catalyst was significantly faster than that over Mn/TiO<sub>2</sub> catalyst;
- ➤ The Sm modified catalyst possessed more –NH<sub>2</sub> species than Mn/TiO<sub>2</sub> catalyst.

#### Adsorption and reaction of $NH_3 + NO + O_2$ : In situ DRIFTS



- $\triangleright$  The co-existence of the NH<sub>3</sub> ad-species and NO<sub>x</sub> adspecies are observed;
- ➤ The reactive bridging nitrate and the -NH<sub>2</sub> and NH<sub>4</sub><sup>+</sup> intermediates are all absent.



- ➤ The adsorption of NO can not happen in the presence of NH<sub>3</sub>;
- ightharpoonup The formed  $-NH_2$  species quickly reacted with gaseous NO to produce  $N_2$  and  $H_2O$ .

### Conclusions

- ➤ The best 20Mn-10Sm/TiO<sub>2</sub> catalyst achieved almost 85% NO conversion with a GHSV of 60000 h<sup>-1</sup> at 120 °C;
- The presence of Sm can improve the dispersion of manganese oxide and the relative concentration of surface oxygen  $(O_{\alpha})$ ;
- The SCR reaction mechanism changed by inhibiting the formation of bridging nitrate in the presence of Sm and the reactions can proceed only through Eley-Rideal mechanism;
- ➤ The enhanced oxygen transport after introduction of Sm boost the reaction rate.



## THANKS FOR YOUR LISTENING!