



Ultra-low cost ionic liquids for biorefining of waste wood

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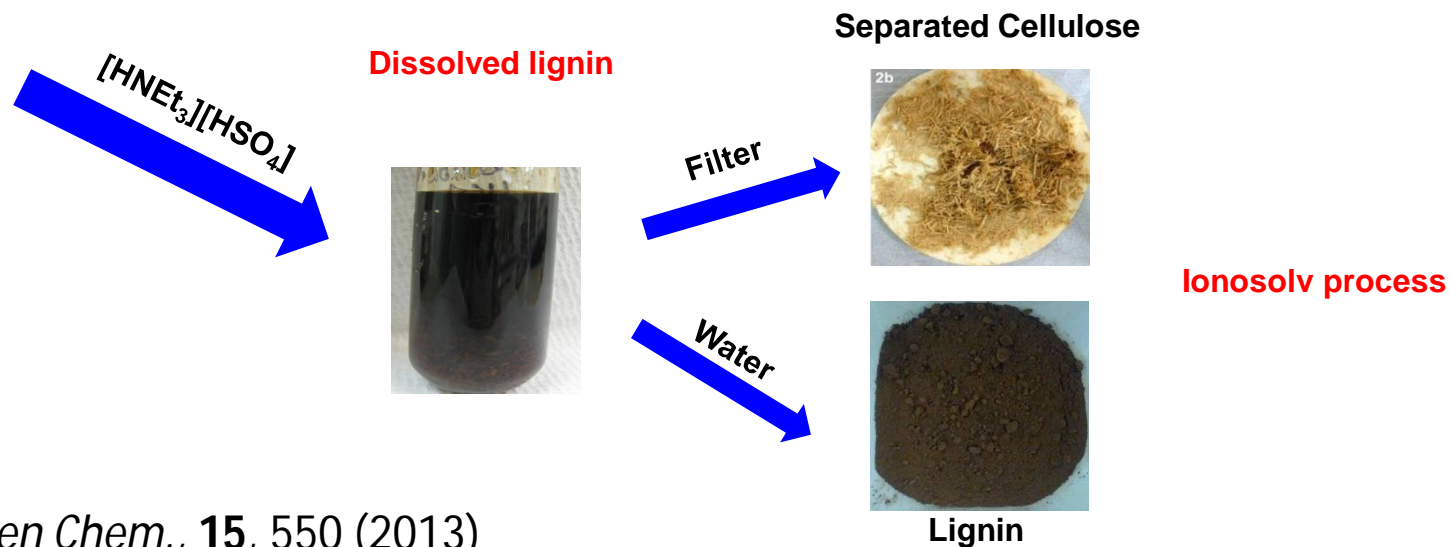
10 April 2010

Why use ionic liquids for lignocellulosic biofuels?

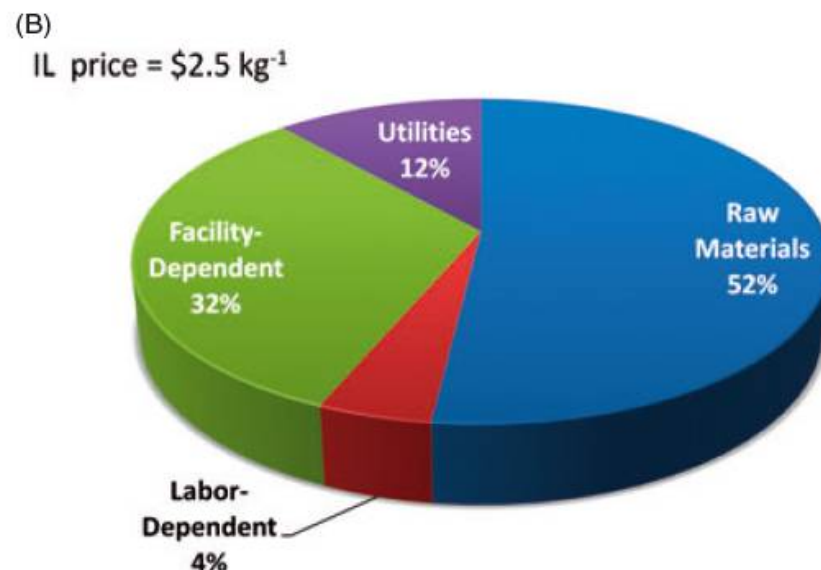
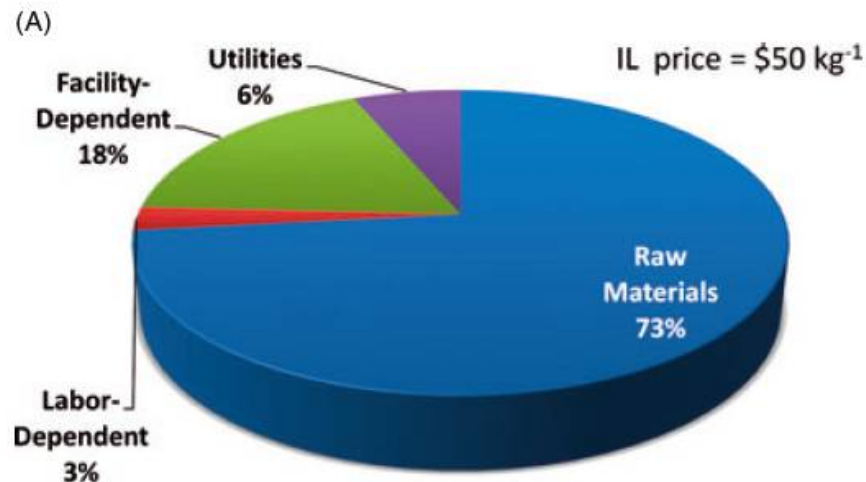
- Increase enzyme activity at minimal cost
 - Several options (kraft, ammonia, organosolv, etc.)
 - Ionic liquids provide **highest activity**
 - Ionic liquids are generally very expensive
- Ionic liquids are just organic salts
 - Have **advantages** over organic solvents
 - Can be designed for a specific function
 - Have **disadvantages** also
- The application must be logical
 - Rational choices must be made

ionoSolv lignin extraction

- Most ILs are not good solvents for cellulose
 - Biocatalytic conversion of cellulose to fuels
 - Want de-lignified cellulose
- **ionoSolv: Dissolve lignin not cellulose**
 - Highly pure cellulose easily recovered
 - Lignin solution for chemical conversion
 - Water helps the process
 - *Do salts have to be expensive?*



Process economics – IL cost are critical



- Other important factors
 - Recycling rate
 - Biomass loading

Can Ionic Liquids be Cheap?

- $[\text{C}_4\text{C}_1\text{im}][\text{NTf}_2]$ (Sigma-Aldrich):

– \$2500/kg (250g)

- Ethaline (Scionix):

– \$60/kg (50kg)

- $[(\text{C}_8)_3\text{C}_1\text{N}][\text{Br}]$ (Solvent Innov.):

– \$40/kg (100t)

- $[\text{C}_2\text{C}_1\text{im}][\text{acetate}]$

– \$60/kg (bulk guesstimate)

- $[\text{C}_1\text{Him}][\text{HSO}_4]$

– \$2.60/kg (bulk estimate)

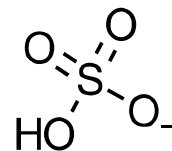
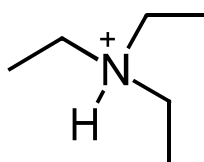
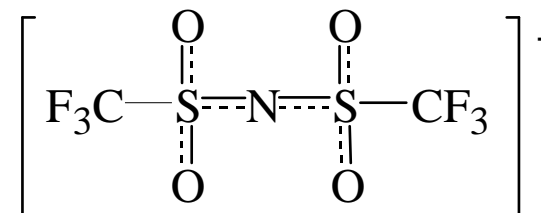
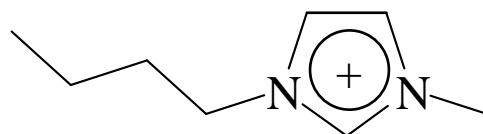
- $[(\text{C}_2)_3\text{NH}][\text{HSO}_4]$

– \$0.84/kg (bulk estimate)

- $[(\text{C}_4)(\text{C}_1)_2\text{NH}][\text{HSO}_4]$

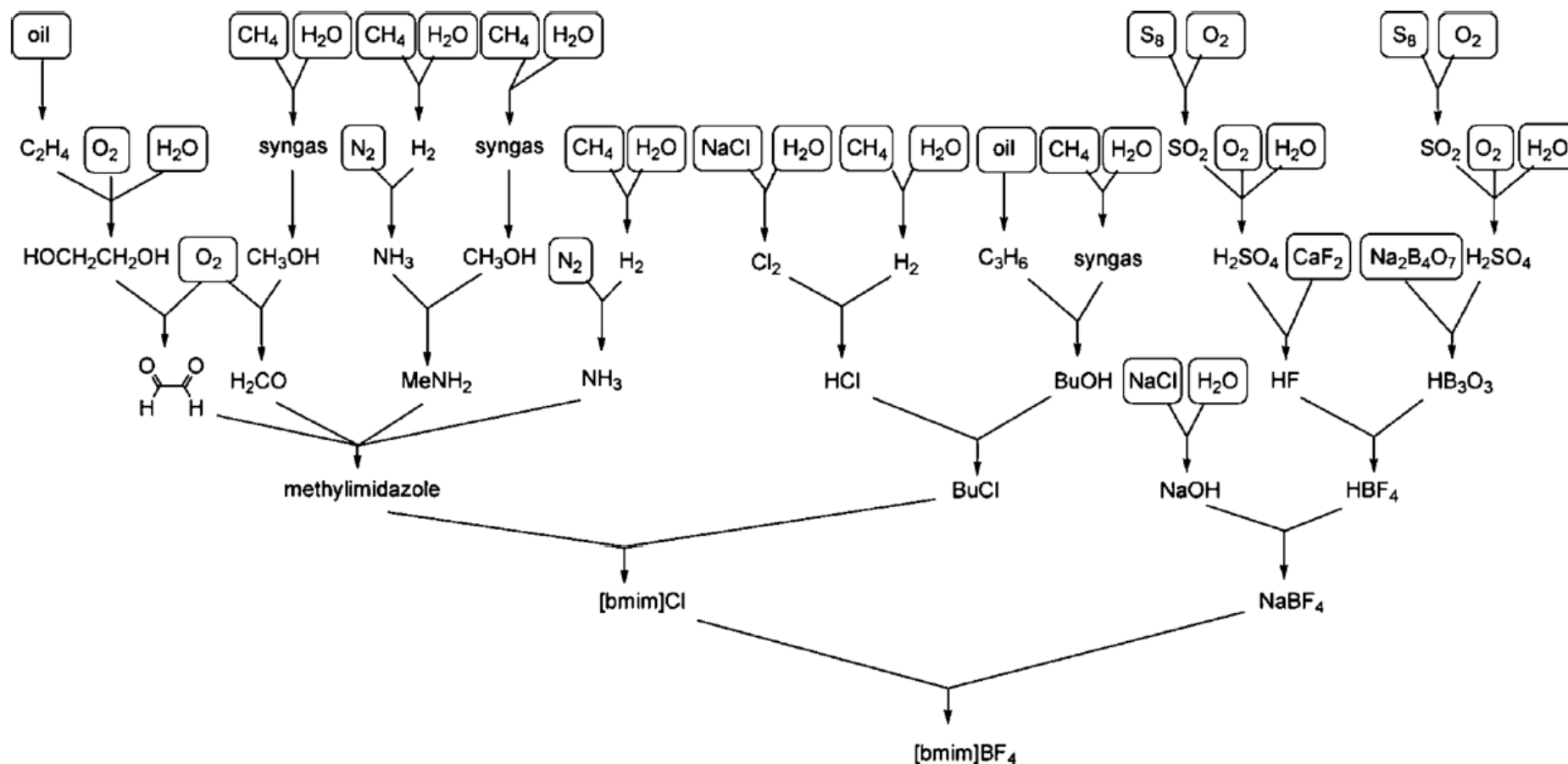
– \$0.44/kg (bulk estimate)

- **Acetone: \$1.30/kg**



Chen *et al.*, *Green Chem.*, **16**, 3098 (2014)

How NOT to make a Green solvent

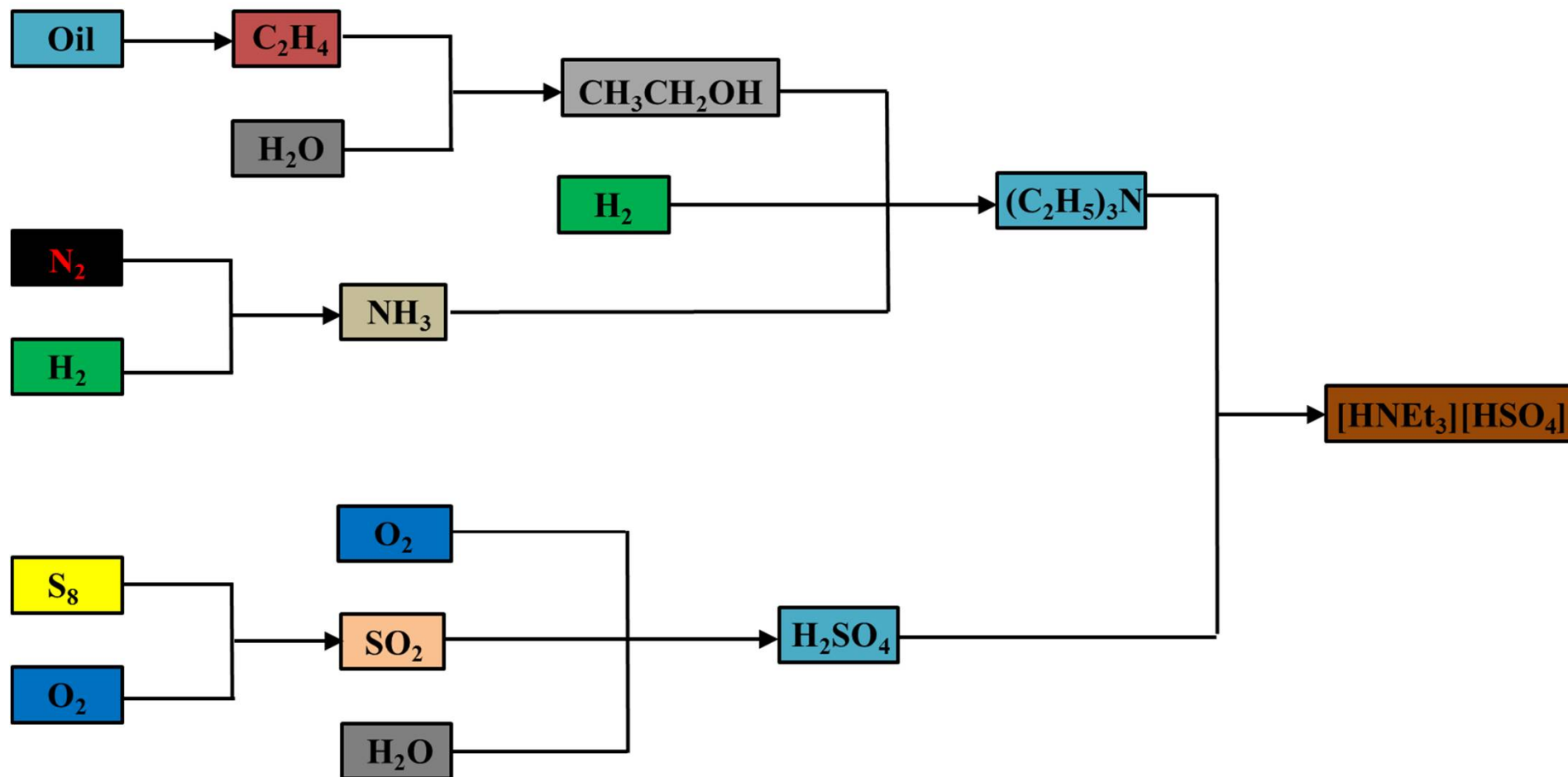


Waste in every step!

Cost = \$2500/kg; E-factor > 100

Jessop, *Green Chem.*, **13**, 1391 (2011)

How to make a Green solvent

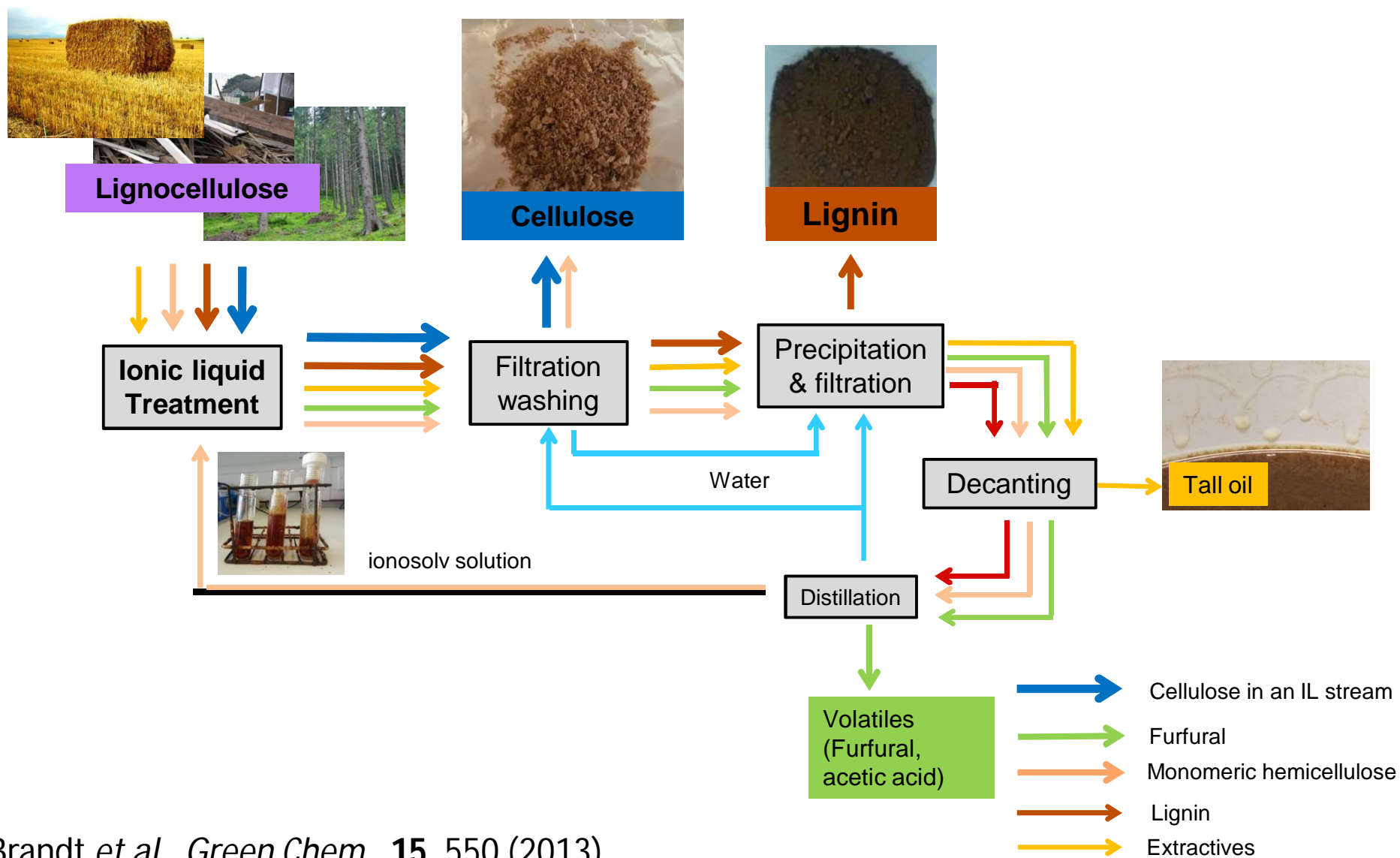


Cost = €1/kg; E-factor < 0.1

Fewer steps = lower cost = less waste

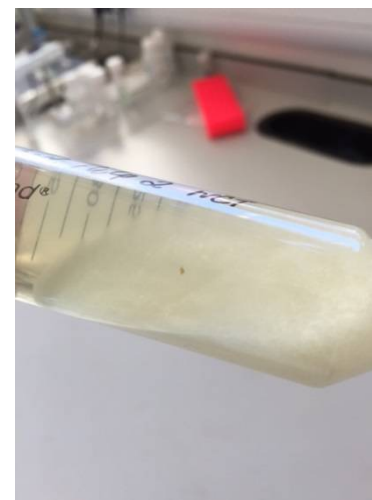
Chen *et al.*, *Green Chem.*, **16**, 3098 (2014)

Material flow diagram



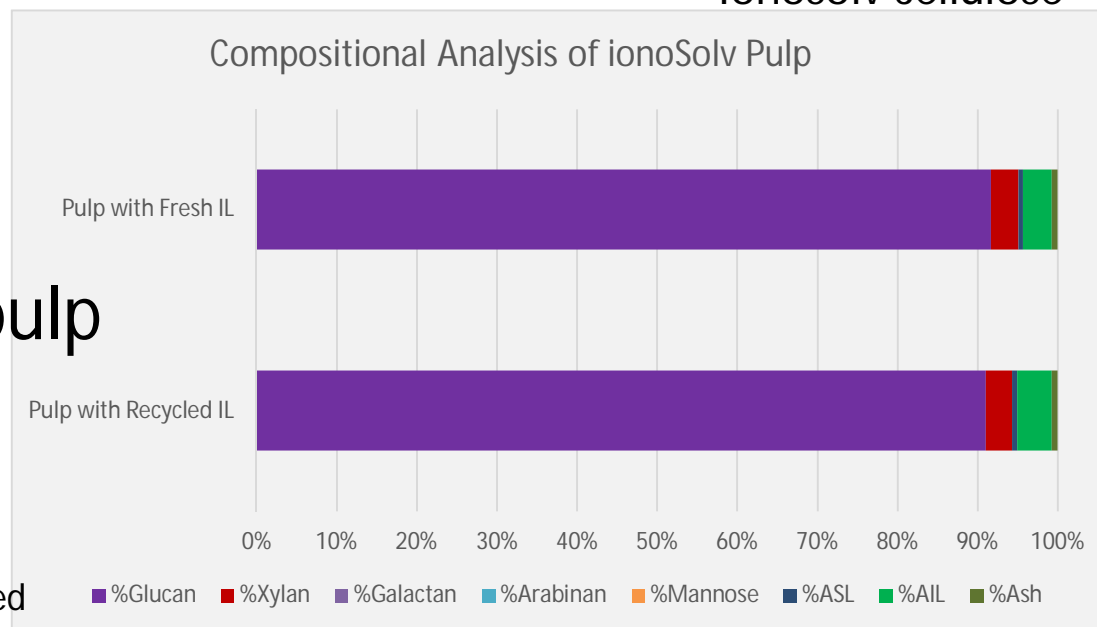


Fun facts about the cellulose



- We typically get ca. 96% glucan recovery (relative to native biomass)
 - 5% of the glucan is in the hemicellulose
- Max saccharification yields (rel. to native)
 - Miscanthus: 96%
 - Willow: 90%
 - Pine: 100%
- Most 'pure' cellulose pulp
ca. 94% glucan
 - 1 h, 150 C, 20% solids

Ionosolv cellulose



Results – Particle size



coarse

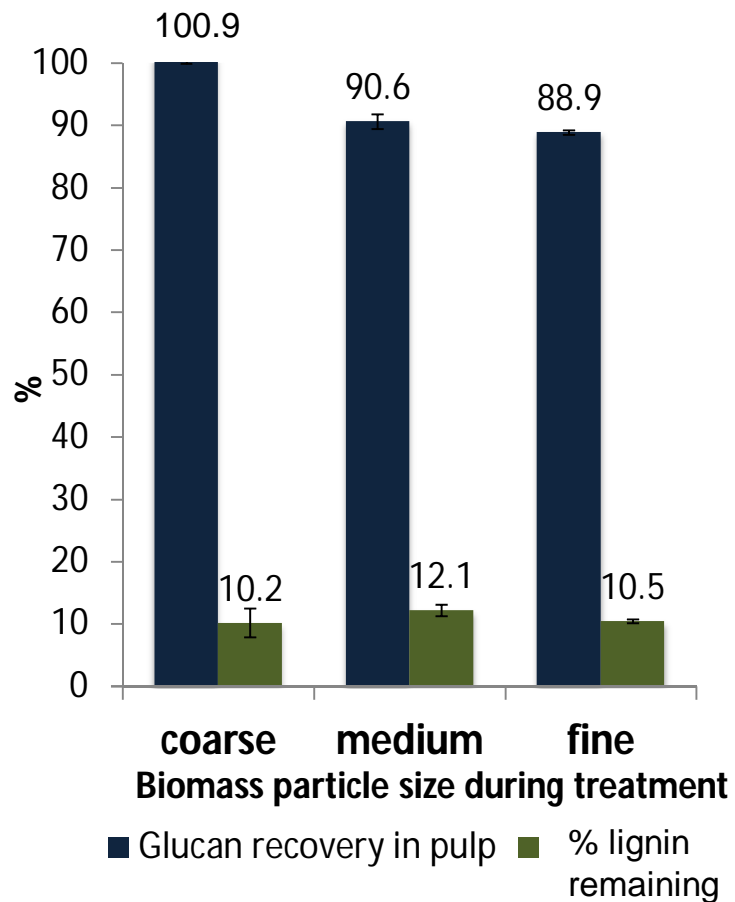


medium



fine





Results – Scale up

- Max sacch. yields at 20% **(50%)** solids
 - Miscanthus: 96% **(78%)**
 - Willow: 90% (??)
 - Pine: 100% **(82%)**

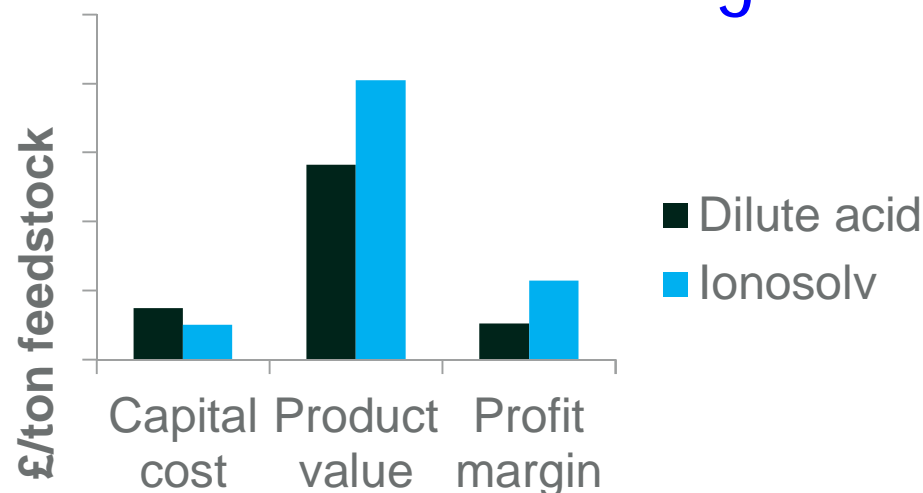


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Comparison of economics with other technologies

| Virgin wood/ton | |
|-----------------|-------------|
| Plant size | 100,000 tpa |
| Solvent | £11 |
| Biomass | £52 |
| Water | £ 4 |
| Capital | £25 |
| Energy | £51 |
| COST | £142 |
| Cellulose | £ 84 |
| Lignin | £ 88 |
| Hemicellulose | £ 36 |
| VALUE | £207 |
| NET | £ 65 |
| MARGIN | 46% |

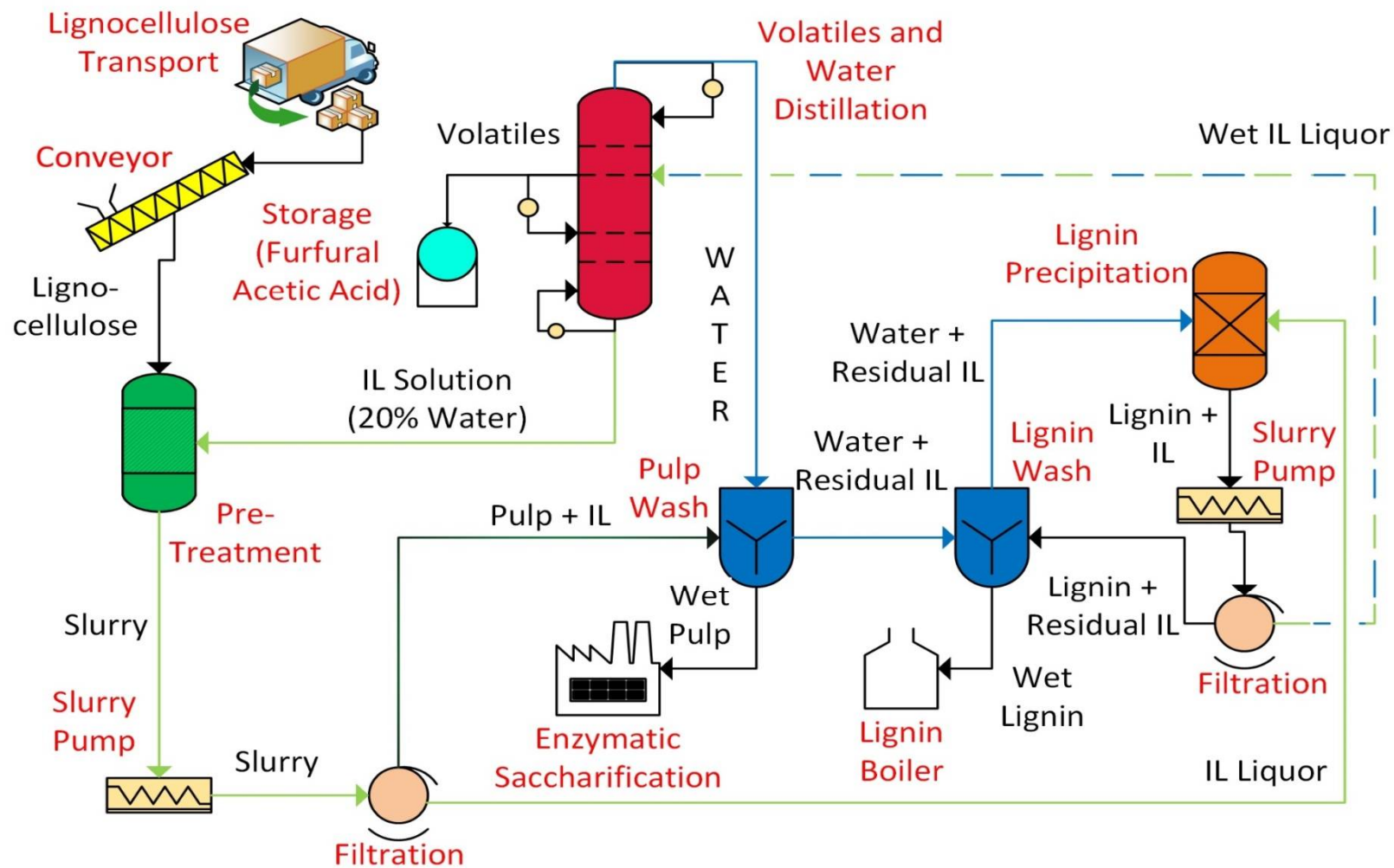
- Compared to (dilute acid pretreatment)
 - **30%** lower capital costs
 - **40%** higher product value
 - **100%** larger profit margin



Glucose can be sold at €0.16/kg
Also lower energy costs per ton of sugar than steam explosion

- **Higher solids loading possible**
 - (based here on 20%)
 - **100% sugar release from grasses or softwoods at 10% solids loading**
 - **80% sugar release from softwoods at 50% solids loading**
- **Less phase change = less cost**

Process Flow Scheme



IL recovery and recycling

- Very high IL stability (>330 C)
- 99.5 +/- 1% IL recovery
- ca. 100% lignin recovery
- No inorganic salt buildup



Fresh IL



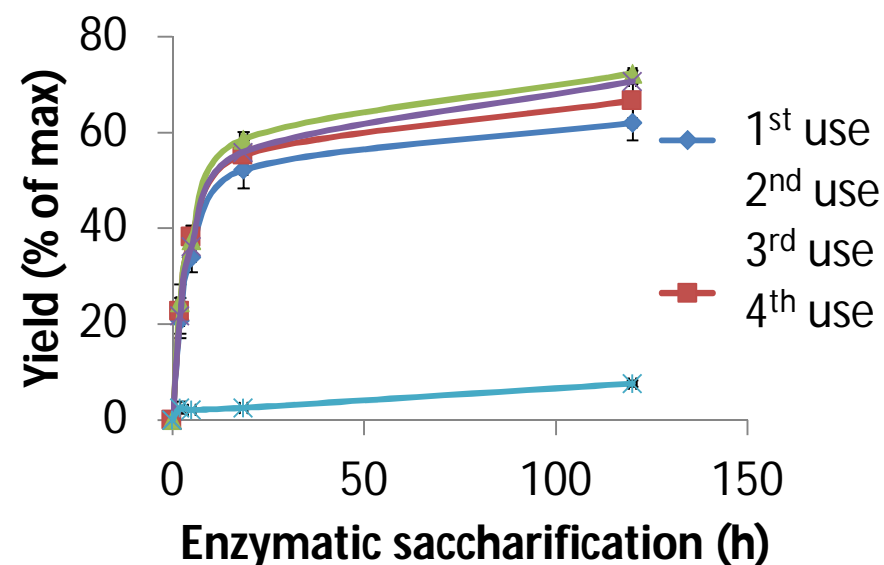
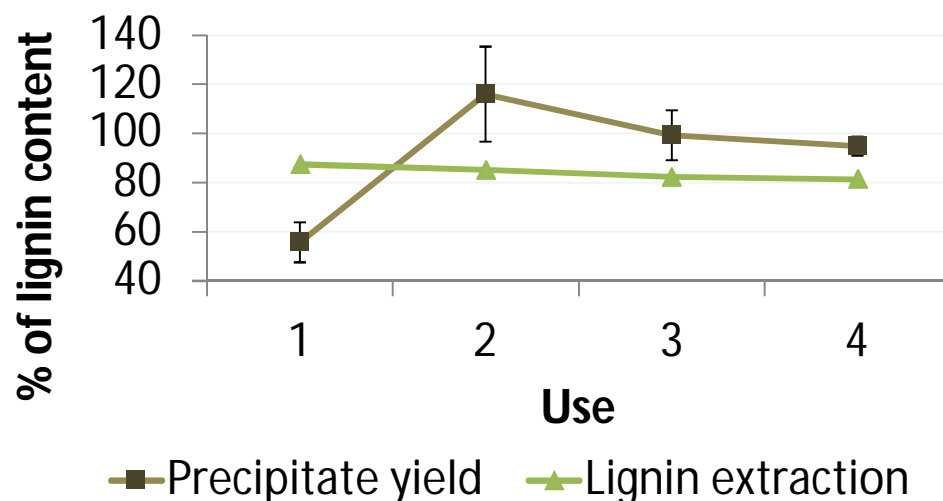
After 1st use



After 4th use

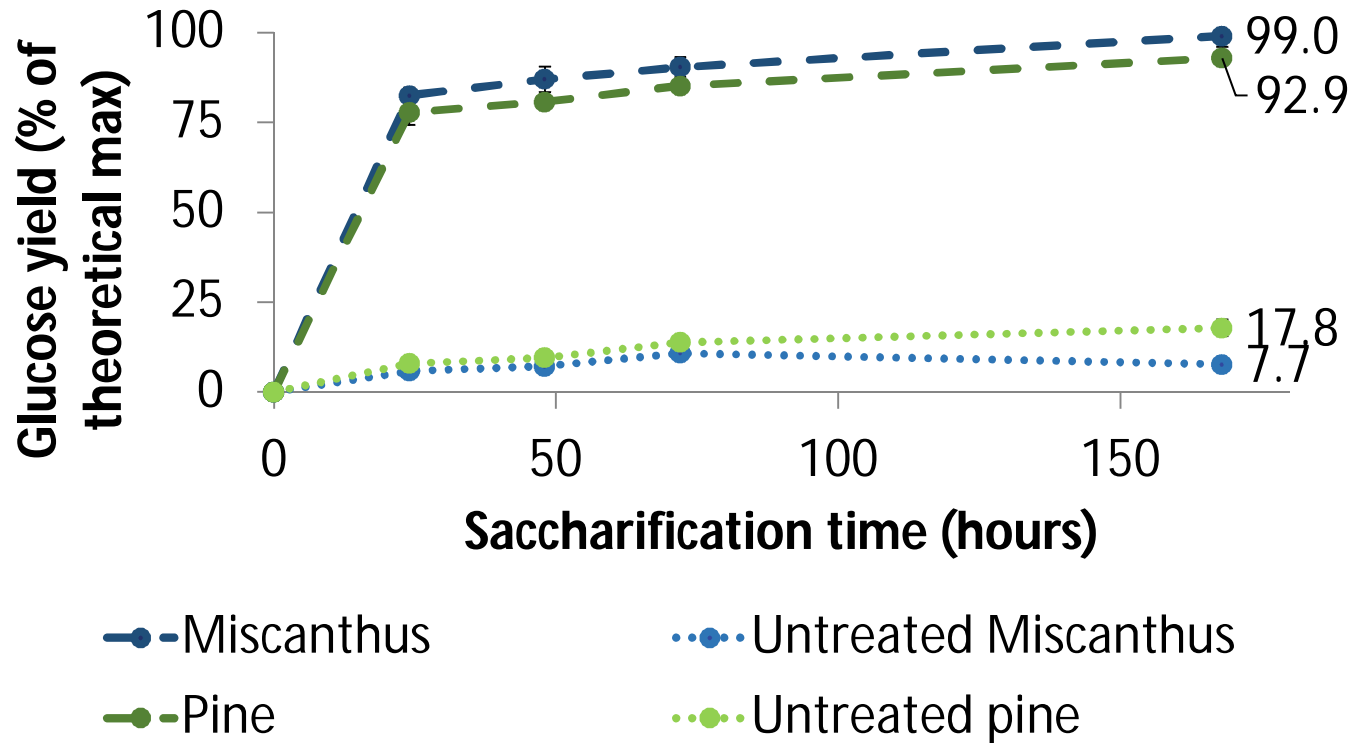
| | IL Recovery (%) | |
|---------------------|-----------------|-------|
| 1 st use | 99.0 | ±3.7 |
| 2 nd use | 97.9 | ±1.7 |
| 3 rd use | 99.4 | ±8.4* |
| 4 th use | 99.3 | ±0.9 |

* error due to mixing two replicates during pulp washing



Brandt *et al.*, *Green Chem.*, **19**, 3078 (2017)

Feedstock doesn't matter?



High Biomass loadings

Saccharification yield

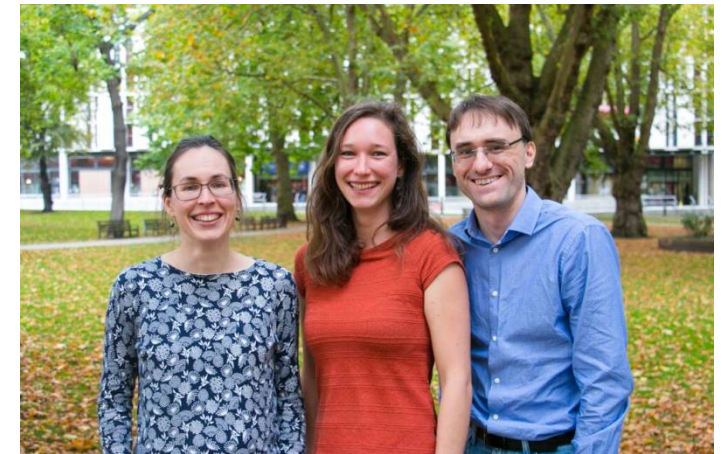
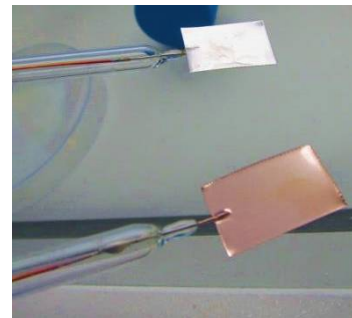
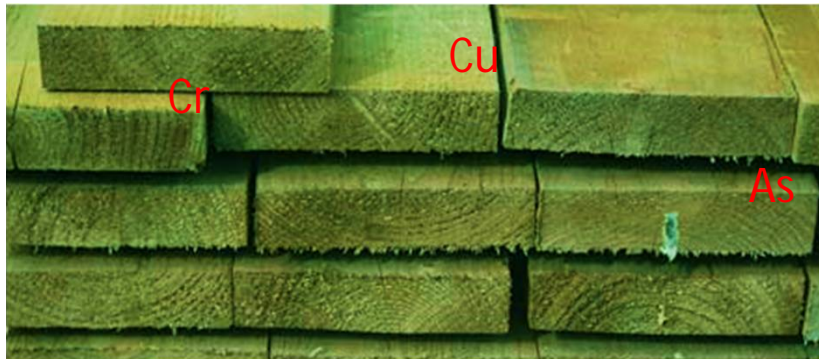
| Loading | with air drying | without air drying | |
|---------|-----------------|--------------------|---|
| 10% | 64.8±3.5% | 99.2±1.9% | ✓ Higher yields if pulp drying is avoided |
| 50% | 34.4±3.2% | 74.9±2.9% | ✓ Larger impact at high loadings |
| | | | ✓ Multiple feedstocks combined |

Metal-containing waste wood

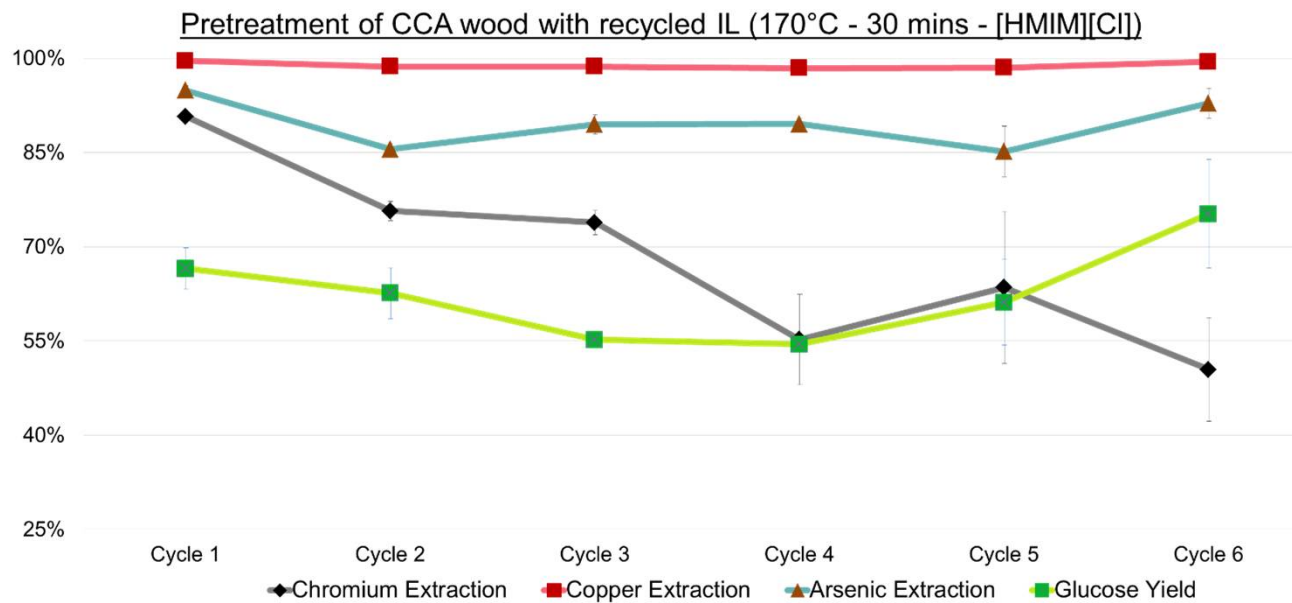


- ✓ Extraction of Cu, Cr and As
- ✓ Recovery of the metals through electro-plating
- ✓ High sugar yields

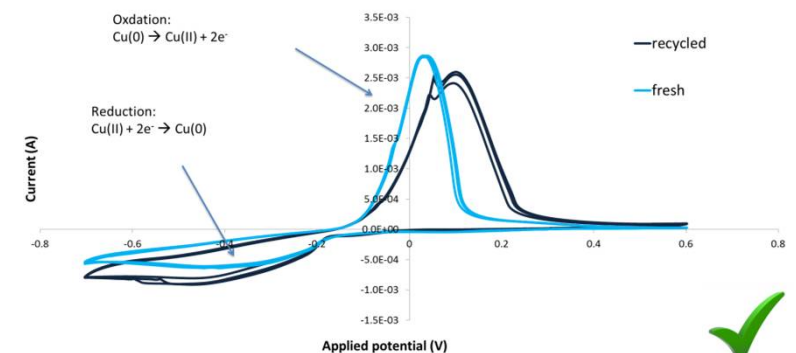
- ✓ 60 Mt/y US; 70 Mt/y EU
- ✓ Cannot be incinerated for biopower
- ✓ UK: £130/t for landfilling



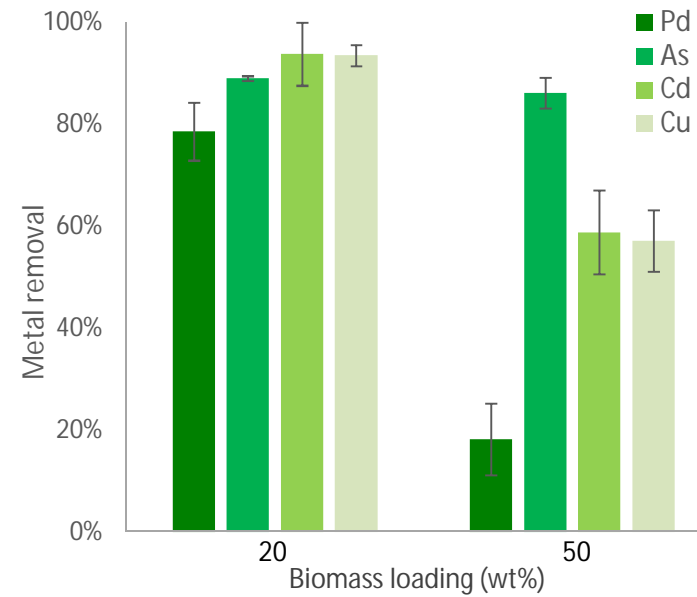
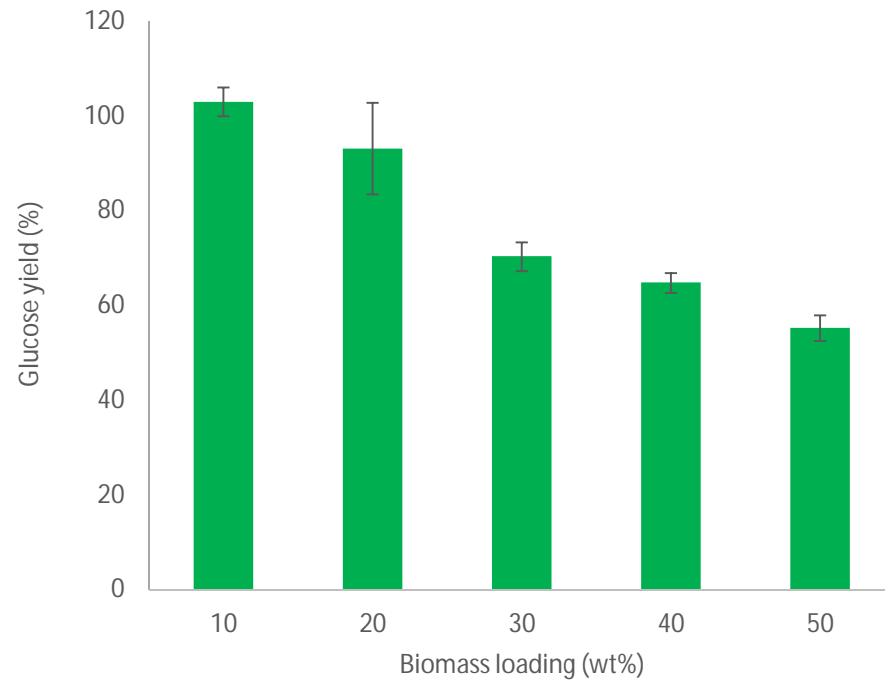
OK, So It Works



Cyclic Voltammetry of [HMIM][HSO₄] saturated with Cu ions and containing 20wt% water



Any Waste Wood?

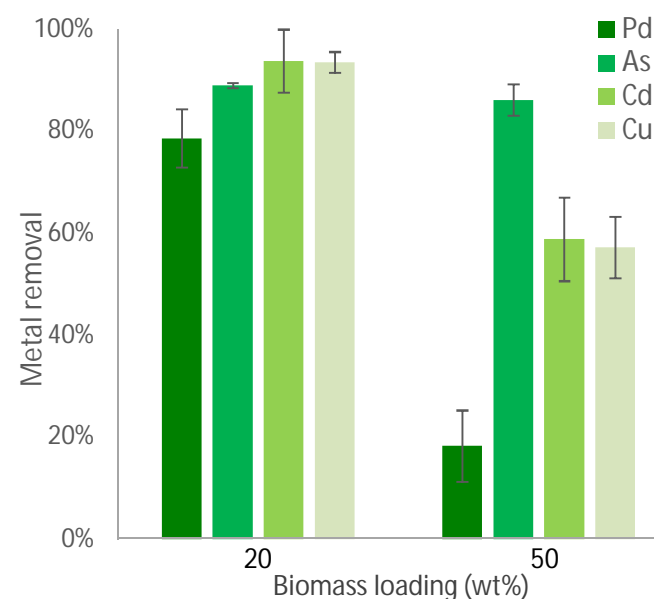
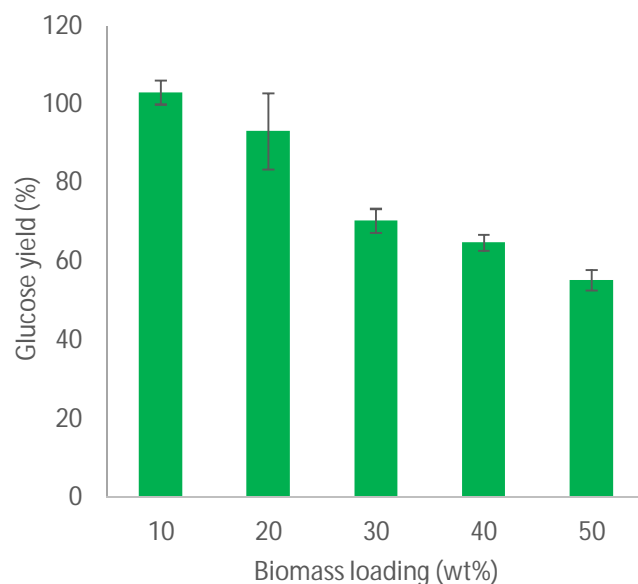
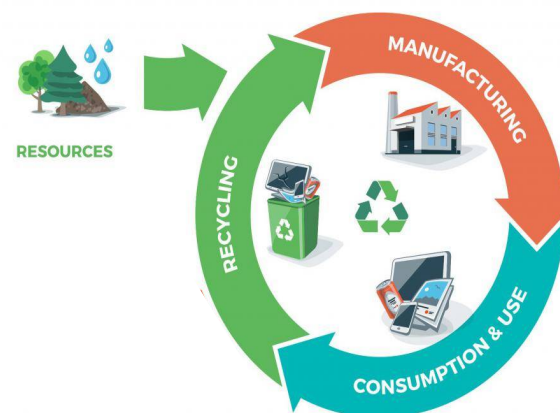


You don't get to choose what is in waste!

Waste wood to fuels & materials

Contributing to circular economy

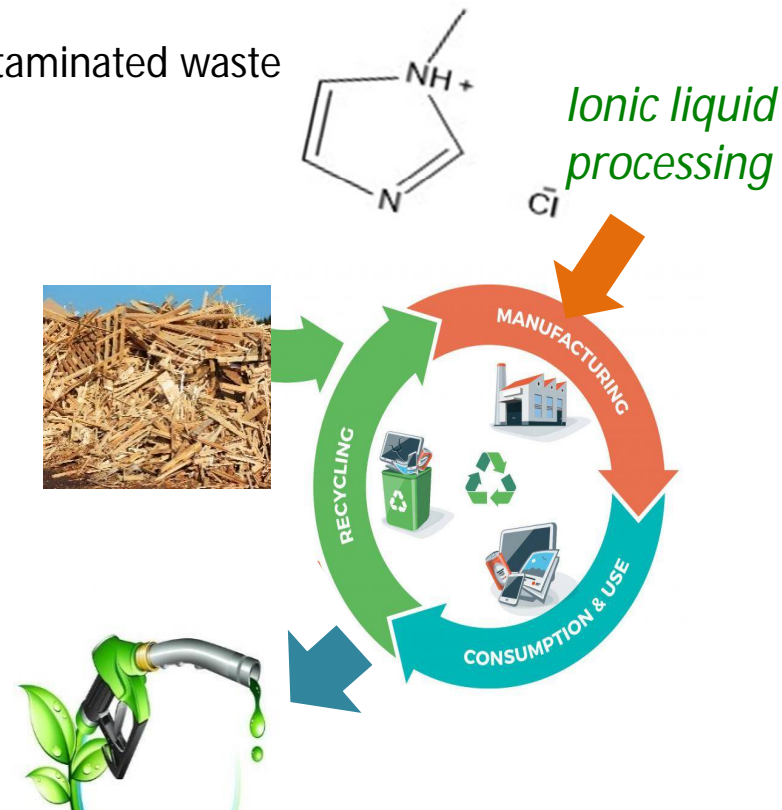
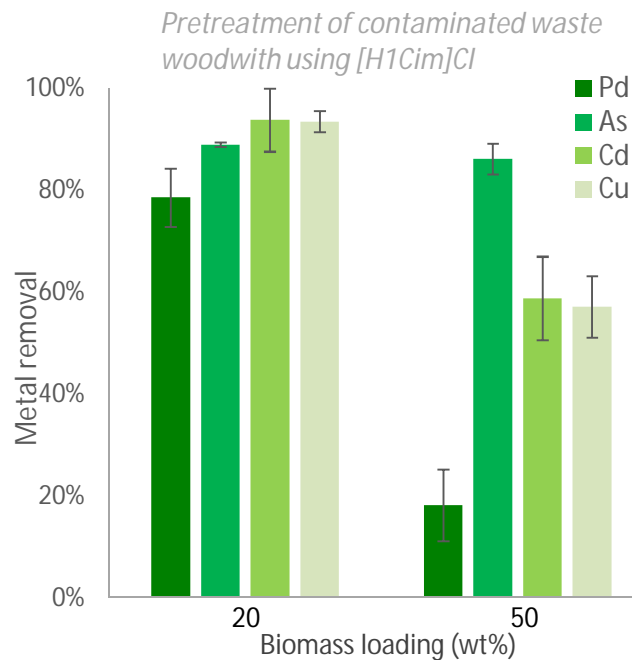
- Use post-consumer waste wood as very cheap (negative) feedstock for biorefinery
- Use low-cost ionic liquid process to:
 - *Save environment*: divert from landfill and remove heavy and toxic metals
 - *Make fuels & chemicals*: fractionate decontaminated waste wood to cellulose & lignin



Waste wood to fuels & materials

Contributing to circular economy

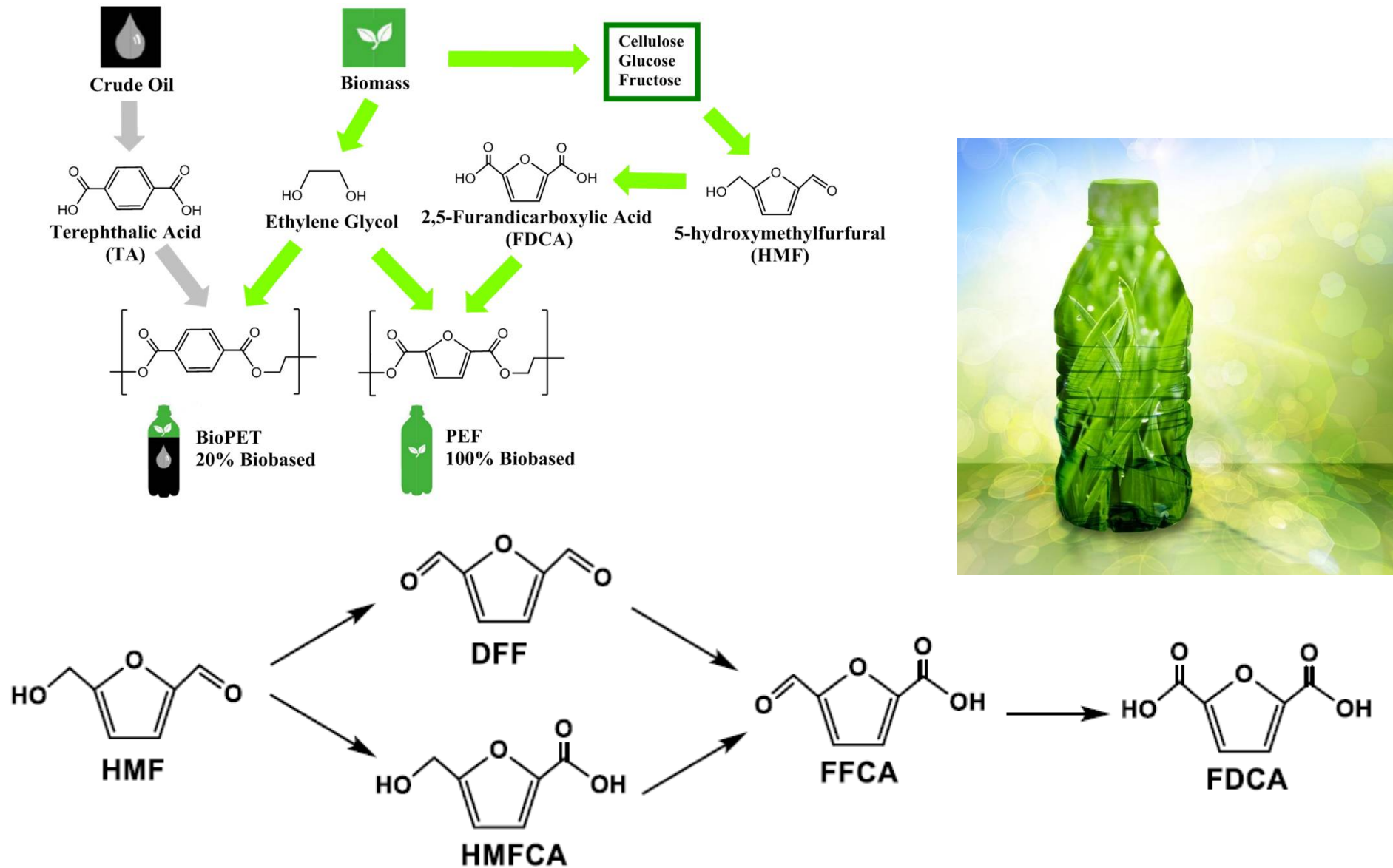
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Feedstock-controlled economics?

| | Waste wood/ton | Virgin wood/ton |
|---------------------|----------------|-----------------|
| Plant size | 20,000 tpa | 100,000 tpa |
| Cellulose | £ 90 | £ 90 |
| Lignin | £ 94 | £ 94 |
| Hemic/Furfural | £ 38 | £ 38 |
| Gate fee | £ 54 | - |
| REVENUE | £ 276 | £ 222 |
| Solvent | £ 11 | £ 11 |
| Biomass | - | £ 56 |
| Water | £ 4 | £ 4 |
| Capital | £ 43 | £ 26 |
| Energy | £ 55 | £ 55 |
| COST | £ 113 | £ 152 |
| PROFIT | £ 163 | £ 70 |
| GROSS MARGIN | 59% | 32% |

Onward to bioderived plastics!



Conclusions

- Ionic liquids do not have to be expensive
 - Targeted applications still possible
 - Use common sense when designing
- Delignification of biomass
 - Simple process
 - Stable, recoverable, recyclable solvents
 - High solids loadings possible
- Recycling improves performance
- Economics-driven approach to solvent design
 - Can be application specific

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