CFD predictions of aerodynamics and mixing in ultra-low NOx lean combustion grid plate flame stabilizer

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Introduction

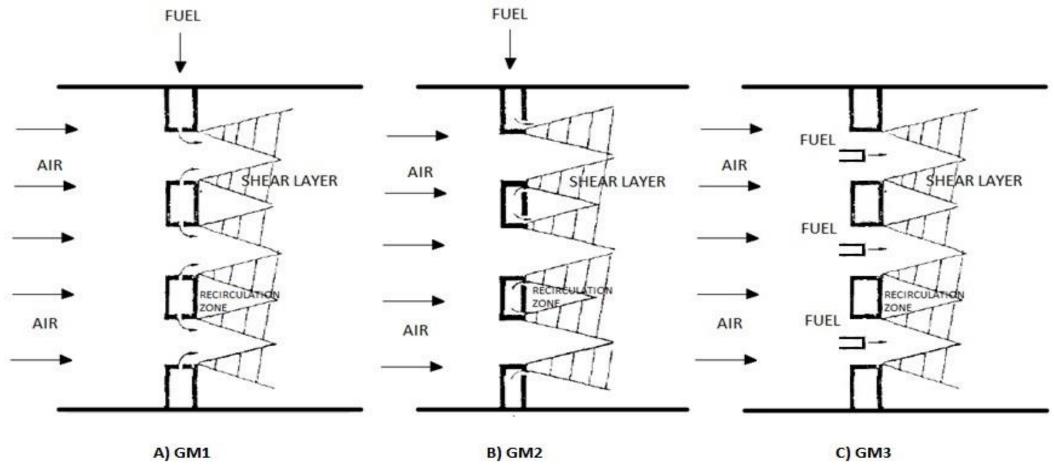
Nitrogen Oxides NOx (NO + NO₂)

NOx emissions from boilers are required to be reduced to ultra-low NOx levels, in many areas of the World including Europe and the USA.

The EU Ecodesign regulations for small residential gas boilers, require NOx to be less than 56 mg_{NOx}/kWh from 26th Sept 2018. For natural gas (NG) with a CV of 50 MJ/kg this is 13.9 g_{NOx}/GJ and an emission index of 0.78 g_{NOX}/kg_{fuel} and this converts to 27ppm NO_x at 0% oxygen. In the USA some areas of California have NOx reglulations at <5ppm at 0% oxygen.

For gas turbines for power generation NOx regulations <25 ppm at 15% oxygen have been in existence for many years, but currently requirements are <10ppm in many areas of the World and in California <2.5 ppm (<8.8 ppm at 0% oxygen).

The rapid mixed grid mix design investigated in this work has been shown capable of meeting these ultra-low NOx requirements.



Grid mix jet shear layer fuel injection: GM1- 8 radial inward equally spaced fuel jets from the wall of the jet; GM2 - annular fuel injection slot around each shear layer jet hole. (Andrews, G.E. and S.A.R. Ahmed, 2008) GM3 new fuel injection considering a fuel insert in the centreline (FLOX burners)

GE hydrogen combustor

GM1

GM1

Funke, H. H-W. et al. U. Aachen and Krebs, W. and Wolf, E. Siemens Energy Experimental characterization of low NOx micromix prototype combustors

for industrial gas turbine applications. ASME GT2011-45305, 2011.

Low NOx for hydrogen containing fuels.

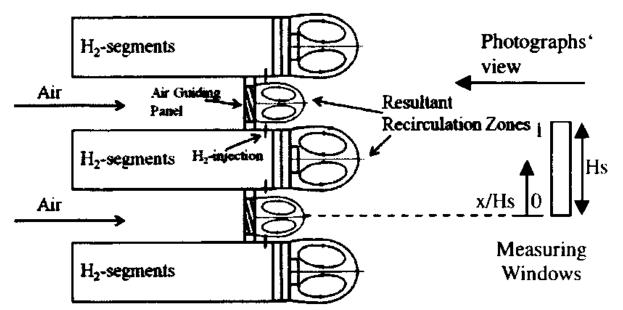
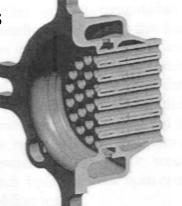


Figure 2: Resultant Recirculation zones

ASME GT2012-69913 York, et a., GE Energy and GE Global Research

Development and testing of a low NOx Hydrogen Combustion System for HDGT



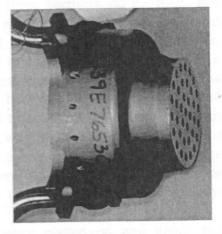
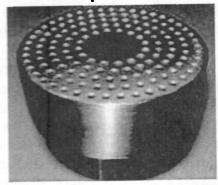


Figure 2. Model cross-section and photograph of small multi-tube mixer for high-hydrogen fuel.

20.3 bar 650K 63.5mm dia Combustor Grid plate stabiliser



MT mixer

Figure 3. Larger scale multi-tube mixer used for single nozzle rig flame operability testing.

HITACHI GM3 Multicluster combustor

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ASME Paper GT2007-27737, Hitachi

FLOX technology GM3

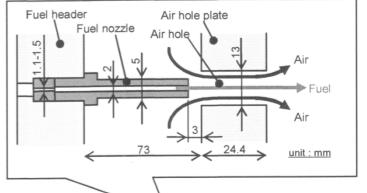
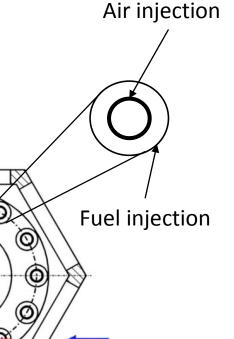
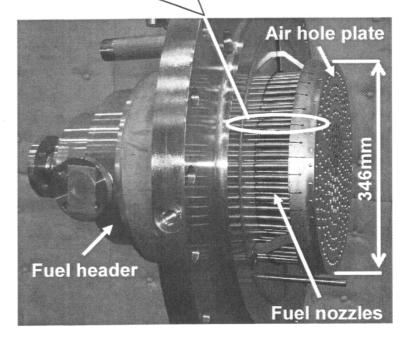


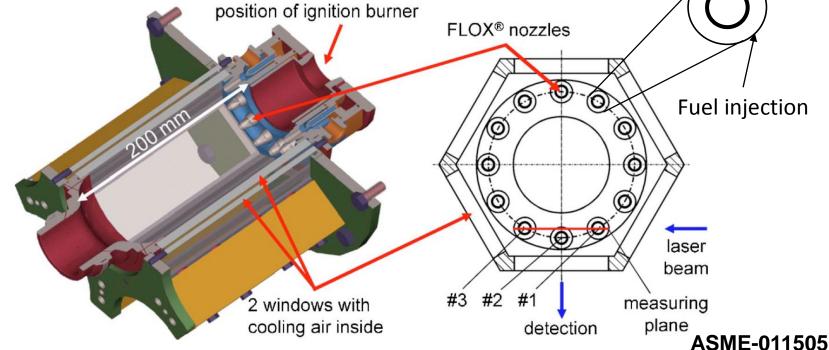


Fig. 2 Cluster Nozzle Burner

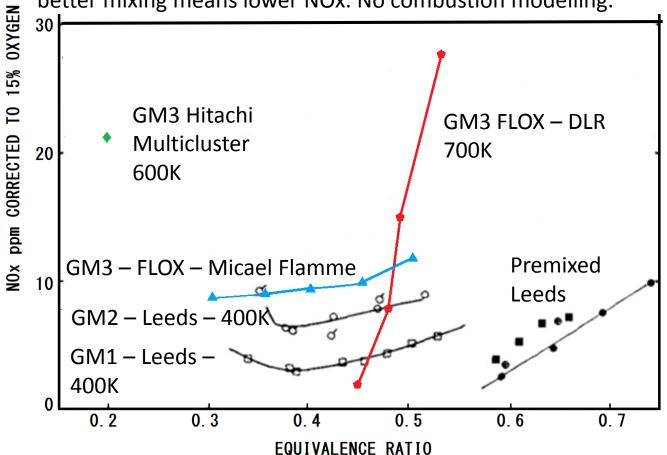
Fuel staged cluster nozzle burner of Hitachi in a 3MW GT.







Comparison of experimental measurements in the literature for the impact of the method of fuelling a grid plate flame stabiliser. Comparison with fully premixed combustion. This CFD investigation models the mixing of fuel and air, as better mixing means lower NOx. No combustion modelling.

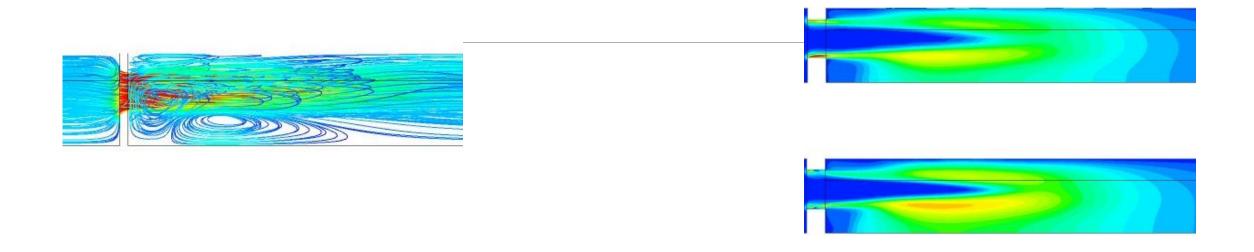


NOx corrected to 15% oxygen as a function of equivalence ratio at 400K (Al-Dabbagh, N.A., G.E. Andrews, and R. Manorharan, 1984 6th ISABE Paris

FLOX BURNER data points
"New combustion systems for gas
turbines (NGT)"
Michael Flamme (2004)

DLR data points (ASME GT2007-27337)

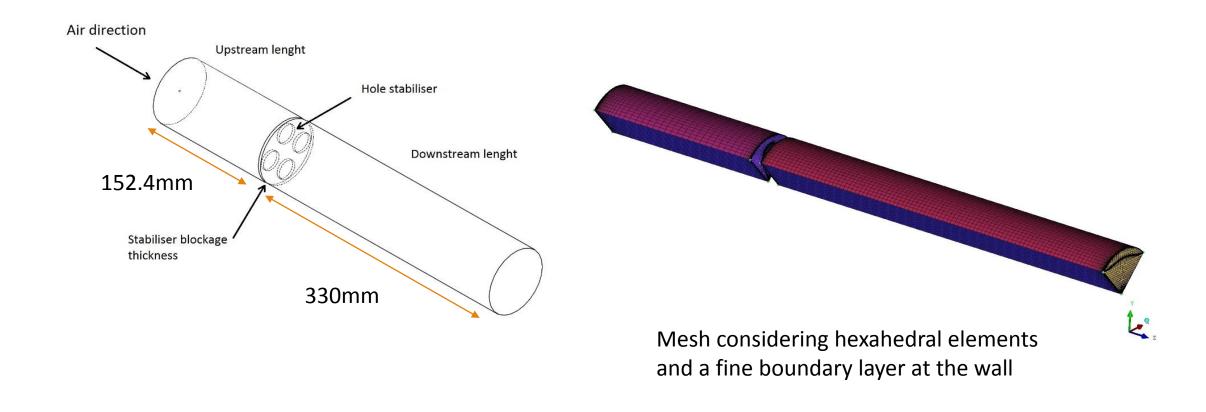
HITACHI Multicluster burner data points (ASME GT2007-27737)



Computational Fluid Dynamics

ANSYS CFX version 17.2

Software and computational methods

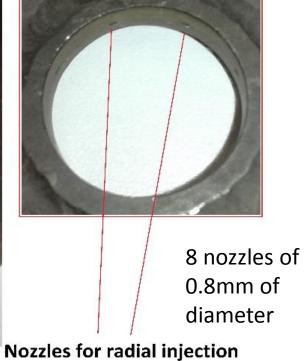


Aerodynamics

Boundary Conditions	Value
Mach number	0.047
Combustion Intensity	20 MW/m ² per bar
Air inlet temperature	400°K
Air inlet mass flow rate	0.0786 kg/s
Air inlet velocity	18.84 m/s
Fuel Inlet temperature (mixing)	288K
Fuel inlet mass flow rate (mixing)	0.0006298 kg/s
Reference Pressure	1 ATM
Outlet pressure (19.27 & 19.62mm	122.58 Pa
geometries)	
Outlet pressure (22.44mm geometry)	61.29 Pa
Convergence Criteria	RMS: 1 X 10 ⁻⁶

Mixing





0.3mm for annular gap

Annular feed

Equations

$$\dot{m} = C_D A_2 (2\rho \Delta P)^{0.5} \longrightarrow C_D = \frac{1}{K^{0.5}} * \frac{1}{\beta}$$
 (1)

$$1/C_C = 1/C_D + \beta \tag{2}$$

$$K = \frac{\Delta P}{0.5 \, \rho_{air} U_{air}^2} \tag{3}$$

Ward Smith formulae
$$K = \left[\frac{1}{0.608\beta(1 - \beta^{2.6}) \left(1 + \left(\frac{t}{d} \right)^{3.5} \right) + \beta^{3.6}} - 1 \right]^{2}$$
 (4)

Jose Hamon Quintile 27 Hee, 211 7 Ham 201 Ham 21 Ha									
			Modelling		Experiment		Ward Smith formulae		
Turbulent model	Mesh	Number	CD	CC	CD	CC	CD	CC	
	Quality	of nodes							
KE									
	Finer	5,974,098	0.741	0.632	0.747	0.628	0.738	0.621	
	Fine	2,189,768	0.768	0.653	0.747	0.628	0.738	0.621	
	Medium	834,828	0.78	0.663	0.747	0.628	0.738	0.621	
	Coarse	254,410	0.78	0.665	0.747	0.628	0.738	0.621	
SST									
	Finer	5,974,098	0.731	0.621	0.747	0.628	0.738	0.621	
	Fine	2,189,768	0.748	0.634	0.747	0.628	0.738	0.621	
	Medium	834,828	0.765	0.65	0.747	0.628	0.738	0.621	
	Coarse	254,410	0.761	0.646	0.747	0.628	0.738	0.621	

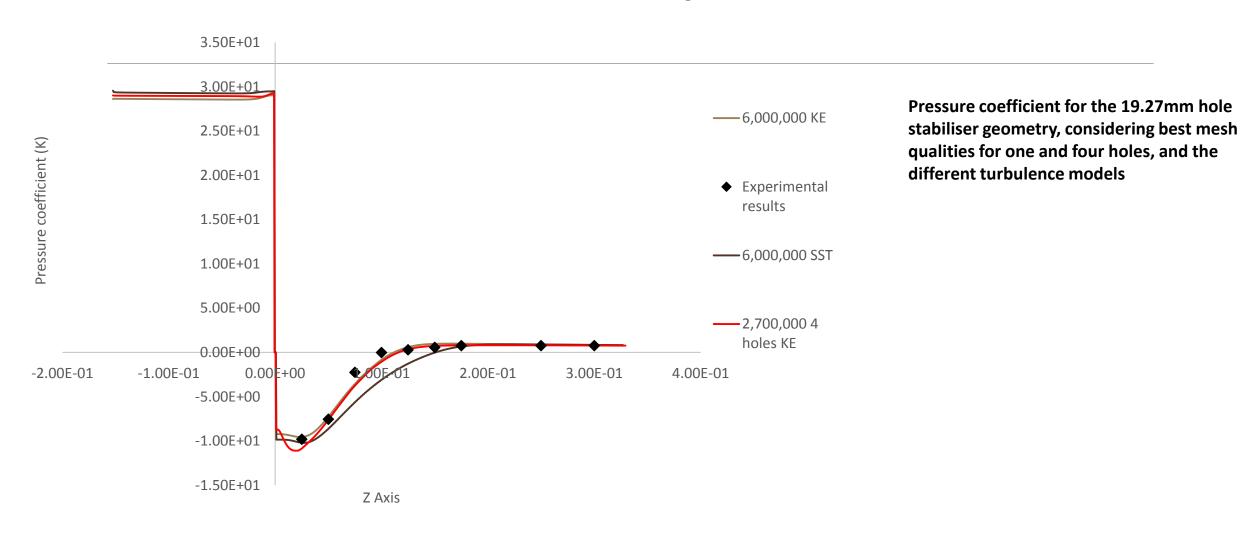
Results for aerodynamics

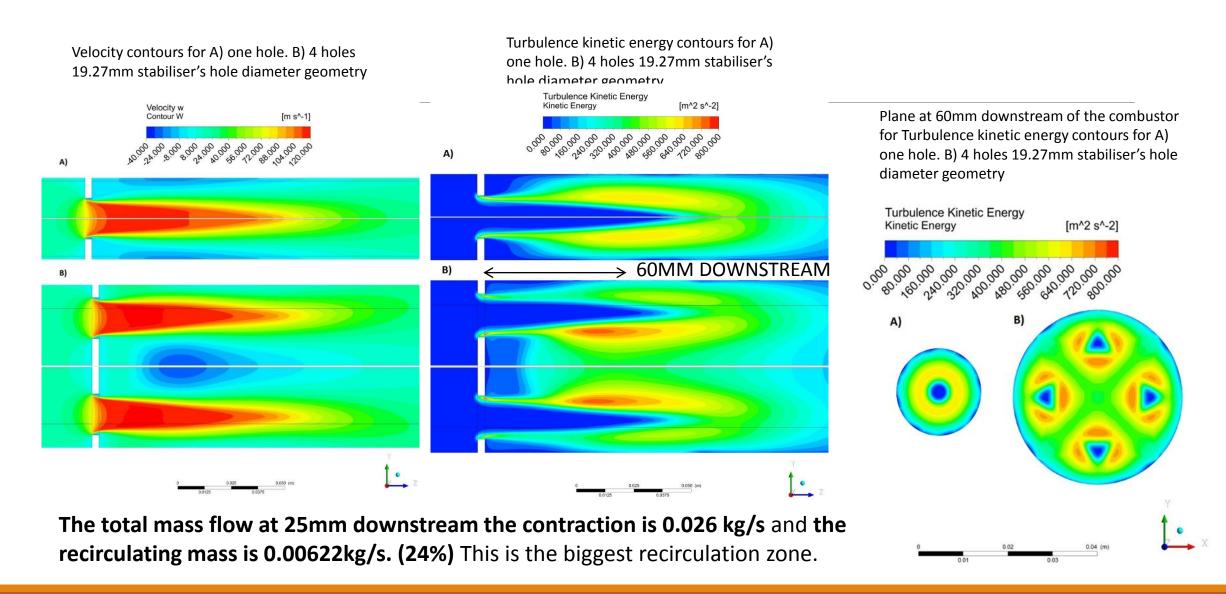
Mesh independence study for the one hole 19.27mm hole stabiliser diameter geometry

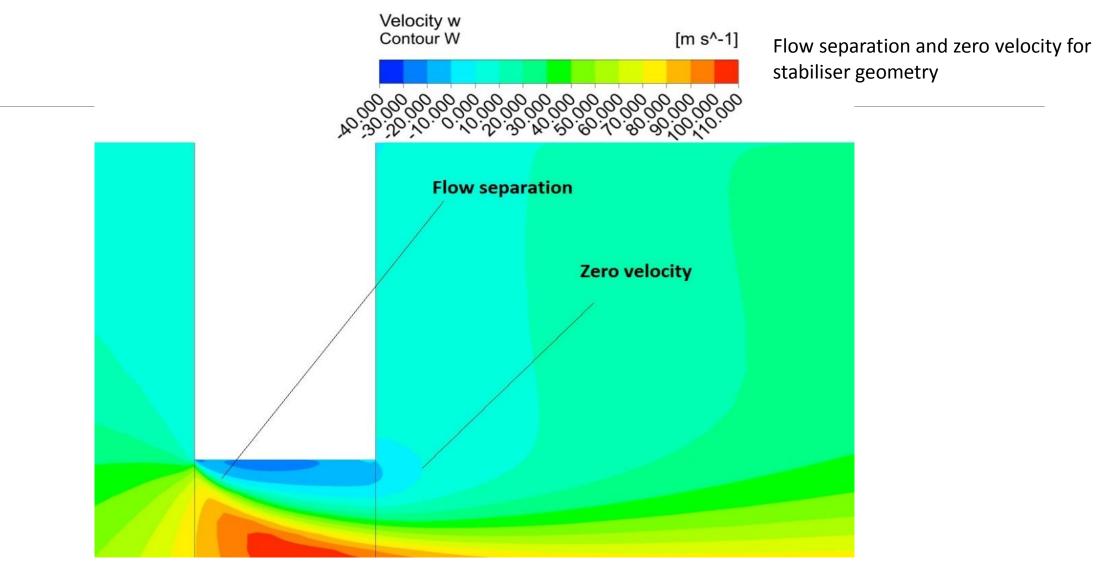
			Modelling		Experiment		Ward Smith formulae	
Turbulent model	Mesh Quality	Number of nodes	CD	CC	CD	CC	CD	CC
KE								
	Medium	2,700,000	0.735	0.616	0.747	0.628	0.738	0.621
	Coarse	1,300,000	0.748	0.629	0.747	0.628	0.738	0.621

Mesh statistics for a fourhole 19.27mm hole diameter stabilizer geometry

Pressure coefficient for 19.27mm stabiliser hole diameter 3.2mm blockage thickness





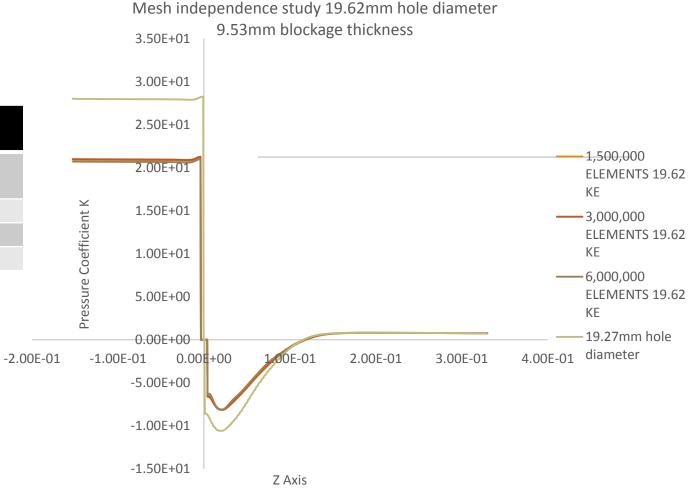


Mesh statistics for a four-hole 19.62mm stabiliser's hole diameter 9.53mm stabilizer thickness

		Model		Experiment		Ward Smith formulae	
Mesh	Number of	CD	CC	CD	CC	CD	CC
Quality	nodes						
Fine	6,000,000	0.845	0.703	0.969	0.804	0.811	0.672
Medium	2,700,000	0.839	0.699	0.969	0.804	0.811	0.672
Coarse	1,300,000	0.841	0.7	0.969	0.804	0.811	0.672

The pressure coefficient calculated from Equation (4) is K=21.678 considering $\beta=0.265$.

The thicker plate geometry has a lower pressure loss due to the shape of the geometry and the size of the hole



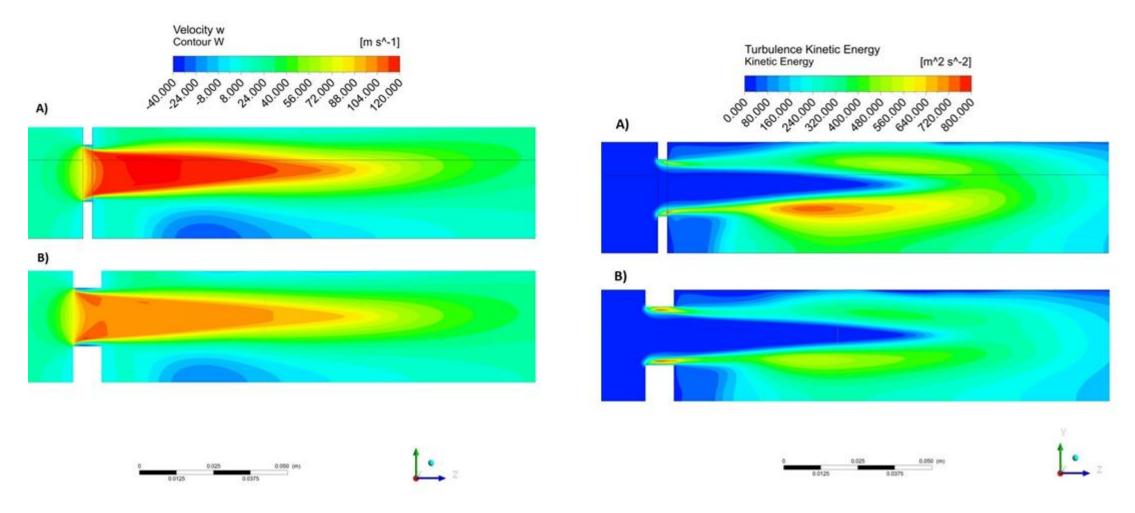
Mesh independence study for the Pressure Loss coefficient along the Z axis for the 19.62mm stabiliser's hole diameter and comparison with 19.27mm hole stabiliser diameter.

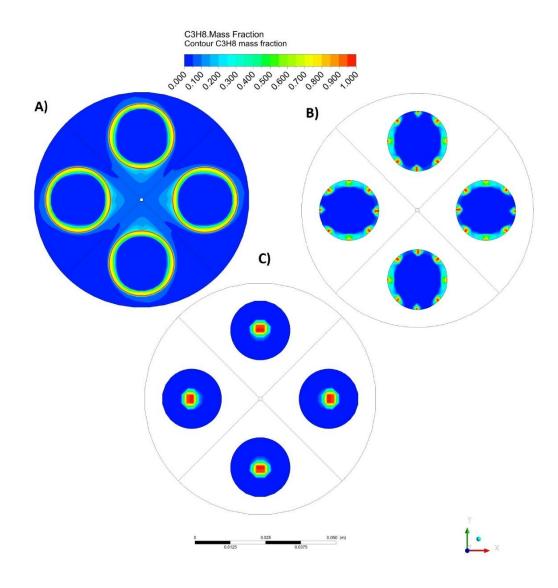
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Comparison of the 19.27 mm stabiliser's hole diameter with 3.2mm blockage thickness and the

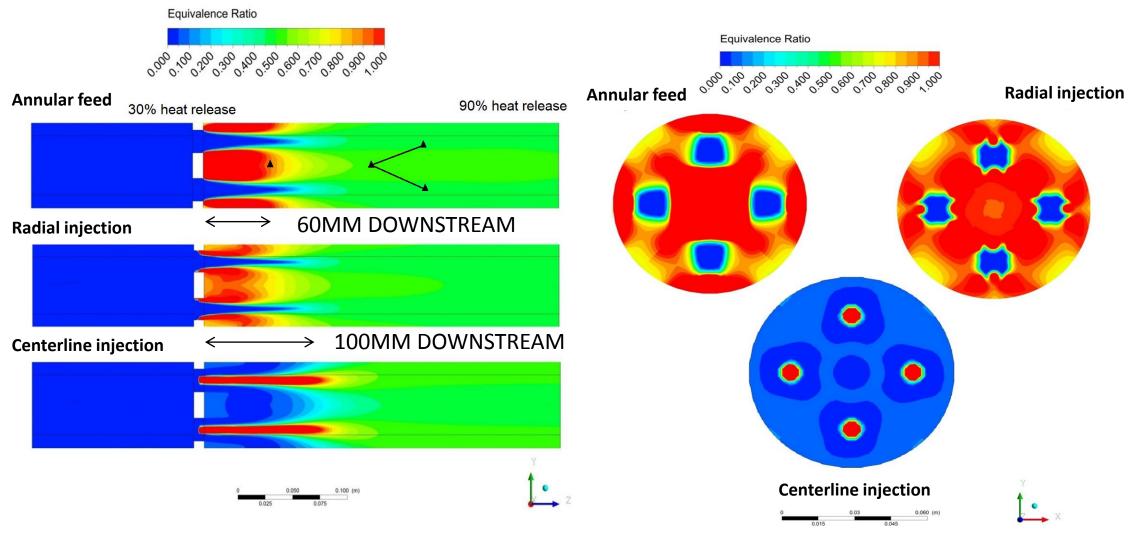
19.62mm with 9.53mm blockage thickness





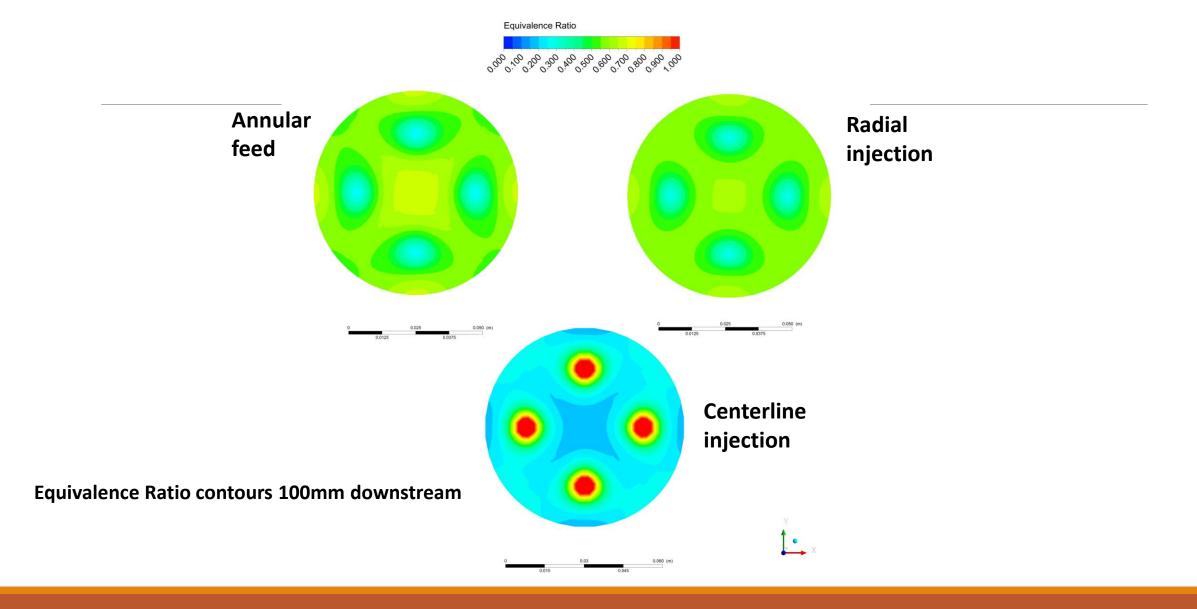
Results for mixing

Results in mass fraction for radial injection. A) Annular feed. B) Radial injection. C) Centreline injection.



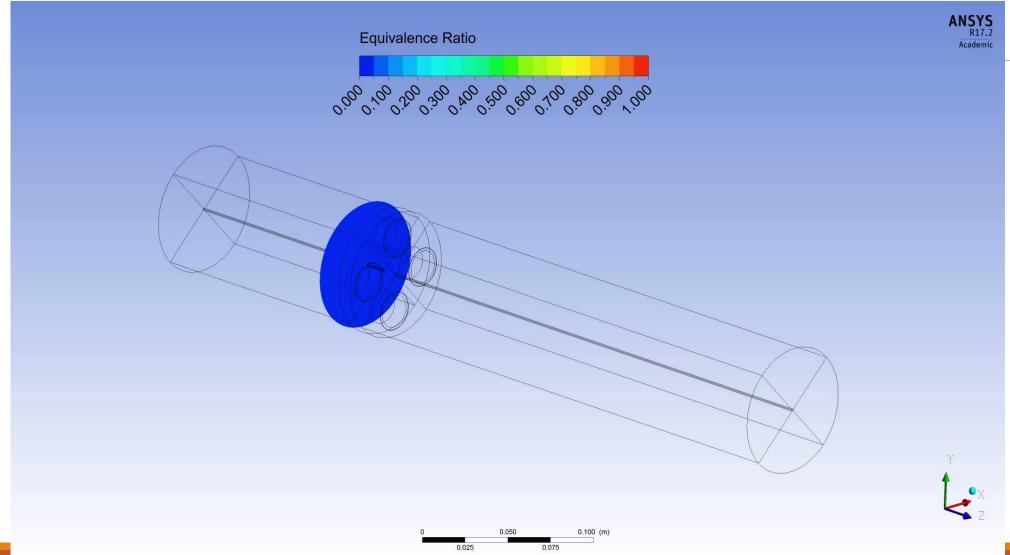
For the radial injection the propane mixes faster than in the other two cases, and this will produce lower NOx (considering half stoichiometric)

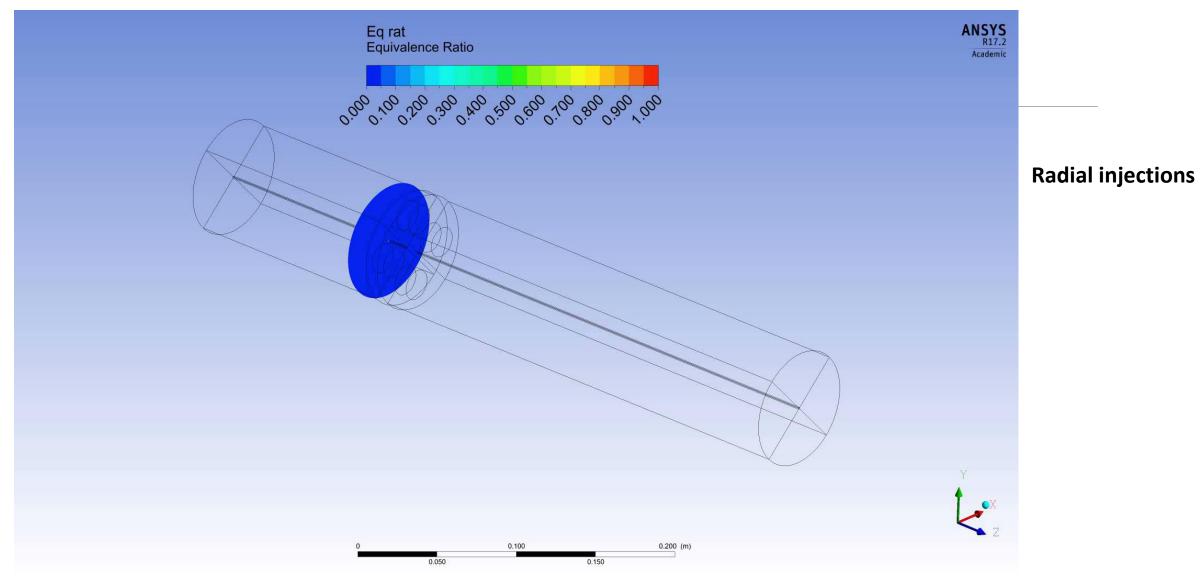
Equivalence Ratio contours 60mm downstream



Equivalence ratio for the three types of fuel injection

Annular feed

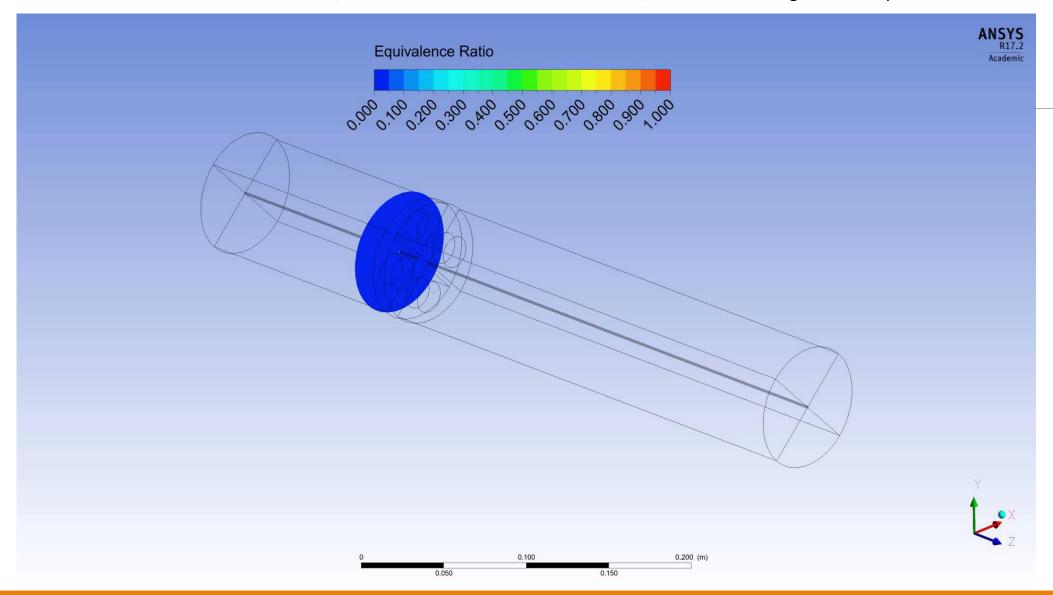




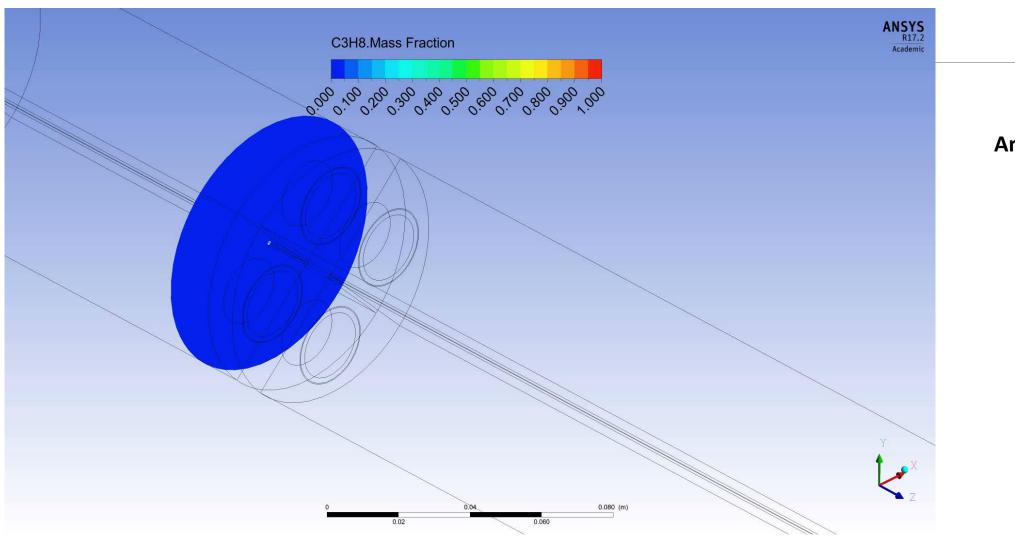
Centerline

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Mass fraction for the three types of fuel injection

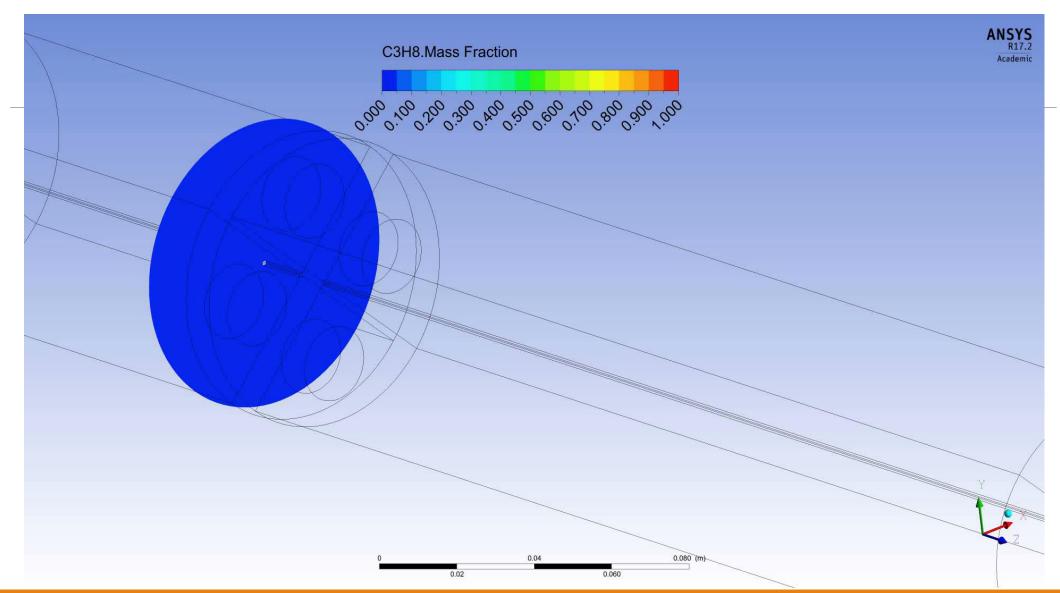


Annular feed

Radial injections

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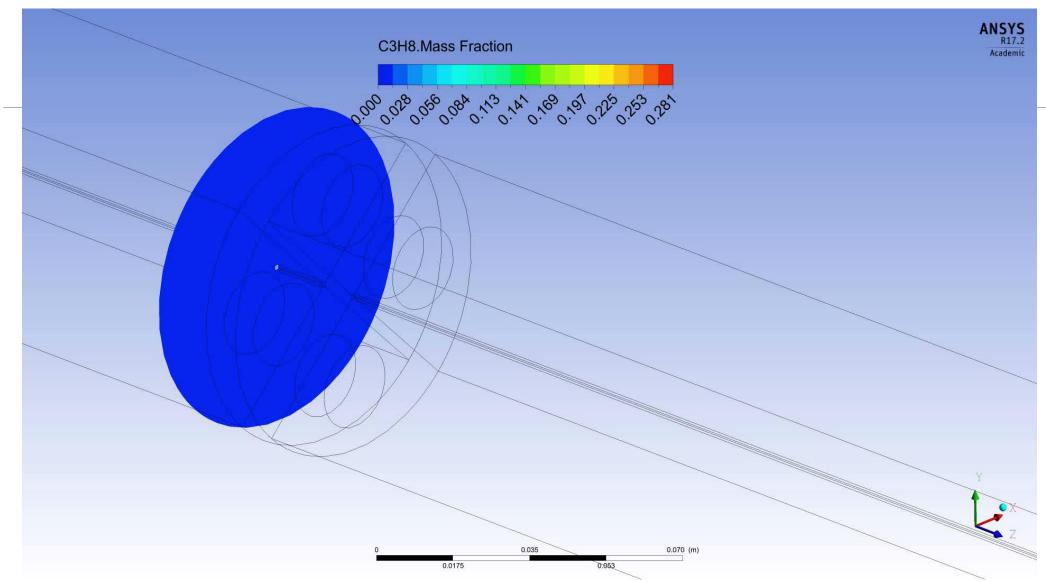
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Centerline

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Conclusions

- The results for the aerodynamics for two combustor flame stabilizer were evaluated, they were taken from the thesis "Emissions and stability of gas turbine combustors with rapid fuel and air mixing" from N. A. Al-Dabbagh (1982) considering one and four holes, as well as a thin and a thick blockage.
- There were evaluated three methods of fuel injections prior combustion
- The obtained predictions for the aerodynamics using simulation showed very good agreement with the experimental results from the thesis
- The radial injection showed to produce a quicker mixing than in the annular feed and the centreline injection so that the NOx emissions will be lower.
- It was shown that it is possible to predict NOx levels by simply looking at fuel and air mixing.

For your attention, Many thanks!