Analytical Solutions for Microwave Drying of Coal Fuel and its Applications



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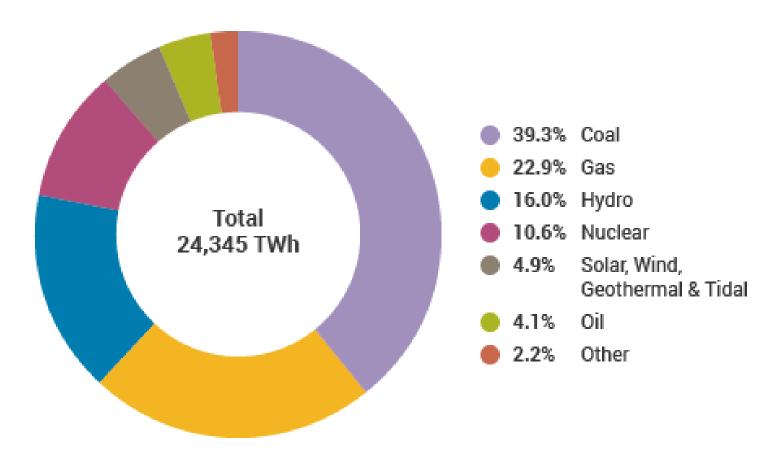


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- Advantages and disadvantages of using coal fuel.
- Microwave treatment of coal.
- Modeling of the coal heating process.
- Modeling of coal drying.
- Conclusions.

World electricity generation by source



Source: IEA Electricity Information 2017

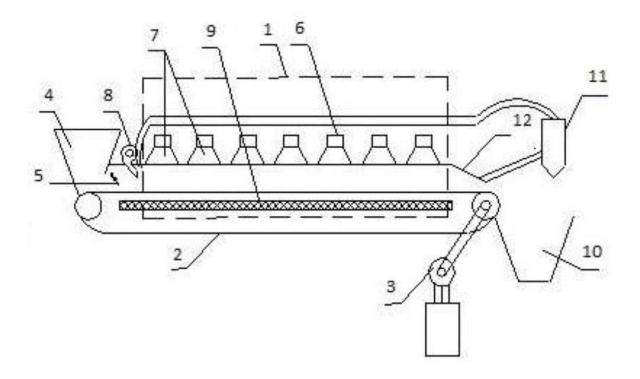
Advantages and disadvantages of using coal fuel.



- 1) Environmental Factor: Abundant emissions of gaseous (CO2, NOx, SOx) and solid (ash) wastes
- 2) Energy factor: the efficiency of coal use is comparable, but still somewhat lower than primary energy resources.
- 1) Gas reserves are enough for \sim 60 years, oil \sim 40 years, and coal for \sim 500 years.
- 2) The prices for a coal resource are lower in comparison with analogues

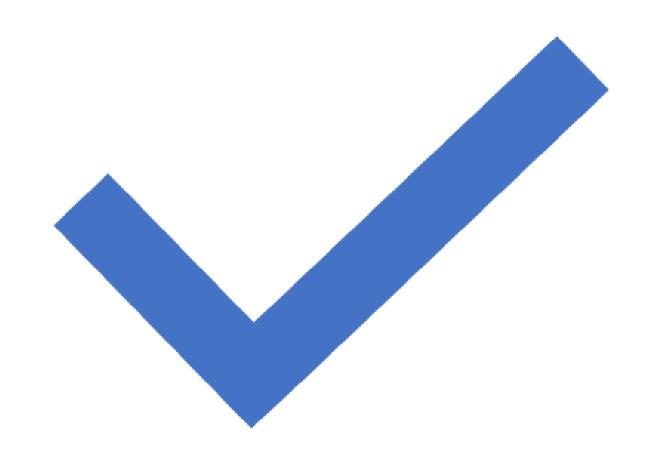
Typical setup for microwave treatment for coal

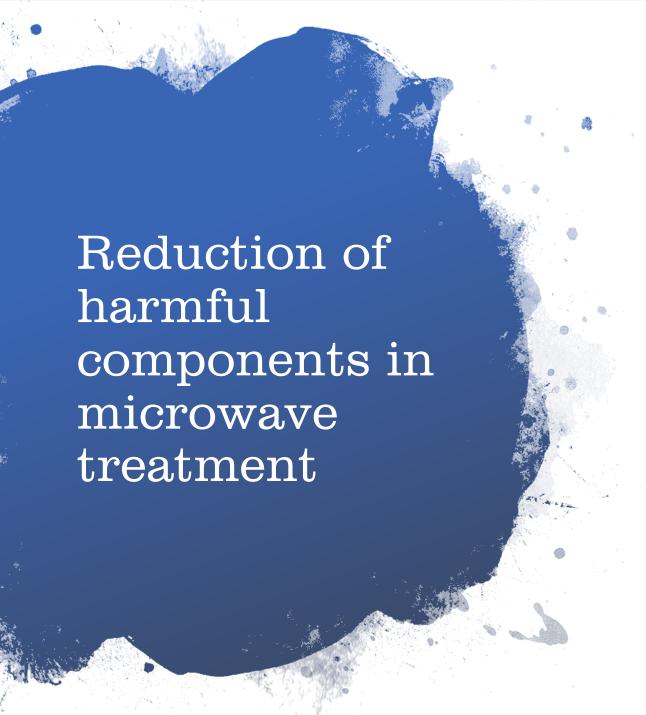
- 1 working chamber
- 2 conveyor
- 3 adjustable electric drive
- 4 loading device
- 5 adjustable slide gate
- 6 magnetrons
- 7 horn antennas
- 8 fan
- 9 absorbing material
- 10 discharge device
- 11 dust collecting device
- 12 protective waveguide.



Benefits of using microwave treatment for coal

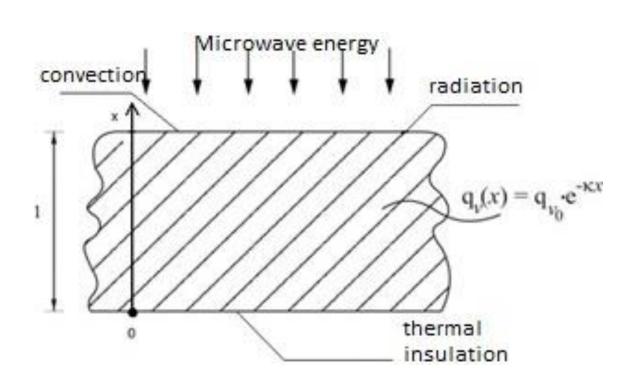
- Significant reduction in processing time
- Removal of harmful component
- Non-inertial process
- Volumetric impact





- Complete removal of nitrogen
- Reducing the sulfur content by 50%
- Mercury by 50%
- Ash content is 30%
- Chlorine by 50%

Modeling of the coal heating process



$$\frac{\partial T(x,t)}{\partial t} = a \frac{\partial^2 T(x,t)}{\partial x^2} + \frac{q_{v_0}}{c\rho} e^{-kx}, \qquad (1)$$

$$0 \le t \le t_{\mathfrak{s}}, \ 0 \le x \le l,$$

$$T(x,0) = T_0, (2)$$

$$-\lambda \frac{\partial T(l,t)}{\partial x} = \sigma \left[T^4(l,t) - T_c^4 \right] + \alpha \left[T(l,t) - T_c \right]$$
(3)

$$\frac{\partial T(0,t)}{\partial x} = 0. (4)$$

Solution scheme

A system with a nonlinear boundary condition

Transition to dimensionless variables

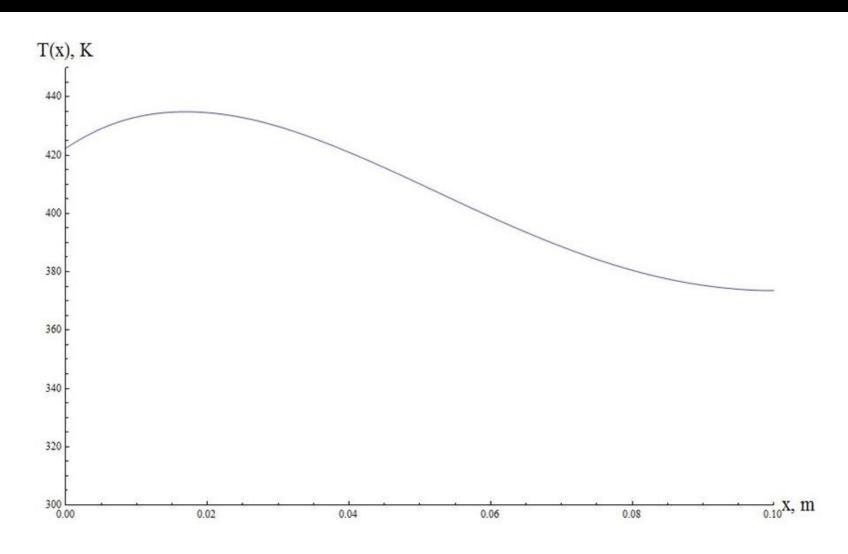
Integral Laplace transform, solution search in images:

$$\theta_L(X,s) = Ki_L(s)F_1(X,s) + Po_L(s)F_2(X,s)$$

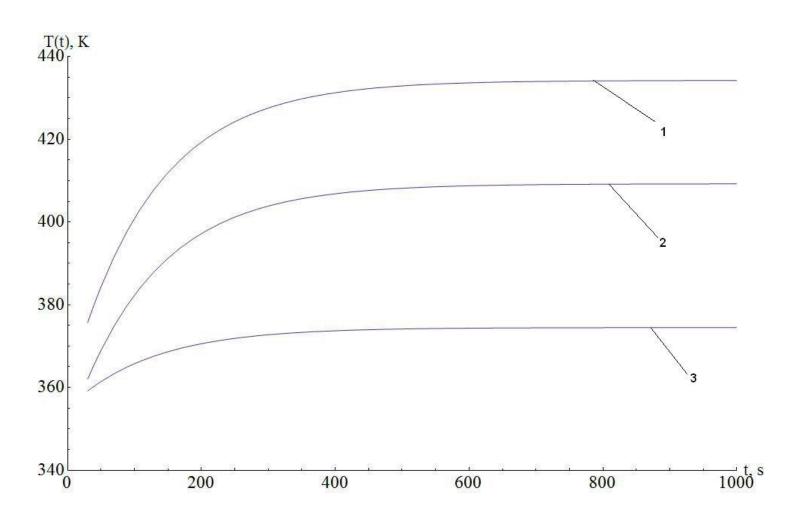
$$F_1(X,s) = -\frac{ch(\sqrt{s}X)}{\sqrt{s} \cdot sh(\sqrt{s})} \qquad F_2(X,s) = \frac{e^{-BuX}}{s(s - Bu^2)}$$

Search for asymptotic solutions for large and small time parameters

Depth distribution of temperature

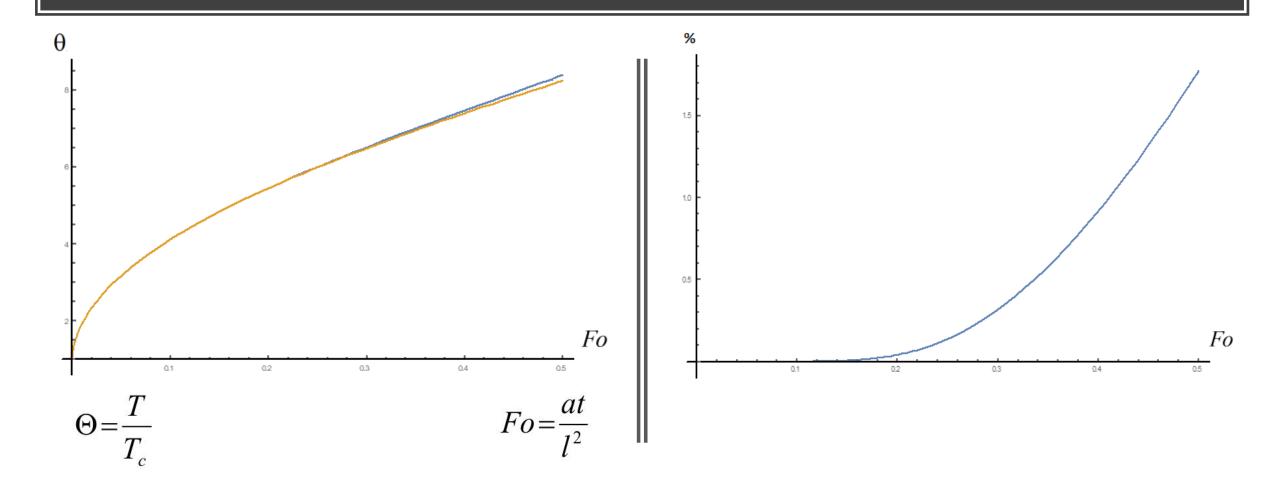


Temperature distribution over time

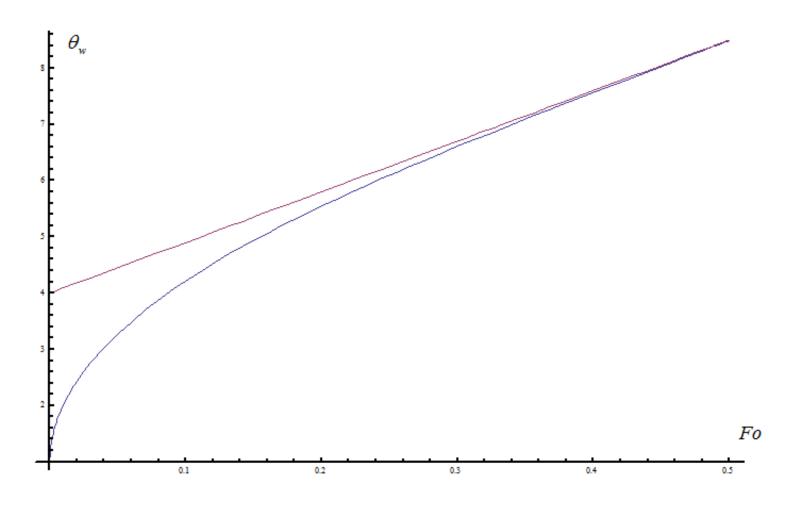


- 1 maximum temperature in the layer
- 2 temperature in the center
- 3 temperature on the surface

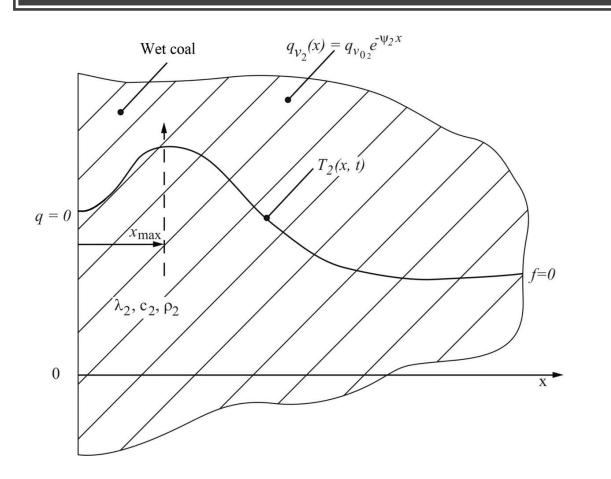
Comparison of asymptotic solution with exact one for simple problem [A. V. Lykov] for small time parameters Fo

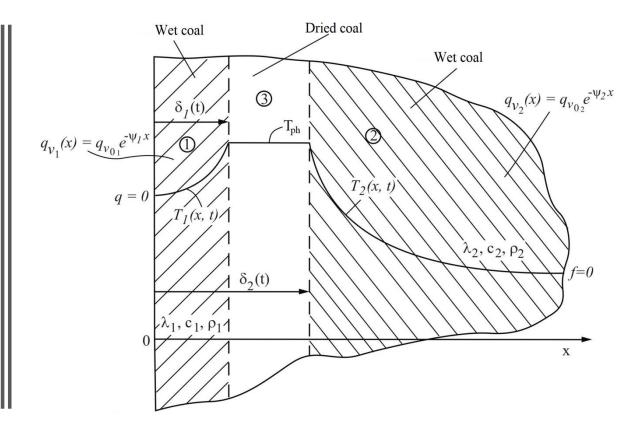


Comparison of asymptotic solution with exact one for simple problem [A. V. Lykov] for big time parameters Fo



Modeling of coal drying.





Equations for different drying zones of coal

$$\frac{\partial T_1(x,t)}{\partial t} = a_1 \frac{\partial^2 T_1(x,t)}{\partial x^2} + \frac{q_{\nu_0}}{c_1 \rho_1} e^{-\psi_1 x}$$

$$t > 0 \quad 0 < x < \delta_1$$

$$\frac{\partial T_1(0,t)}{\partial x} = 0$$

$$-\lambda_{1} \frac{\partial T_{1}(\delta_{1},t)}{\partial x} = \rho_{1} H_{H} \frac{d\delta_{1}}{dt}$$

$$T_1(x, 0) = \varphi_1(x)$$

$$T_1(\delta_1, t) = T_{\phi}$$

$$\frac{\partial T_2(x,t)}{\partial t} = a_2 \frac{\partial^2 T_2(x,t)}{\partial x^2} + \frac{q_{\nu_o}}{c_2 \rho_2} e^{-\psi_2 x}$$

$$t > 0 \qquad x > \delta_2$$

$$\frac{\partial T_2(\gamma_2, t)}{\partial x} = 0$$

$$-\lambda_2 \frac{\partial T_2(\delta_2, t)}{\partial x} = \rho_2 H_u \frac{d\delta_2}{dt}$$

$$T_2(x, 0) = \varphi_2(x)$$

$$T_2(\delta_2, t) = T_{\phi}$$

The motion law of phase front for zone 1

$$t \cong D^{-1} \left[\frac{1}{2G} \ln \left| E - \delta_1 F + \delta_1^2 G \right| + \frac{F}{G} \frac{1}{\sqrt{4EG - F^2}} \operatorname{arctg} \frac{2G\delta_1 - F}{\sqrt{4EG - F^2}} \right]_{x_{\max}}^{\delta_1}$$

$$D = \frac{3\lambda_{1}}{\rho_{1}H_{1}}; \quad E = \frac{q_{\nu_{01}}}{\lambda_{1}T_{\phi}\psi_{1}^{2}} + \frac{H_{1}x_{\text{max}}}{c_{1}}; \quad G = \frac{q_{\nu_{01}}}{2\lambda_{1}T_{\phi}\psi_{1}^{2}}; \quad F = \frac{q_{\nu_{01}}}{\lambda_{1}T_{\phi}\psi_{1}^{2}} + \frac{H_{1}}{c_{1}}.$$

$$\delta_{1}(t) = 2\varepsilon\sqrt{a_{1}t},$$

$$\varepsilon = \sqrt{\frac{3m(m+2)}{m^2 + 9m + 12}} \quad m = \frac{c_1(T_{\phi} - T_{w})}{L_{\phi}}$$

$$W_{e}(t) = \rho_{e} \left(\delta_{\max} - \delta_{1}(t) \right) + \rho_{e} \left(\delta_{2}(t) - \delta_{\max} \right) =$$

$$= \rho_{e} \left(\frac{1}{4P} \left(C_{L1} - C_{L2} \cdot t + 4M^{2} \cdot t^{2} \right) - 2\varepsilon \sqrt{a_{1}t} \right) \quad V = W_{e}'(t) = \rho_{e} \left(\frac{1}{4P} \left(C_{L2} + 4M^{2} \cdot t \right) - \frac{2\varepsilon a_{1}}{2\sqrt{a_{1}t}} \right)$$

Conclusions

- The task of microwave heating of wet coal was posed and solved analytically. Comparison with exact solutions showed high accuracy.
- On the basis of the solution for the heat-up stage, the problem of finding the microwave drying front for wet coal was posed and solved analytically. Comparisons were made with exact solutions.
- Expressions for the determination of moisture loss, calculation of time and drying rate are found.



Thank you!

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