### THE FUEL AND ENERGY RESEARCH FORUM

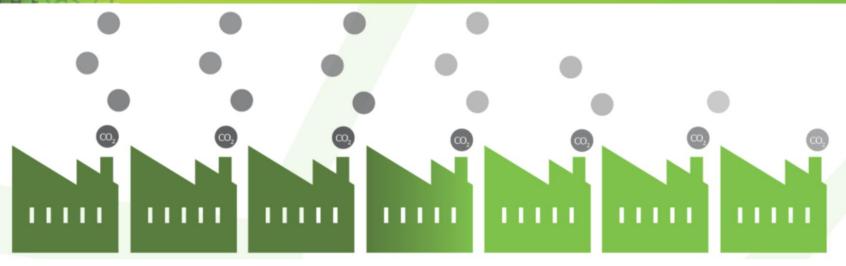
Wednesday 11<sup>th</sup> April 2018 – University of Sheffield



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NanoMaterials Enhanced Membranes for Carbon Capture



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## **CONTENTS**



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The NanoMEMC<sup>2</sup> project is funded by the European Commission through the European Union's Horizon 2020 Research and Innovation programme



## NanoMEMC<sup>2</sup> INTRODUCTION



- Nano-material enhanced membranes for carbon capture
- Membrane separation can be applied to CO<sub>2</sub> capture processes:
  - pre-combustion (CO<sub>2</sub>-H<sub>2</sub>/CO<sub>2</sub>-CH<sub>4</sub> separation)
  - post-combustion (CO<sub>2</sub>-N<sub>2</sub>)
  - o oxyfuel-combustion (O<sub>2</sub>-N<sub>2</sub>)
- Membrane separation can be applied to a range of carbon-intensive industry sectors
- Compared to other capture methods, membrane-based separation can potentially be highly flexibility, with lower operating costs
- Current materials lack the separation performance and durability needed for an efficient and economically feasible exploitation of such technology



## NanoMEMC<sup>2</sup> INTRODUCTION



- The NanoMEMC<sup>2</sup> research aims to overcome current limitations by focusing on the development of innovative CO<sub>2</sub> selective membranes with high flux and selectivity, suitable for application to both pre and post-combustion capture processes
- Various materials will be manufactured and functionalized:
  - nanofibrillated cellulose (NFC)
  - graphene (G)
  - graphene oxide (GO)
- These will be used to form two different types of membranes:
  - novel facilitated transport hybrid membrane (FTHM)
  - o continuous phase hybrid membrane (CPHM)



# **BACKGROUND, AIM & GOAL**

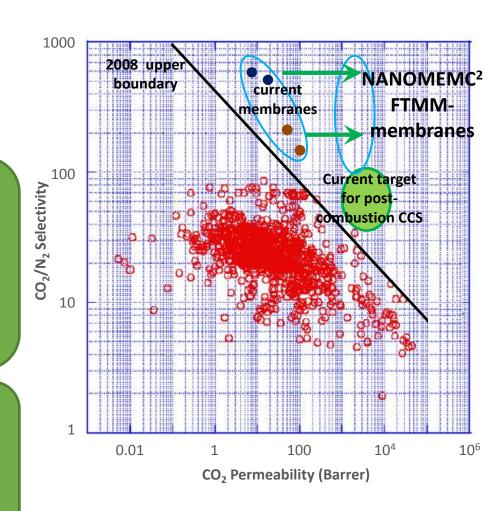


#### **MEMBRANES:**

selectivity vs. permeability capture ratio vs. gas purity energy costs vs. membrane area

AIM: to contribute to the real, effective deployment of CCS technologies by reducing the cost and energy penalty of CO<sub>2</sub> capture through the development and optimal integration of innovative membranes within different energy-intensive processes

GOAL: to fully develop the potential of membranes in the selective capture of CO<sub>2</sub>, increasing the efficiency of the capture and reducing the overall CCS cost below the value of €40/t of CO<sub>2</sub> avoided





### **PROJECT PARTNERS**



Project Coordinator: Dr Marco Giacinti Baschetti Alma Mater Studiorum - Università di Bologna



















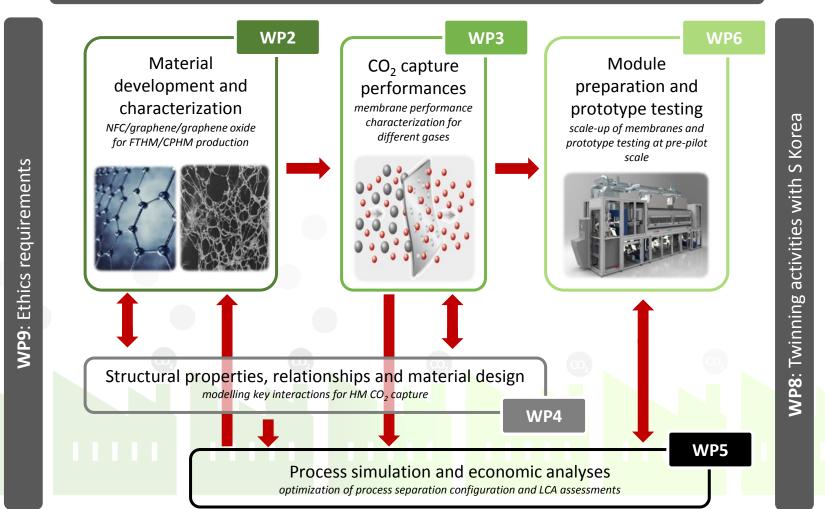




### **WORK PROGRAMME**







**WP7**: Dissemination and exploitation of results



### MEMBRANE SCENARIOS



### **POWER PRODUCTION: natural gas**

- conventional NGCC (BAU)
- NGCC + post-combustion capture
- raw-hydrogen-fuelled CCGT + precombustion capture

# <u>POWER</u> PRODUCTION: coal integrated gasification combined cycle

- IGCC with acid removal using Selexol (BAU)
- IGCC with acid removal and precombustion CCS

# INDUSTRY: hydrogen production by steam methane reforming (SMR)

- conventional SMR plant (BAU)
- SMR plant with post-combustion carbon capture
- SMR plant with pre-combustion carbon capture from syngas
  (burners: NG- + H<sub>2</sub>-fired)

### **INDUSTRY**: cement production

- conventional dry kiln cement plant (BAU)
- dry kiln cement plant with postcombustion capture



### RESULTS SO FAR . . . .

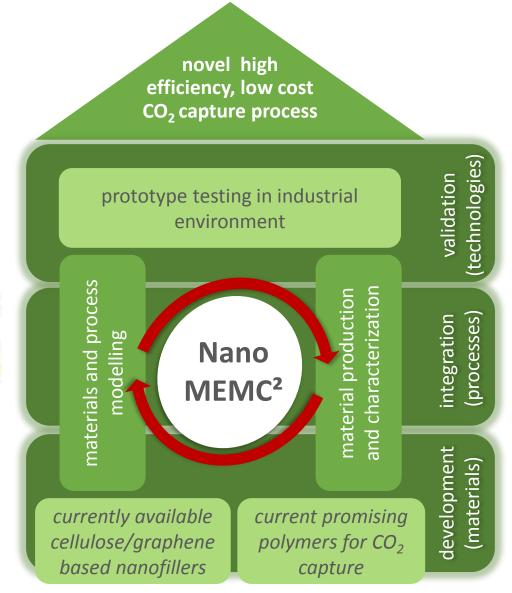


The research has focused on WP2, 3, 4 and 5



Raw Material Acquisition





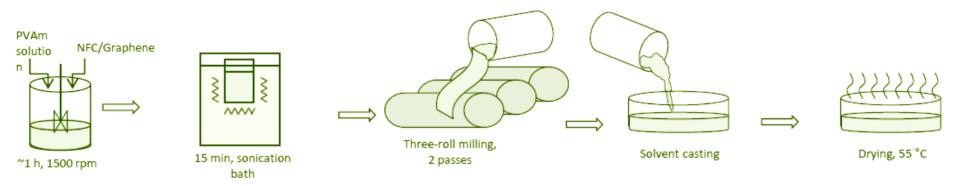
& Assembly



### RESULTS SO FAR . . . . .



- PVA-based membranes:
  - fillers: G and NFC
  - polymer: polyvinylamine (CO<sub>2</sub> selective polymer) at different degrees of purification
  - casting: solution casting in water
  - thickness: 60 μm
  - test conditions: 35 °C, 1 bar upstream, single humid gas
- Characterisation and testing for permeability and selectivity for over
  50 first generation membranes using NFC, G and GO

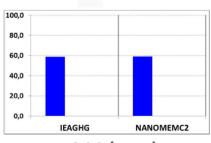


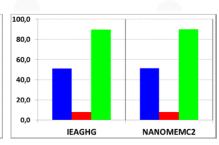


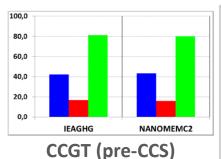
### RESULTS SO FAR . . . .



- Molecular modelling facilitated transport membranes
  - analyse/quantify interactions between CO<sub>2</sub> and membrane materials and develop structure-property associations
  - predictive tools for inside modules as a function of conditions
- Process design, optimisation and assessment scenario analysis and development for baseline and membrane integrated models





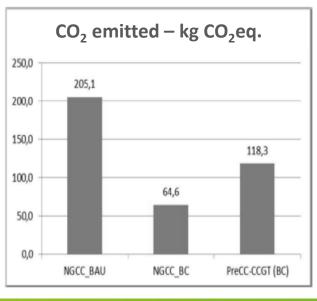




- solvent = n/a
- $\eta_{1HV} = 59.1\%$
- EP = 0.0 % points
- CPR = 0.0%
- overall efficiency (%)

### NGCC BC (post-CCS)

- solvent = MEA-based
- $\eta_{\text{LHV}} = 51.2\%$
- EP = 7.9 %points
- CPR = 90.0%
- solvent = Selexol
- $\eta_{LHV} = 43.3\%$
- EP = 15.9 %points
- CPR = 80.2%
- energy penalty (%pt) capture rate (%)

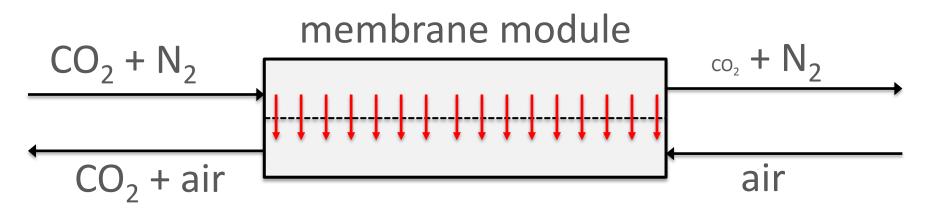




## **MEMBRANE TESTING AT PACT**



comprehensive baseline tests with  $CO_2$ - $N_2$  for benchmarking over the whole range of operational regimes



#### Measurements for:

- compositions
- flowrates
- temperatures
- pressures



## **PACT AT SHEFFIELD**



# PACT







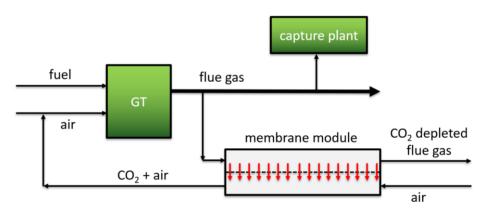




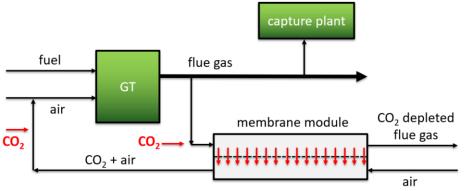
## **MEMBRANE TESTING AT PACT**



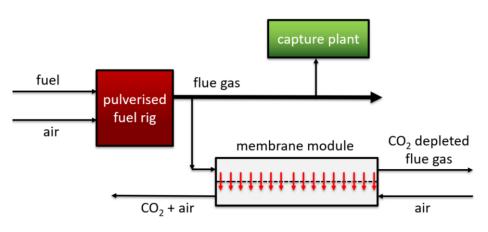
#### membrane integration with gas turbine



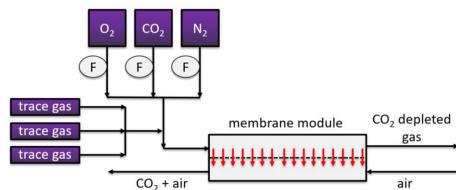
### membrane with GT and CO<sub>2</sub> injection



#### membrane with coal/biomass fuels



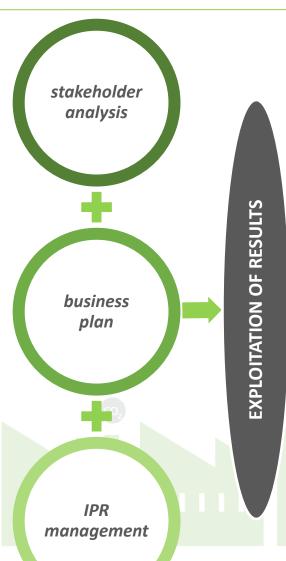
# membrane integration synthetic gas skid (industrial separation)





### **CONCLUDING REMARKS**





### **VALUE CHAIN**

#### **SUPPLIER**

materials produces,  $CO_2$  suppliers



### PROCESS DEVELOPER

industrial/engineering consultants, EPC engineering procurement, construction



#### **END USERS**

power, steel/cement plants, oil refineries, manufacturing industry



#### **INFLUENCERS**

policy makers, local communities, association, etc.

The NanoMEMC<sup>2</sup> project is now generating significant exploitable results, used for dissemination activities and extensive stakeholder engagement throughout the value chain



## **CONCLUDING REMARKS**



Sign up for our newsletter on the NanoMEMC<sup>2</sup> website:

www.nanomemc2.eu





# THE FUEL AND ENERGY RESEARCH FORUM

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Thank you to all of the NanoMEMC<sup>2</sup> project partners for their inputs to this presentation